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# Investigation of Enhanced Titanium and Zinc Oxide Semiconductors for the Photodegradation of Aqueous Organic Compounds

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Investigation of Enhanced Titanium and Zinc Oxide Semiconductors for the  
Photodegradation of Aqueous Organic Compounds

by

Innocent Udom

A dissertation submitted in partial fulfillment  
of the requirements for the degree of  
Doctor of Philosophy in Chemical Engineering  
Department of Chemical and Biomedical Engineering  
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## **DEDICATION**

To my wife, Kimberly, and Son, Gabriel; my father, Peter Okon Udom, and mother, Martha

Udom.

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## ABSTRACT

Growing demand and shortages of potable water sources due to industrialization have become a great concern worldwide. Various approaches and solutions have been adopted to provide cleaner and quality water. In a preliminary study, a method of treating wastewater was investigated in which algae were used to remove nutrients (nitrogen and phosphorous) from wastewater and then the algae were harvested for use as a biofuel. The results from this investigation are included in the Appendix B. Employing traditional oxidants, such as hydrogen peroxide, chlorine, and ozone, for treatment of recalcitrant organic compounds have achieved less promising results. However, photocatalysis, an advanced oxidation process (AOP), which is a low-cost and high-efficiency technique, has been widely recognized as a promising approach for water purification and elimination of organic constituents in wastewater. Photocatalysis is the increase in the rate of a chemical reaction by employing a catalyst in the presence of photons. Generally, for a high performance photocatalyst, light of appropriate wavelength is used to activate a catalyst in close contact with contaminants, thereby modifying the rate of the reaction. The presence of these contaminants could pose potential health and environmental concerns, especially in a controlled environment such as on a space station or during long-term manned missions. Thus, the development of energy efficient and “green” technologies to reduce or eliminate organic constituents in wastewater has important potential applications.

This research investigated the supported semiconductor photocatalysts ( $\text{TiO}_2$  and  $\text{ZnO}$ ), particularly  $\text{ZnO}$  nanorods and nanowires, their synthesis methods, properties and

corresponding effectiveness in photocatalysis. The effect of transition metal co-catalysts on the photocatalytic properties of  $\text{TiO}_2$  was investigated. Although  $\text{TiO}_2$  is the most extensively studied photocatalyst for water decontamination,  $\text{ZnO}$ , as presented in this work, could be a substitute because of its lower cost, relative energy bandgap and higher visible light photoactivity. Both photocatalysts were doped and screened for the decomposition of model contaminants, rhodamine B (RhB), phenol and methyl orange, under ultraviolet and/or visible light irradiation. In the photodegradation of RhB,  $\text{TiO}_2/\text{Ru}$  1% showed a superior photocatalytic activity relative to P25- $\text{TiO}_2$  under broad-band irradiation, while doped  $\text{ZnO-Ag}$  resulted in better photodegradation of methyl orange, compared to P25- $\text{TiO}_2$ , under visible light irradiation.

The morphology and estimated chemical composition of photocatalysts were determined by energy dispersive spectroscopy (EDS) and scanning electron microscopy (SEM). Brunhauer, Emmett and Teller (BET) analysis was utilized to measure mass-specific surface area(s). A X-ray diffraction (XRD) study was carried out to confirm the identity of photocatalyst phase(s) present. The cause of low photocatalytic activity under an inert atmosphere, the simple effective fabrication technique of doped  $\text{ZnO}$  nanowires over  $\text{TiO}_2$  and properties of the photocatalyst are also discussed.

## CHAPTER 1: INTRODUCTION AND BACKGROUND

### 1.1 Introduction

Daily, an enormous amount of dyes and other organic chemicals produced by industrial processes are discharged into the environment. The presence of these contaminants in water causes considerable problems to aquatic ecosystems and public health [1-14].

Approximately 1-15% of the total dye produced in the world is wasted in the production process and released into the environment [15-17]. The discharge of these colored, contaminated wastewaters into the environment represents a significant cause of pollution and could create hazardous byproducts through chemical reactions occurring in the wastewater stream [17].

Decontamination of dyes in polluted wastewaters has therefore attracted increased attention and several purification methods have been proposed. Conventional treatment methods for textile wastewaters include coagulation, sedimentation, filtration and adsorption. Chemical oxidation processes, using chlorine, ozone, or electrochemical methods, have also been used. Problems with these processes include poor removal of color and trace organic compounds, production of chemical sludges that are difficult to dispose, and production of toxic by-products [18-21] [22, 23] . [24-26]. Forgacs et al. [27] reported that conventional wastewater treatment techniques have proven to be mostly unsuccessful for removing textile dyes from wastewater stream due to the resilient and stability of these pollutants.

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<sup>1</sup>Portions of this chapter have been previously published (I. Udom, M.K. Ram, E.K. Stefanakos, A.F. Hepp, D.Y. Goswami, One dimensional-ZnO nanostructures: Synthesis, properties and environmental applications, Materials Science in Semiconductor Processing, 16 (2013) 2070-2083.)

A large amount of textile dyes are resistant to chemical and biological degradation to be mostly unsuccessful for removing textile dyes from wastewater stream due to the resilient and stability of these pollutants; they also verified that most of the azo dyes tested in their investigation was untreated after the activation sludge process. To summarize, the aforementioned processes have wide-ranging limitations in efficacy for the decontamination of dyes from industrial wastewater.

To minimize these limitations, advanced oxidation processes (AOPs), have received enormous research attention as innovative treatment techniques [28-33]. The rationale of these AOPs is based on the production of powerful oxidant for the decomposition of “stubborn” constituents of the dyes from industrial wastewater, pathogens and trace organics [34]. Among these AOPs, heterogeneous photocatalysis is a tertiary water treatment process and has attracted increased attention in the past decades, because of its ability to completely mineralize many target pollutants [35-40].

Heterogeneous photocatalysis semiconductor using catalysts ( $\text{Fe}_2\text{O}_3$ , CdS,  $\text{TiO}_2$  and ZnO) have shown good effectiveness in photo-induced oxidation processes to decompose organic compounds and destroy pathogens, such as viruses and bacteria [41-44]. Over three decades, Titanium has become one of the significant candidates for photocatalysis and has been the most commonly studied as an environmentally friendly water treatment technology for the decontamination of organic compounds [45-49]. Titanium has been employed in the degradation of numerous organic compounds including acetaldehyde [50], acetone [51], chlorophenols [52], insecticides (e.g. monocrotophos) [53] and dyes ( Rhodamine B (*RhB*) methyl orange [54-57]. Anatase, rutile and brookite are the main crystalline phases of Titania, while anatase and rutile both exhibit higher photocatalytic activity in mixed phase. Anatase, brookite and rutile have been

reported to be most stable nanoparticle within the range of  $< 11$  nm,  $11 - 35$  nm and  $< 35$  nm, respectively [58]. Photocatalytic activities of  $\text{TiO}_2$  are greatly enhanced when doped with transition metals and some non-metals. Doping shifts the optical adsorption edge, reduces recombination rates and improves charge transfer of titanium [59]. In addition, many studies have reported that the photoreactivity of doped titanium depended on the type, energy level and concentration of dopants, as well as the distribution of dopants within the titanium lattice and the light intensity. The doping of titanium with various metals and subsequent improvement in photocatalytic results are discussed in Chapter 2 of this work.

Zinc oxide could be a substitute to  $\text{TiO}_2$  due to its similar band gap (BG) energy (3.3 eV) [60] with titanium (3.2eV) [61] and comparatively lower cost of production [62-64]. In comparison with  $\text{TiO}_2$ , ZnO is a better candidate due to the numerous point defects mainly from oxygen vacancies, higher production of hydroxyl ions and relatively greater rate of reaction. In addition, ZnO has been found to be safe and biocompatible for most environmental applications [65-69].

Figure 1 depicts schematic crystal structures of three ZnO phases: wurtzite, zinc blende and rocksalt. Generally, under normal conditions, the wurtzite structure is the most stable, while rocksalt structures may be fabricated at high pressure and the zinc blende structure can only be synthesized on cubic substrates. Wurtzite, a hexagonal crystal system belonging to the space group  $C6v4$  (No. 186,  $P6_3mc$ ), possesses two lattice parameters  $a=3.2495\text{\AA}$  and  $c=5.2069\text{\AA}$  with a ratio of  $c/a = 1.60$ . This axial value correlates with the ratio (1.633) of an ideal crystal [64][70]. Although ZnO exhibits a slight covalent bonding, the ionic character in the Zn-O is very strong. It has facets that exhibit massive surface reconstruction unlike the basal plane [71-74]. ZnO reveals a number of novel structures by modifying the fabrication conditions. One of the major

factors that predict the morphology of the fabricated structure is the relative surface activity under controlled growth conditions. However, three dimensional and well-defined crystallites with low index crystallographic faces can be developed during growth after an initial phase of seed layer formation [74].

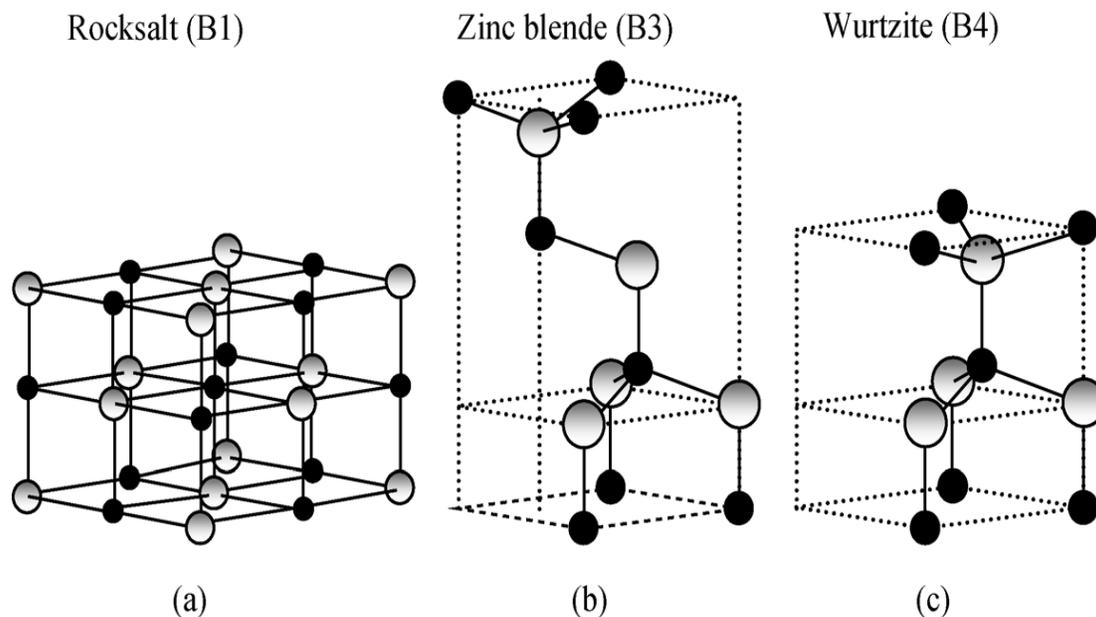


Figure 1 Stick-and-ball representation of ZnO crystal structures. (a) cubic rocksalt (B1), (b) cubic zinc blende (B3), and (c) hexagonal wurtzite (B4). Shaded gray and black spheres denote Zn and O atoms, respectively. (Reproduced with permission from [70] Copyright @ 2009 WILEY-VCH

The review presented in Chapter 2 of this dissertation assesses recent studies on ZnO nanowires, with an emphasis on one-dimensional (1D) ZnO-based nanostructures employed as photocatalysts for the decomposition of environmental contaminants, particularly textile and industrial dyes under appropriate light irradiation. In this work, we have investigated different ZnO photocatalysts, discuss their properties, and highlight fabrication techniques for the ZnO

nanowire (nanorod) and its characterization. We also present the photocatalytic degradation of selected contaminants (dyes) using the 1D-ZnO based photocatalyst.

The long term goal of this work is to develop a simple and commercial photocatalyst for the degradation and decontamination of organic pollutants in an aqueous matrix under visible irradiation. The overall objective of this research is the preliminary development of a new photocatalyst and illustration of photocatalysis as an effective technique for the decontamination of organic materials in wastewaters.

The overall objective will be achieved via the successful accomplishment of the following specific goals: (1) investigate the effect of a transition metal dopant in photocatalytic materials, (2) develop a simple, inexpensive, scalable and effective Ag-ZnO nanowire (NW) photocatalyst by modifying the morphology via a synthesizing method, and (3) optimize the photocatalytic degradation of phenol using simple photocatalytic reactor.

Although this research was not carried out with real textile wastewater, studies have shown that wastewater originating from the textile industry contains unreacted dyes, dispersing agents, surfactants, salts and organics. Generally, the wastewater is characterized by high pH variation (2-12), elevated total dissolved solids, chemical oxygen demand (COD) and color density [23].

In real textile wastewaters, surfactants could compete with other solutes for reactive sites at the surface of the photocatalyst, which could influence the photocatalytic degradation of the target compound. Other compounds in the matrix, such as dissolved organic matter and salts, can reduce the hydroxyl radicals produced at the photocatalyst surface resulting in lower photocatalytic performance. Dissolved oxygen presents an opposite effect, enhancing photocatalytic activity, by acting as electron scavenger, resulting in improved parting of

electron–hole and allowing for more proficient movement of the charge carriers into the photoreaction sites.

Finally, in order to optimize the efficiency of photocatalysis in the removal of colors from real textile wastewater, it is paramount that upstream treatment processes be applied prior to photocatalysis. Figure 2 outlines how the proposed alternative can be approached. The figure illustrates pretreatment of dye-containing wastewater by the addition of coagulants to facilitate the removal of dissolved and suspended solid by coagulation, flocculation and sedimentation. Afterward, the discharged water is biologically treated to reduce chemical oxygen demand (COD) and nutrients. The pH of the treated wastewater is then adjusted and the wastewater is aerated to achieve the optimal photocatalytic performance.

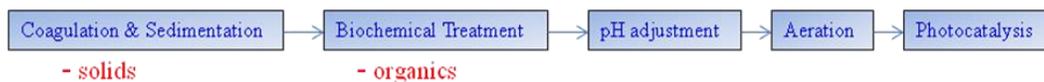


Figure 2 Alternative photocatalytic purification train for textile wastewater

## 1.2 Photocatalysts

Photocatalysis is the enhancement of a chemical reaction using a catalyst under light irradiation. Generally, the catalysts participate in and accelerate the reaction but remain unaltered at the end of the reaction. The catalyst uses the characteristics of semiconductors in a photochemical reaction to decompose organic pollutants [75]. The semiconductor possesses a band gap which separates the electron-packed valence band (VB) from the empty conduction band (CB) (Fig. 2). When a photon's energy ( $h\nu$ ) is greater than the band gap energy, it excites an electron from the valence band to the conduction band, thereby, producing an electron ( $e^-$ ) and a positive hole ( $h^+$ ), in the CB and VB, respectively. The electron ( $e^-$ ) and hole ( $h^+$ ) both

migrate to the catalyst surface to recombine or facilitate a redox reaction with compounds absorbed on the catalyst. A powerful hydroxyl radicals ( $\text{OH}^\bullet$ ), is produced from the combination of  $\text{H}_2\text{O}$  and/or  $\text{H}_2\text{O}_2$  with the positive hole ( $\text{h}^+$ ), that oxidize the organic compounds in the photocatalytic system. Simultaneously, oxygen atoms absorbed on the photocatalyst are reduced by the electrons in the conduction band [76, 77].

As illustrated in Fig. 3, during the photocatalytic process, superoxide radical ( $\text{O}_2^\bullet$ ), and other reactive groups are produced, resulting from reactions with moisture oxygen ( $\text{O}_2$ ). Although  $\text{ZnO}$  and  $\text{TiO}_2$  have similar bandgaps and low production cost, more recently,  $\text{ZnO}$  has been investigated by a large body of researchers due to its higher photoactivity (by a factor of 2-3) in visible light irradiation for the decontamination of water [78, 79]. Furthermore, due to

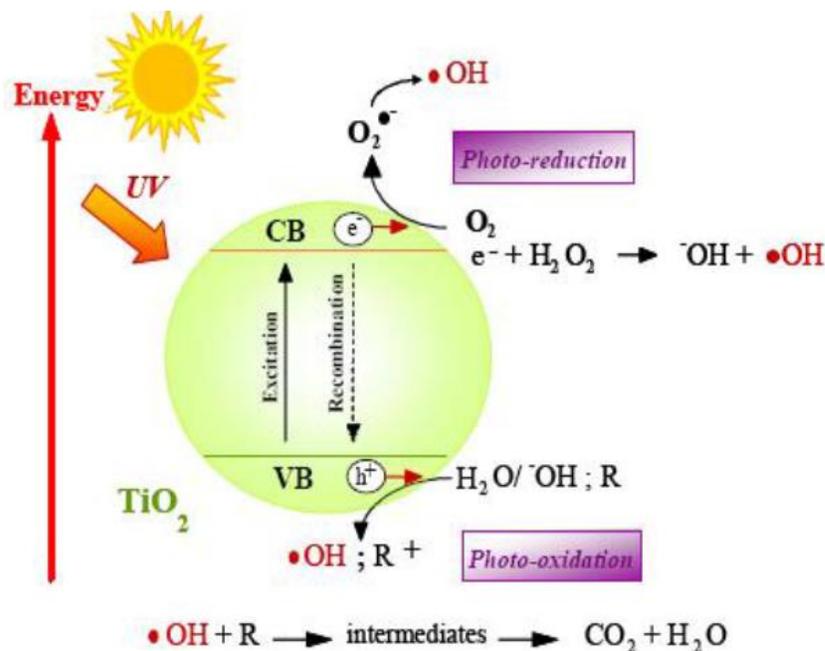


Figure 3 A schematic of the principle of photocatalysis (reproduced with permission from [52] © 2010 Elsevier)

$\text{ZnO}$ 's higher efficiency in the production of hydroxyl radicals ( $\text{OH}^\bullet$ ) and reduced recombination of photoinduced electron-hole pairs, it has been considered to be more photoactive [80-86].

Generally, the surface area as well as the number of defects on the surface of the catalyst are significant for effective photochemical reaction. Although nanoparticles offer a larger surface area, they are limited in their use in a water suspension because of the difficulty and high cost of separation and recovery. One dimensional (1D) nanostructures, such as nanorods (NRs) and nanowires (NWs), present improved photocatalytic performance [87-89], and could be well aligned on most surfaces with no post-treatment of the catalyst. A comparison of various ZnO nanostructures for photocatalytic applications is presented in Table 1.

Table 1 Comparison of different ZnO nanostructures used in photocatalytic applications (reproduced with permission from [80] © 2012 Hindawi Publishing Corporation)

Nanoparticles		Nanowires		Nanothin film	
Advantages	Disadvantages	Advantages	Disadvantages	Advantages	Disadvantages
Could be suspended in a solution	Particles aggregation in a solution leads to a reduced surface area	Growth could be well aligned on most substrates	Growth conditions are most restricted	Coated on certain substrates	Lower performance because of small surface area
High performance because of larger surface areas	Post-treatment for catalyst removal is required	Offer larger surface area compared to Nanothin film	Lower surface area compared to nanoparticles	Post-treatment for catalyst removal is not required	
	Difficult to recover all the catalyst	Post-treatment for catalyst removal is not required			
		Lower crystallinity and more defects			

As illustrated, 1D nanostructures, such as nanowires, nanorods and nanotubes, provide elevated aspect ratio (surface area to volume ratio) in contrast to thin films (two-dimensional nanostructures). Among the one-dimensional nanostructures, zinc oxide NWs has been significantly studied because of their simple fabrication techniques and applications [52-56].

### **1.3 Synthesis of ZnO Nanowires**

There are two primary approaches for the fabrication of ZnO nanomaterials: Gas phase synthesis (GPS) and solution phase synthesis, the section that follows includes a description of each method as well as an overview of the advantages and disadvantages.

#### **1.3.1 Gas Phase Synthesis**

Gas phase synthesis (GPS) includes several synthesis processes such as: vapor-liquid-solid (VLS) growth [81][90], chemical vapor deposition (CVD) [82][91], metal organic chemical vapor deposition (MOCVD) [83][92], physical vapor deposition (PVD) [84][93], molecular beam epitaxy (MBE) [85][94], metal organic vapor epitaxy (MOVPE) and pulsed laser deposition (PLD) [95]. GPS is the most commonly used-approach for the fabrication of 1D nanostructures [87][96]. Generally, the ZnO source material is sublimed with the assistance of elevated temperature (500-1500°C) and low pressure. Under specific conditions, the vapor condenses onto a surface of a solid substrate and produces high-quality nanowires/nanorods, nanobelts, nanobows, nanohelices/nanorings. Because the growth conditions can be better manipulated, nanowires/rods are predominately produced by using a horizontal tube furnace, an alumina tube, and a gas supply.

Although the vapor-liquid-solid (VLS) process was initially developed by Wagner and Ellis to fabricate microstructures over four decades ago [88][97], recently, it has been modified and broadly employed for the synthesis of 1D nanorods. It is a simpler, less expensive method

and can be employed to grow ZnO on large wafers [89][98]. In a VLS fabrication method, ZnO nanoparticles will nucleate homogeneously once the thermodynamic kinetic and supersaturation conditions are favorable, followed by an orderly growth of the crystalline wires and rods. Wang et al. [99] successfully fabricated precisely ordered zinc oxide nanowire arrays on specific substrates (GaN and Al<sub>0.5</sub>Ga<sub>0.5</sub>N).

Using the VLS method aligned large scale zinc oxide nanowires have been effectively synthesized on nitrides and on a common contact [100, 101]. Furthermore, Chu et al. [93][102] adopted the VLS method to produce well-aligned ZnO nanowires for enhanced photocatalytic and field properties by optimizing the aspect ratio, temperature (600-950 °C) and pressure (0.75-3 torr). They also reported a decrease in the growth rate and length of the nanowires at elevated chamber pressures.

Another common fabrication technique used to produce ZnO nanowires is CVD. Protasova et al. [82] reported a novel production technique to grow Palladium doped on the surface of zinc oxide catalysts. The fabricated catalyst was employed in the hydrogenation of acetylene alcohols. The well arranged zinc oxide nanowires were fabricated by CVD technique onto a zinc oxide seed layer by an atomic layer deposition at 553K. This method provides a strict control of the growth of the nanowires at various stages. After numerous reaction cycles, the as prepared ZnO nanowires showed stability and relative same performance at 323K.

MOCVD is a catalyst-free-low-temperature method of fabricating ZnO nanowires. The MOCVD of ZnO, compared to other deposition techniques, presents a number of benefits, including the potential for larger amount of composition, easy shape control and commercial scale fabrication process. In addition, well arranged zinc oxide nanowires can be fabricated without the initial formation of a seed layer. Fabrication of high quality ZnO at low temperature

via MOCVD offers great potential for higher performance nanoscale photonic and electronic device applications.

Ashraf et al. [83] investigated the synthesis of well-aligned ZnO nanowire via the MOVCD technique using chelating bidentate ether adducts of dimethylzinc. They showed that the latter prevents initial reaction with oxygen and, under most favorable conditions, leads to the fabrication of well arranged zinc oxide NWs by MOCVD. The nanowires were prepared in the absence of a seed layer on a glass substrate and silicon wafer. In another paper, Zeng et al. [103] used near 100% purity diethylzinc and nitrous oxide ( $N_2O$ ) to supply zinc and oxygen, respectively, at an optimal working pressure ( $10^{-5}$  – 50 torr) and temperature (400-650°C) to fabricate well arranged ZnO NWs.

Physical vapor deposition (PVD), like vapor-solid (VS) processing, involves the sublimation of a source material without the use of a catalyst [96]. Typically, the PVD technique is a combination of thermal evaporation, oxidation (Zn powder) and deposition of ZnO nanowires on a substrate. Tigli and Juhala [104] reported the growth of high quality ZnO NWs by subliming Zn powder at elevated temperature and deposition of the vapor on the silicon substrate at about 500°C in a relatively lower temperature chamber. Zhang et al. [105] fabricated numerous high quality ZnO NWs using the PVD method. In another fabrication via PVD, they obtained well arranged superior ZnO nanowires on Si substrates with high aspect ratio and uniform diameter (100 nm). The ZnO nanowires were synthesized in a reactor chamber, with Zn powder as the  $Zn^{+2}$  source, at a rapidly elevated temperature (500°C) under the stream of a  $N_2$  gas flowing at 50  $cm^3/min$  for 60 minutes.

### 1.3.2 Solution Phase Synthesis

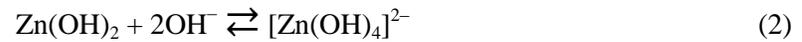
Typically, the fabrication technique in a solution phase process is carried out in an aqueous solution, such as an organic solution, at a relatively low temperature (<200°C). Currently, the solution phase synthesis technique has emerged as one of the most important methods due to its numerous advantages, such as low production cost, scalability and reduced temperature.

Hydrothermal synthesis provides another commonly used methodology for generating ZnO NWs or NRs [106, 107]. “Growth occurs at a relatively low temperature, compatible with flexible organic substrates; there is no need for the use of metal catalysts, and thus it can be integrated with well-developed silicon technologies” [108]; and, also there a number of variables that can be effectively controlled to provide the desired morphologies and properties of the prepared catalyst. Hydrothermal synthesis is superior to other solution phase techniques due to the many point defects of ZnO NWs mainly because of oxygen vacancies [42]. Baruah and Dutta [109] showed the enhancement of the photocatalytic activities of ZnO NW by intentionally creating defects in the crystal lattice through the hydrothermal method without doping with transition metals. The typical mechanism for well-aligned ZnO NWs fabricated on specific surfaces is as follows:

- a. The ZnO nanoparticle forms a seed layer on the surface by sputtering or spin coating. At a lower activation energy, the film induces a homogeneous nucleation and a precisely ordered array of ZnO nanowires; lower energy non-polar planes being more stable [110, 111].

- b. A commonly used precursor (growing solution) is prepared that contains an aqueous-mixture of an alkaline reagent, such as NaOH or hexamethylenetetramine (HMT), also known as hexamine, and zinc nitrate (source of  $Zn^{2+}$ ).
- c. The substrate is then positioned upturned such that the seeded plane faced down in the growth solution for certain duration of time and temperature. The resultant product is washed and dried.

Generally, NaOH and KOH are the most frequently used alkali compounds in the preparation of zinc oxide via a solution phase method. Typically, “the solubility of ZnO in an alkali solution increases with the alkali concentration and temperature, and super saturation allows a growth zone to be attained” [112]. Usually, potassium hydroxide is preferred to sodium hydroxide due to the lower possibility of integration of potassium ion,  $K^+$ , into the zinc oxide lattice because of its bigger radius ( $K_r^+ > Na_r^+$ ) [113]. In addition, the development of a capping layer by the sodium hydroxide ions prevents the formation of nanocrystals during the fabrication process. The major reactions involved in the formation are shown by the following equations [114, 115]:



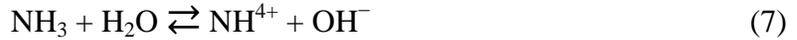


Table 2 Comparison of ZnO NWs growth mediated by alkaline or HTM solutions [122-126]

ZnO NWs growth mediated by alkaline solution	ZnO NWs growth mediated by HTM aqueous solution
Commonly used alkali compounds: KOH and NaOH.	
O <sup>2-</sup> ions in ZnO comes from the base not from the solvent (H <sub>2</sub> O)	H <sub>2</sub> O molecules provides the O <sup>2-</sup> ions
Growth does not necessary require solvent to be water could be organic solvents e.g methanol, ethanol or even ionic liquids	HMT hydrolyze in water (main solvent) and produces HCHO and NH <sub>3</sub>
Polarity and saturated vapor pressure of the solvents control ZnO NWs morphology	Growth time and temperature control the ZnO NWs morphology.
Aspect ratio (AP) of ZnO NWs is directed by the relative growth rate of polar and nonpolar surfaces; AP increases on going from more polar solvent methanol to less polar solvent 1-butanol.	Aspect ratio of ZnO NWs is dictated by the growth time and temperature.
Under alkali conditions, the reactions could take place at room temperature by adjusting the ratio of Zn <sup>2+</sup> and OH	There's an increase in entropy during reaction, so increasing the reaction temperature will push the equilibrium forward.

In equation (2), the product could be in the form of ZnOH<sup>+</sup>, Zn(OH)<sub>2</sub> or Zn(OH)<sub>3</sub><sup>-</sup>, depending on certain parameters such as the pH value and the concentration of Zn<sup>2+</sup>. When hexamethylenetetramine (CH<sub>2</sub>)<sub>6</sub>N<sub>4</sub> or HTM and Zn(NO<sub>3</sub>)<sub>2</sub> are chosen as precursors, the main reactions involved in the growth are illustrated by the following equations [116-118]. Equations (1) to (5) summarize the reaction process, however, in reality; the process is more complicated than what has been expressed above. For example, O<sub>2</sub> plays a important function in the formation

of the final crystal quality of the ZnO NW. Tang et al. [119] reported that high quality ZnO NW was grown with sharp top surfaces when  $\text{H}_2\text{O}_2$ , which decomposes into  $\text{H}_2\text{O}$  and  $\text{O}_2$ , was added to the growth solution. Conversely, other researchers have suggested the formation of very ragged surfaces if the solution (synthesized with steam distilled water) is used in the process to eliminate the dissolved  $\text{O}_2$ . Preparation of ZnO nanowires using  $\text{Zn}(\text{NO}_3)_2$  and HMT as precursors, is most commonly used in the hydrothermal method [120, 121]. Table 2 compares the ZnO NW mediated by an alkaline and HTM aqueous solution, the latter providing the  $\text{Zn}^{2+}$  ions required for the formation of ZnO nanowires. The  $\text{H}_2\text{O}$  molecules provide  $\text{O}^{2-}$  ions in the system unlike the alkali-mediated process. There are many advantages of the ZnO NWs growth mediated by HTM as shown in the Table 2.

### **1.3.3 ZnO Seeding Layer on Substrates**

Besides cost effectiveness and scalability, the major benefit of wet chemical methods is that zinc oxide seeds can be used in the formation of thin films or nanoparticles. ZnO NWs can be developed on numerous substrates including silicon wafers (smooth [112], pillar array [127], dimethicone E900 [128], thermoplastic polyurethanes (TPU) [129], paper [121], fibers [130-132] and carbon fibers [133]. The bond of the nucleation layer (seedling layer) to the substrate is important to improve the quality of the NWs vertically grown alignment. Kang et al. [134] reported the dependence of NWs on the Si substrate orientation. Qin et al. [137] suggested that the “adhesion of the seed layer to the substrate can be improved by depositing an intermediate metal layer, such as Cr or Ti, on inorganic substrates, and by introducing an interfacial bonding layer, such as tetraethoxysilane molecules, on a polymer substrate”. Green et al. [135] examined the influence of calcination on the growth of the seed layer and formation of well-aligned ZnO NWs. They reported that the optimal temperature ranges for seed alignment and seed

crystallinity were 100 to 350°C and 150 to 200 °C, respectively. At a temperature of 350°C, images revealed a uniform film of ZnO nanoparticles, while for  $T > 450^\circ\text{C}$ , more nanoparticles were crystallized [136]. Because of the rapid oxidation of zinc film in air or in aqueous solution, it can be employed as a potential seedling layer [137]. Fang et al. [138] effectively fabricated uniform, well arranged, and ultrathin zinc oxide nanowires on a zinc material by the hydrothermal treatment of a zinc foil in a mixture containing water, alcohol and ammonia, at lower temperature in the absence of a catalyst. They demonstrated that the thickness of the zinc oxide seed layer affects the morphology of the zinc oxide nanowires preparation.

Gbayour et al. [139] investigated the effect of the ZnO film thickness on the morphology of the ZnO nanorods, and concluded that the aspect ratio and the density decreased as the film thickness increased.. In another experiment, an increment in seed layer thickness resulted in an increase in diameter (50 to 130 nm) and decrease in nanorods (wire) density ( $110$  to  $60 \mu\text{m}^{-2}$ ) [140]. Liu et al. [141] established that, when the thickness of the nucleation layer (seed layer) was increased from 1.5 nm to 3.5 nm by sputtering, the concentration of the ZnO arrays changed from  $6.8 \times 10^4$  to  $2.6 \times 10^{10}$  nanowires/cm<sup>2</sup>. The effect of epitaxial growth of ZnO films with different thickness, 40-120 nm, on the preparation of ZnO nanorods was investigated by Solis-Pomar et al. [142]. The result revealed that nanorods with ~34.5 nm diameter were obtained from 40-nm films, and ~51.5 diameter from 120-nm film. When the seed layer thickness was beyond the range  $6.8 \times 10^4$  to  $2.6 \times 10^{10}$  nanowires/cm<sup>2</sup>, the nanowire density was less sensitive. No formation of ZnO NWs can be achieved if the seedling layer thickness is extremely low, due to the effect of the surface area and the partial molar free energy of the multi-crystalline layers. Generally, the heteronucleation is favored over homogeneous nucleation due to the higher activation energy barrier associated with the latter. To facilitate the nucleation and growth of

well aligned nanowires, the substrate and crystal must have an interfacial energy which is lesser than the energy between solution and crystals.

Again, in some cases, in the absence of zinc oxide seed layer, nanowires could still be fabricated on a substrate. Tian et al. [143] developed a “simple seedless method for growing vertical, ultradense and ultra long ZnO nanowire arrays on Au/glass and Au/Si substrates. By adding an adequate amount of ammonium hydroxide to the nutrient solution, the density and the growth rate of ZnO nanowires significantly increased. ZnO nanowires of more than 22  $\mu\text{m}$  long could be readily obtained within 24 h without refreshing the nutrient solution”.

#### **1.4 Doping of Zinc Oxide Nanowires**

A number of groups have reported on doping as the primary technique of modifying semiconductors characteristic such as electrical conductivity. Several metals including Co [144], Ga [145], Eu [146], Al [147], Cu [148], and Ni [149], and non-metals such as: C [150], N [151], P [152], and Cl [153] have been effectively integrated inside the crystalline lattice of zinc oxide nanowires.

Zhou et al. [154], for example, “produced wool-like films of  $\sim 65$  nm diameter ZnO nanowires doped with 1-5 % of Cu by using intermixed CuI-  $\text{ZnI}_2$  powders as the growth precursors”. The data from XRD, TEM, and high-resolution TEM microscopy propose that the nanowires are monocrystals, with the fast-growth path equivalent with vertical orientation (101). They” also show that other precursors, particularly high purity powders of Cu, Zn, and graphite mixed in the proportion of Zn:Cu:C=3:1:1 can be also used to produce crystalline Cu:ZnO nanowires. In this case, the growth of the nanowires was achieved at  $\sim 800$   $^{\circ}\text{C}$  in an Argon atmosphere with an Argon flow rate maintained at 0.12 L/min”.

Li et al. [155] doped ZnO NWs with Cr, Co and Mn using an aqueous solution of zinc nitrate, HTM and hydrated nitrates of the dopants (Cr, Co and Mn). Gu et al. [156] fabricated heterogeneous Ag/ ZnO NWs via a facile 2-stage chemical technique in a commercial scale. The heterogeneous catalyst consisted of extremely dense well arranged (0001) zinc oxide nanowires as branches and numerous individual crystals of silver nanorods as trunks. After zinc oxide nanowires (diameter 60-400 nm) were fabricated on the 6 sided-surfaces of the silver doped nanorods. Das et al. [154] used a hydrothermal by sputtering method to fabricate co-doped ZnO nanowires. The latter was heated in a NH<sub>3</sub>-saturated reactor chamber at 500°C for 30 min. Wang et al. [157] “demonstrated the deposition of large-scale ZnO–CdTe core–shell nanowire arrays on indium-tin-oxide (ITO) substrates through a electrodeposition method (pH 8.3), which was compatible with the ZnO nanowires”.

## 1.5 Properties

Scanning electron microscopy and X-ray diffraction methods have been employed to characterize ZnO NW array structures. Figure 3 illustrates the SEM image of the as-prepared ZnO NWs with a diameter < 100nm. As observed, well-aligned ZnO NWs with hexagonal tips were produced and position perpendicular to the substrate surface. Figure 4 shows the XRD pattern of ZnO nanowire arrays and thin films. Although there are some extra peaks in Spectrum b to Spectrum a, the predominant peak from the (002) atomic plane shows that the ZnO nanowire structures were fabricated with a c-axis orientation normal to the material surface, data from SEM and XD revealed the hexagonal crystal structure of ZnO nanowires.

Transmission electron microscopy (TEM) was employed to describe the fabricated ZnO NWs and to examine the effect of elevated temperature on its structure. Figure 5a depicts a TEM data which illustrates the crystallinity of the nanowires with average diameter of about 150-200

nm. The data also show a significant consistency in the aspect ratio in the density of the nanowires [158]. HRTEM and SAED data in Fig. 5b show the high-purity of the fabricated nanowires. It established that a well arranged vertical zinc oxide NWs are produced due to the lowest surface energy between the crystal and the solution [159]. “The (0 0 2) texture of the zinc oxide NW must form in an effective equilibrium state where enough surface mobility is given to impinging atoms under a certain deposition condition” [160].

Raman measurements were used to explore the sample features and purity, so as to comprehend the phonon-electron interaction of the material [161]. In Figure 6, dominant peaks ( $100 - 438 \text{ cm}^{-1}$ ), represented by the E2 optical mode were observed, which are usually identified in the wurtzite structure of zinc oxide. A more careful study of the E2 on the elevated mode of prepared samples shows that the crystalline superiority of the zinc oxide thin films was enhanced with increased temperature. For instance, well-aligned zinc oxide crystal material was achieved when the Raman spectrum of the ZnO film was prepared at an elevated temperature ( $400 \text{ }^\circ\text{C}$ ).

The superior morphology of zinc oxide nanostructures, including the presence of profound native defects can be examined by photoluminescence (PL) [162]. Figure 7a shows a PL spectrum of the fabricated sample consisting of a wide asymmetric near bandgap band with a prominent tail in the area of low energy photons. Similarly, the same observation has been previously reported by using vastly doped zinc oxide samples fabricated by diverse techniques [99]. Typically, a PL band is due to the direct movement of electrons between the CB to the VB tail. Furthermore, the elevated concentration of native defects produces broadening band edges due to induced potential fluctuations [163]. The hydrothermal treatment ( $> 400 \text{ }^\circ\text{C}$ ) of the sample produces a truncated PL band and elevates the intensity by multiple folds (Fig. 7b). Heating the

sample in air within the temperature range 150–400 °C also elevates the PL intensity by three times (Fig. 7c and d) [149]. The broadening of the PL band involved can be accounted for by the broadening of the band edges due to potential fluctuations induced by the high concentration of intrinsic defects or impurities. The width of the band tails, and the dependence of the full width at half-maximum (FWHM) of the PL band on carrier concentration, can be calculated using the model for broadening of impurity bands in heavily doped zinc oxide. The electron density in the prepared sample can be estimated by the correlation of the different treatment temperature of the sample as a function of FWHM in the PL band.

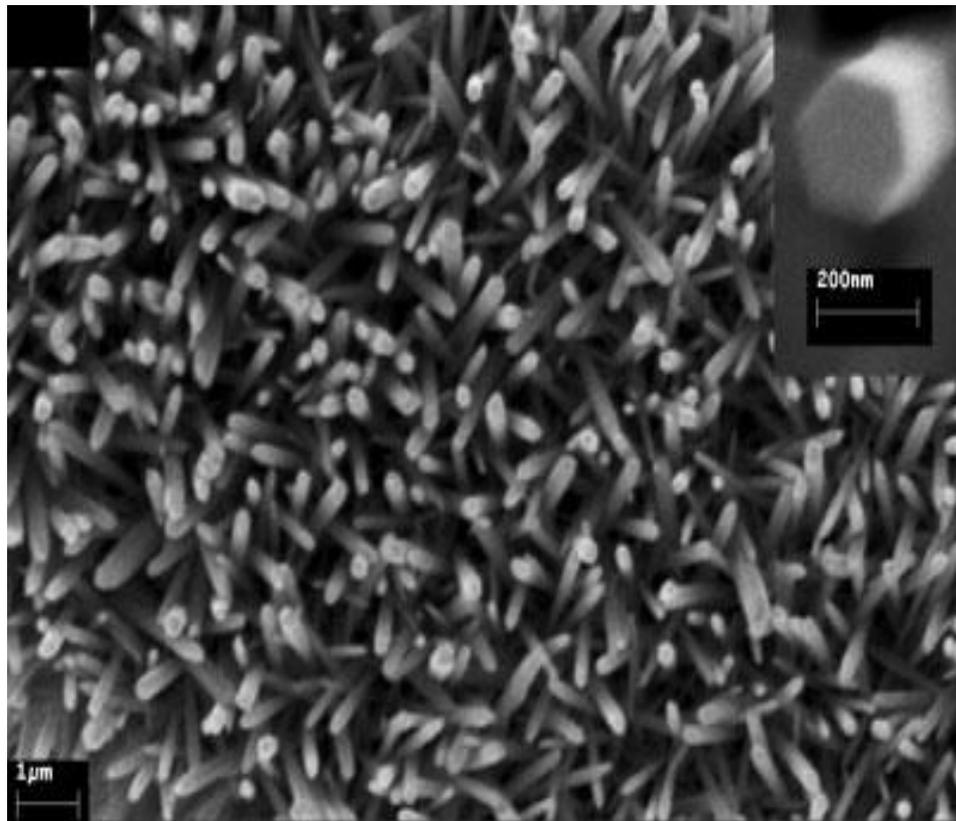


Figure 4 Scanning electron microscopy (FE-SEM) images of ZnO nanorods (reproduced with permission from [164] ©2003, Elsevier)

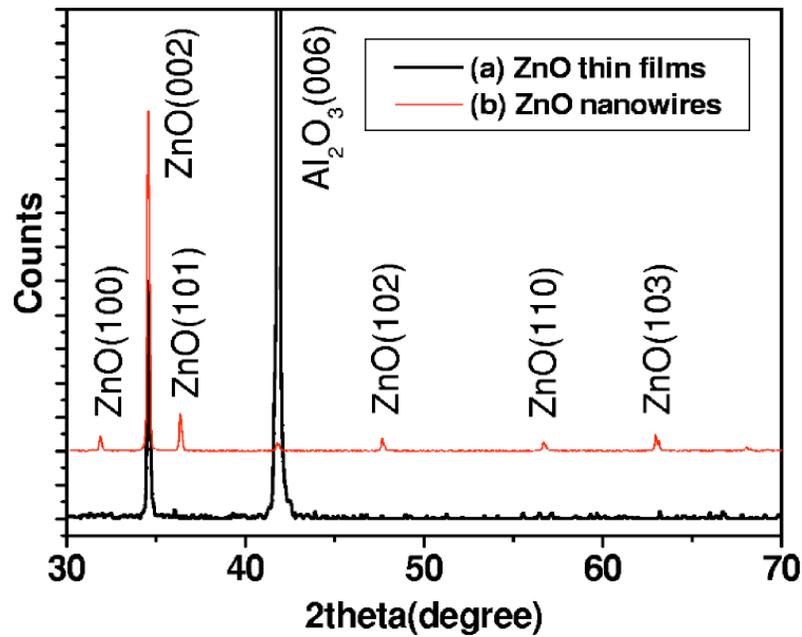


Figure 5 XRD results of ZnO thin films and synthesized ZnO nanowire arrays (reproduced with permission from [64] @ 2005 The American Institute of Physics)

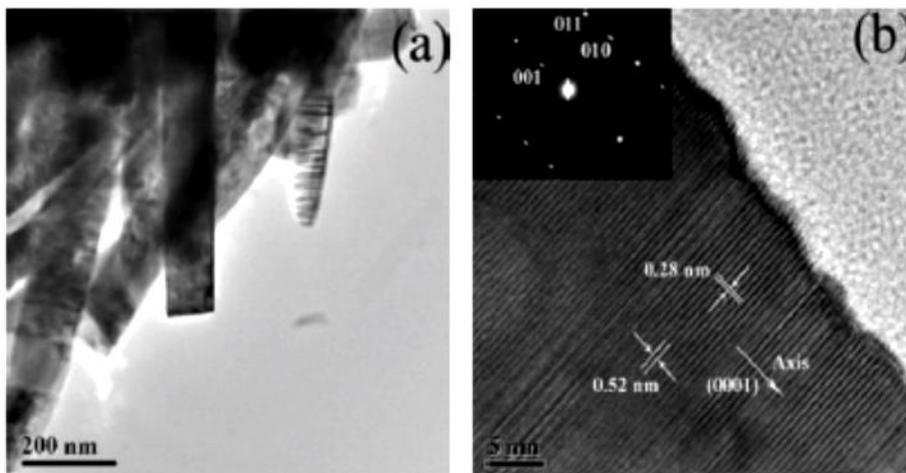


Figure 6 TEM and HRTEM data of ZnO NW. (a) A general view of TEM of ZnO nanowires on an ITO substrate. (b) Individual nanowires with [0 0 2] growth direction shown in HRTEM image. The inset shows selected electron diffraction (SAED) patterns (reproduced with permission from [149] ©2010, Elsevier).

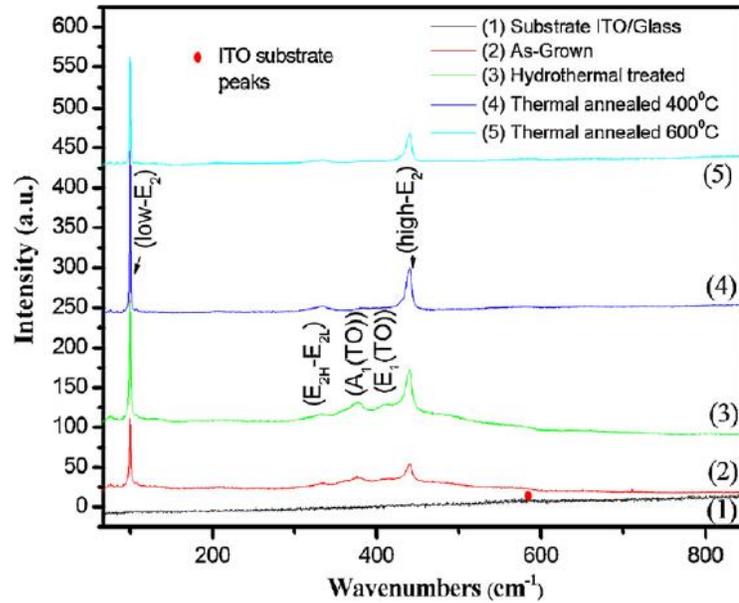


Figure 7 Raman spectra of hydrothermally treated ZnO NW (reproduced with permission from [149] ©2010, Elsevier)

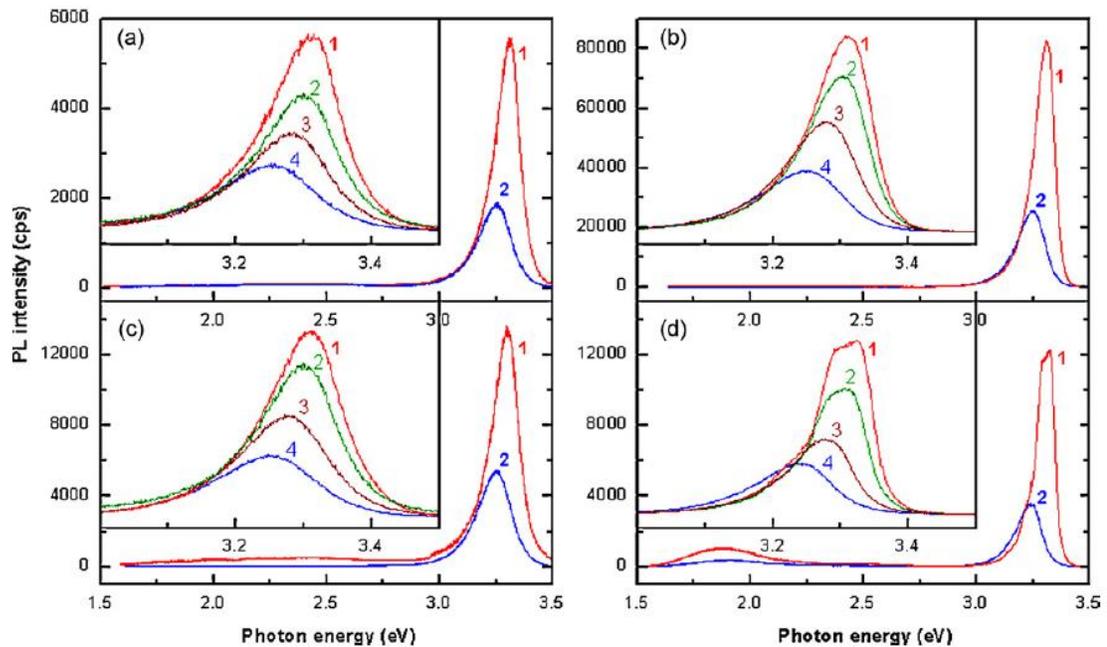


Figure 8 Bandgap photoluminescence (PL) data of doped ZnO NW. (a) Near bandgap PL spectrum of the as-prepared sample with ZnO NWs on an ITO substrate; (b) the sample subjected to the HT treatment; (c) the sample annealed in air at 150 °C (c); and (d) 400 °C. The spectra were measured at  $T = 10\text{K}$  (curve 1) and  $T = 300\text{K}$  (curve 2). Inset shows the spectra measured in the near bandgap spectral ranges (reproduced with permission from [149] ©2010, Elsevier).

## 1.6 Photocatalytic Applications

Photocatalysis is one of the main application areas of zinc oxide NWs where the native surface defect play the most essential role. “The photocatalytic activity of the ZnO NW is expected to be enhanced not only because of its increased surface area and aspect ratio but also because of changes of surface properties such as surface defects and oxygen vacancies” [165]. Sugunan et al. [166] described the incorporation of a synthesized ZnO NW, on a poly-L-lactide nanofiber in a continuous flow system, for photocatalytic water decontamination. Several organic contaminants that have been mineralized under UV irradiation include monocrotophos (MCP, an organophosphate insecticide), N-Phenylbenzenamine (DPA) and methylene blue. The authors also reported good photocatalytic mineralization of multiple organic pollutants, the scalability of the entire photocatalytic water purification system and that it can be used in remote or rural areas.

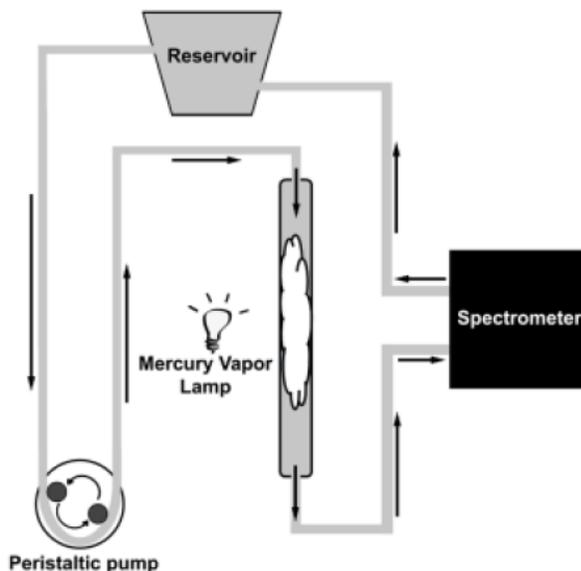


Figure 9 Schematic of a continuous – flow photocatalytic water treatment system (reproduced with permission from [157] © 2010 The American Ceramic Society)

Table 3 shows a selected list of common wastewater dyes /organic contaminates degraded using one-dimensional (1D) ZnO nanostructures. Liu et al. [158][167] demonstrated the preparation of ZnO nanofibers from a solution using *N,N*-dimethylmethanamide (DMF)/propanone, cellulose acetate (CA) and zinc acetate (ZnAc), are employed as a solvent, a fiber template and a precursor, respectively. They reported that “from the solution system, ZnO nanoparticles smaller than 40 nm in diameter are obtained by the direct calcination of ZnAc/CA composite nanofibers, whereas ZnO fibers with radii down to about 12 nm are synthesized by the calcination of Zn (OH)<sub>2</sub> cellulose composite nanofibers, which is obtained from the hydrolysis of ZnAc/CA composite nanofibers in a base solution” [158]. The photocatalytic performance of zinc oxide nanorods was assessed and evaluated with that of zinc oxide particles by measuring the photodegradation of dyes, including Rhodamine and Amido black 10B. ZnO nanofibers with a diameter of 23 nm, under visible light irradiation for 1 hr, demonstrated higher photocatalytic efficiency (30%) than ZnO nanoparticles (14%) in degrading some RhB. Additionally, Li et al. [158] reported the” porphyrin heteroaggregate modified ZnO microrods, prepared by simply mixing ZnO microrods with the TAPPI-CoTPPS porphyrin heteroaggregate”. The enhanced photocatalysts demonstrate a vital bond involving the zinc oxide and porphyrin heteroaggregate, which is essential to channel electron from porphyrin to the CB of the zinc oxide nanostructure. They reported that ZnO/TAPPI-CoTPPS is a very effective photocatalyst for the photodecomposition of RhB (16%/h) in aqueous solution under visible light irradiation. This could be extended to water purification in a wastewater treatment sector.

In another decontamination study, using ZnO NWs, Zhao et al. [150] fabricated homogeneous silver coated ZnO NW arrays. Dried zinc oxide arrays were immersed into an aqueous solution of AgNO<sub>3</sub>, and subsequently placed in growth solution to initiate the deposition

of Ag film. The decomposition of RhG dye molecules by NaBH<sub>4</sub> was studied in the absence and presence of the fabricated Ag-coated zinc oxide NW arrays. Evidently, without the photocatalyst, R6G was photodecomposed by ~70%/hr. While 80% photodecomposition of R6G was achieved using zinc oxide NWs and Ag-coated zinc oxide NWs at about 0.5 h and 0.25 h, respectively.

Baruah et al. [151] fabricated ZnO nanorods via a simple hydrothermal technique. Zinc oxide nanorods were tightly attached to cellulose fibers and the fabricated materials were used multiple times during the experiment. Photodecomposition of about 93% and 35% were achieved for methyl blue and methyl orange, respectively, under the irradiation of white light at 963W/m<sup>2</sup> for 2 hrs in the presence fabricated photocatalyst (zinc oxide NRs).

Gu et al. [147] investigated the fabrication and photodegradation performance of dendrite-like ZnO/Ag nanostructures. Dendrite-like ZnO/Ag nanocrystals were prepared by a facile solution base technique. They reported that “crystalline Ag nanowires were first synthesized by the polyol process, then highly dense ZnO nanorods with diameters of about 50 - 400 nm were vertically grown on the lateral surface of the Ag nanowires, by a simple aqueous solution route, with a uniform growth along the (0001) direction” [147]. Afterward very thin zinc oxide nanowires with a radii < 15 nm were synthesized on top of the ZnO nanorods. The ZnO/Ag NRs exhibited a superior photocatalytic performance when compared to undoped ZnO nanorods, and the ZnO/Ag with ~ 8% Ag revealed the highest photocatalytic activity. In a similar decontamination of MB, zinc nanowires, grown by the hydrothermal method, were found to be more effective (12-24%) compared to nanofilms due to numerous point defects from the oxygen vacancies. In the same work, Baruah et al. [78] reported a 7% increase in photocatalytic activity, under visible irradiation after 3hr, using a hydrothermal method compared to other conventional techniques.

Guo et al. [160] prepared “ZnO and TiO<sub>2</sub> 1D nanostructures (nanorods and nanotubes) by low-cost, low-temperature, solution-based methods and their properties and photocatalytic performance were studied, after 90 min, it was reported that faster MO degradation under simulated solar illumination was observed for ZnO NRs (51%) , while under UV illumination faster degradation was observed for TiO<sub>2</sub> (57%)”. The absorption spectra and the surface defect on the zinc oxide nanowires accounted for the huge variation in photocatalytic performance when compared to titanium under different light irradiation in UV and visible range.

Sun et al [161] prepared a well –arranged monocrystal zinc oxide nanobelt arrays on a silicon wafer by a carbothermal reduction route with the assistance of a SnO<sub>2</sub>/Sn species. The as-prepared ZnO nanobelts decomposed > 94% of MO in a solution after 5h of UV irradiation.

Hamedani et al. [162] successfully prepared zinc oxide nanorods via a hydrothermal technique. Congo red was employed to study the catalyst performance for the photodegradation of contaminants. For example, under UV light irradiation (30W), the photodegradation of Congo red was reported to be 90% in about 2.5 h.

Mohan et al [163] investigated the photodegradation performance of zinc oxide NWs with different diameters within 30-300 nm, under UV light irradiation (80 W/cm<sup>2</sup>), for the decomposition of Resazurin dye (RZ) in the aqueous solution. The zinc oxide nanorods were fabricated by a mixture of carbon powder and zinc oxide particles in a horizontal tube furnace via a vapor pressure technique. The addition of the carbon powder considerably reduced the decomposition temperature of the catalyst. The mixture was placed in a 100 cm long quartz tube, bubbled with high purity argon stream from one side with the other end of the quartz joined to a water bubbler. At 900°C, oxygen gas flowing at 25 sccm was introduced for 0.5 h, and then allow to cool to room temperature. The nanowires were collected 60 cm away from the source.

The degradation efficiency of RZ for 30 nm and 300 nm nanowires were 75% and 18%, respectively, under a 40 min UV exposure time. It was revealed that the 30 nm diameter ZnO NW showed the highest photocatalytic activity. The results also revealed that as the intensity of the RZ peak ( $\lambda = 604$  nm) decreased, concurrently, a new peak (575 nm) was observed which corresponds to the formation of Resarufin (RF). Hence, the photocatalytic reaction involves 2 steps: photo reduction (RZ into RF) and photo degradation (RZ and RF).

Furthermore, ZnO nanofibers were used to remediate dye molecules such as acid fuchsin and amido black 10B. Zinc oxide nanofibers were fabricated via electrospinning a precursor solution of zinc acetate (ZnAc)/cellulose acetate (CA) mixed in the solvent *N, N*-dimethylmethanamide (DMF)/acetone. After photocatalytic activity for 0.5 h, under UV irradiation, 95% of the acid fuchsin was decomposed and decolorized. In the same time interval, 85% of the amido black 10B was degraded, with the color changing from dark to light blue. It was also reported that in 0.3 h the decomposition efficiency of acid fuchsin was 73% and 85% by zinc oxide nanoparticles and nanofibers, respectively, signifying that the photocatalytic performance of the ZnO nanofibers was superior to zinc oxide nanoparticles.

Although a well – arranged less than 10-nm monocrystal zinc oxide nanobelt arrays were obtained by Sun et al [161] prepared on a silicon wafer via a carbothermal reduction route, little has been documented on the fabrication of well-aligned zinc oxide nanowires with radii of less than 20 nm. Therefore, one of the fabrication challenges of nanowire materials is to reduce the nanowire diameter and, at the same time, align the nanowires in a controlled fashion. The solution to this challenge is proposed in this work.

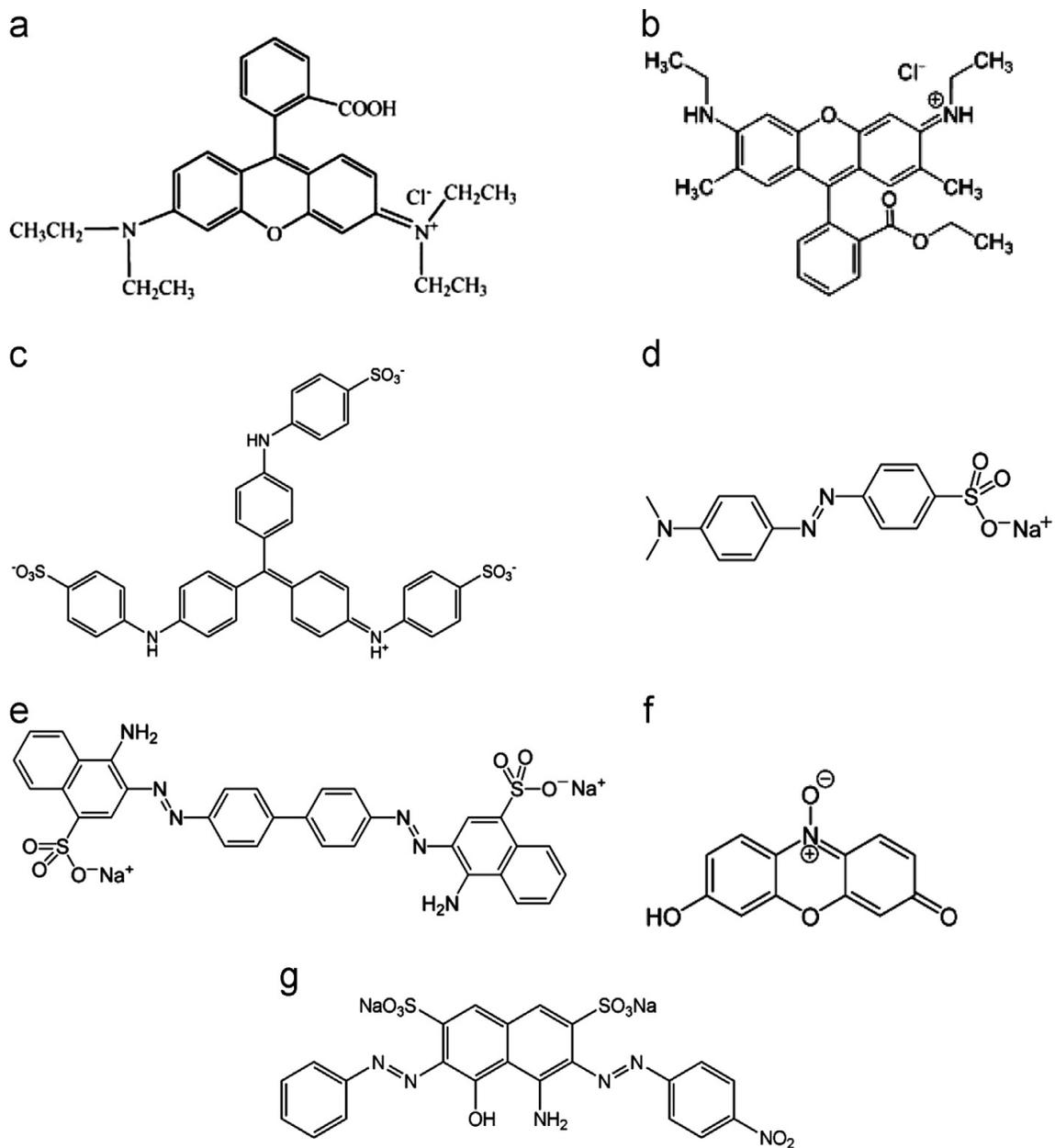


Figure 10 Structures of selected dyes. (a) Rhodamine B(RhB), (b) Rhodamine 6G (Rh6G), (c) Methyl blue (MB), (d) Methyl orange (MO), (e) Congo red (CR), (f) Resazurin (RZ) and (g) Amido black (AB)

Table 3 Selected list of common wastewater dyes /organic matter degraded using one-dimensional (1D) ZnO nanostructures [87], [159, 160], [167-172]

Compound	Formula	Photocatalyst	Light source	% Degradation (Duration)	ef.
RhB	$C_{28}H_{31}ClN_2O_3$	ZnO/ TAPPI-CoTPPS	Visible $\lambda \geq 420nm$	98 (1hr)	58
		ZnO nanofibrous mats	Visible (500w)	60 (2hr)	59
RhB 6G	$C_{28}H_{31}N_2O_3Cl$	Silver-coated ZnONW	UV	80 (14 min)	50
		photocatalytic paper with ZnO nanorods	visible (963w/m <sup>2</sup> )	>95 (2 hr)	51
Methyl blue	$C_{16}H_{18}N_3Scl$	ZnO NR/Ag 8% atom		>75(5.5 hr)	60
		ZnO nanorods	visible	98 (3hr)	8
Methyl Orange	$C_{14}H_{14}N_3NaO_3S$	photocatalytic paper with ZnO nanorods	white light (963w/m <sup>2</sup> )	>35 (2hr)	51
		ZnO NRs	UV	51 (90 min)	60
Congo Red	$C_{32}H_{22}N_6Na_2O_6S_2$	ZnO nanobelts	UV	94 (5hr)	61
		ZnO nanorods	UV (30W)	90 (160 min)	62
Resazurin	$C_{12}H_7NO_4$	ZnO NW	UV (80/cm <sup>2</sup> )	75 (40 min)	63
Amido black 10B	$C_{22}H_{14}N_6Na_2O_9S_2$	ZnO nanofiber (23nm)	Visible (500W)	85 (30 min)	58

ZnO/ TAPPI-CoTPPS = ZnO microrods and nanoheteroaggregates containing tetrakis (4-trimethylaminophenyl) porphyrin (TAPPI) and tetrakis (4-sulfonatophenyl) porphyrin cobalt (II) (COTPPS)

## 1.7 Conclusions

Although titanium has been thoroughly investigated as an effective photocatalyst, zinc oxide has been considered an appropriate substitute since it is less expensive and possesses a similar band gap (~ 3.3eV). Compared to TiO<sub>2</sub>, ZnO has been reported to produce better degradation due to the higher efficiency of photoexcitation under visible light for

decontamination of water. Furthermore, ZnO is considered a better candidate than TiO<sub>2</sub> due to its higher activity because of the larger number of surface defects, oxygen vacancies and the facile preparation of well-aligned crystalline nanowires, all of which significantly enhance the photocatalysis process. To further improve the photoactivity, there is a need to increase the photocatalyst surface area, for optimal mass transfer and efficient dye degradation, without additional equipment cost in catalyst separation from water. To this end, one-dimensional (1D) ZnO nanostructures such as rods, wires, and tubes provide improved photocatalytic performance due to their higher aspect ratio (interactive surface). This paper highlighted the fabrication, properties and water treatment applications of 1D ZnO nanostructures; many methods can be employed in the preparation of ZnO NW-based photocatalysts. Nevertheless, the hydrothermal technique is widely used because the method is simple, scalable, and efficient. In addition, it facilitates the fabrication of quality nanoscale crystalline ZnO-based photocatalysts. Evidently, ZnO has proven to be a potent tool for water purification, via photocatalysis, as well as other environmental applications, this obviously provides the motivation for advances in the fabrication of high quality ZnO nanowires (nanorods).

## CHAPTER 2: TiO<sub>2</sub> PHOTOCATALYST FOR GREEN SPACE EXPLORATION

### 2.1 Introduction

Work is underway at NASA Glenn Research Center (GRC) and numerous other research laboratories to develop technologies based upon heterogeneous photocatalysis to decompose organics and/or decontaminate wastewaters [1-3, 41, 44, 173, 174]. The presence of these contaminants in water could pose potential health and environmental problems in a controlled environment such as on a space station or during long-term manned missions. There are also significant terrestrial concerns about chemicals, such as azo dyes and pesticides that are discharged to the environment; many of these are toxic, carcinogenic, mutagenic, and/or resistant to biodegradation [4, 7, 175-178]. Additionally, conventional wastewater treatment techniques are usually ineffective in the decontamination of these compounds. Thus the development of energy efficient and “green” technologies to reduce or eliminate organic wastes has important potential dual-use applications.

To this end, semiconductors like titanium oxide (TiO<sub>2</sub>), zinc oxide (ZnO) and other transition metal compounds (mostly oxides) are being studied for their photocatalytic properties to decompose a number of contaminants and organic compounds into harmless inorganic such as CO<sub>2</sub> and H<sub>2</sub>O [41, 44]. The basic principles concerning these catalysts are well understood; when a light source of sufficient energy illuminates a photocatalyst, electron/hole (e<sup>-</sup>/h<sup>+</sup>) pairs will be formed as electrons absorb the energy from the irradiated photon, the electron tunnel from the VB to the CB, leaving the positive charged holes in the VB (see fig 3). Hence, the produced pair initiates series of photochemical reactions that lead to the decomposition of contaminants

adsorbed on the surface of the catalyst in aqueous solution. Transition metals serve as co-catalysts by trapping free electrons and prevent the electron/hole pair-recombination process resulting in higher photocatalytic performance. Titanium ( $\text{TiO}_2$ ) is the most commonly used photocatalyst due to its excellent optical properties and ability to facilitate very rapid light-induced reactions.  $\text{TiO}_2$  exists in three phases: rutile and anatase (most commonly) and brookite. Compared to most catalysts, titanium dioxide is quite inexpensive, chemically very stable, and readily available.

In this study, Rhodamine B (RhB) an organic dye (see Figure 11), a model compound for organic waste, was decomposed by  $\text{TiO}_2$  photocatalysts with various transition metals added as co-catalysts by traditional catalyst processing methods, and were characterized by Brunauer, Emmett and Teller analysis (BET), X-ray diffraction (XRD) and scanning electron microscopy (SEM).

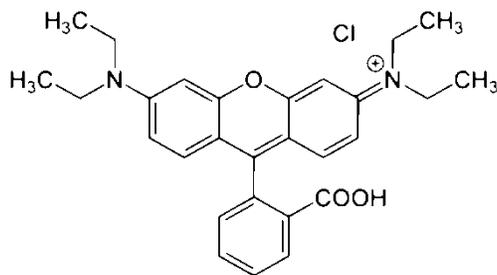


Figure 11 Molecular structure of rhodamine B

This research intends to probe  $\text{TiO}_2$  photocatalytic activity by enhancing its efficacy with different transition metal co-catalysts such as: copper (Cu), palladium (Pd), platinum (Pt), silver (Ag), gold (Au), and ruthenium (Ru). To achieve this purpose, different metal-co-catalyst-titanium photocatalysts were synthesized on either anatase or a 4:1 mixture of anatase and rutile

(P25), one of the better reference photocatalysts. All photocatalysts were tested in a broadband photoreactor to determine their effectiveness in dye degradation.

RhB is a common dye often used as a tracer in water to study flow rate and direction (Figure 11). It is reddish violet, highly soluble in water, and dangerous if swallowed. The maximum absorbance ( $\lambda_{\text{max}}$ ) of RhB is around 550-555 nm [179] The color of this family of dyes results from conjugated chains or rings that absorb light at visible wavelength [176].

## 2.2 Materials and Methods

All chemicals were of high purity (> 99%) and used as received. To process the promoter-loaded photocatalysts, a Büchi Rotavapor 210 with a Vacuum Pump (V-700) was used, see Fig. 2 below. Experimental and instrumentation details not given below are described in a recent report from the group at NASA Glenn Research Center [180].

The following promoters or co-catalyst precursors were used: tetraamine platinum (II) nitrate ( $\text{Pt}(\text{NH}_3)_4(\text{NO}_3)_2$ ), ruthenium (III) nitrosyl nitrate ( $\text{RuNO}(\text{NO}_3)_3$ ), palladium (II) chloride ( $\text{PdCl}_2$ ), and sodium tetrachloroaurate (III) dihydrate 99.99% ( $\text{NaAuCl}_4 \cdot 2\text{H}_2\text{O}$ ); all were packaged under argon and obtained from Alfa Aesar of Ward Hill, MA. Silver nitrate ( $\text{Ag}(\text{NO}_3)_3$ ) and RhB (packaged under argon ) were obtained from Acros Organics, Morris Plains, NJ and cupric nitrate ( $\text{Cu}(\text{NO}_3)_2$ ) was obtained from Fisher Scientific of Pittsburgh, PA. A  $8.0 \times 10^{-6}$  M RhB solution was prepared from a stock solution containing 0.447 g of RhB dissolved into 100 ml of deionized water. The stock and the diluted solutions had very dark reddish-purple and pink colors, respectively.

### **2.3 Preparation of Transition Metal-Promoted TiO<sub>2</sub> Photocatalysts**

Either 1% or 5% of the metal complex was dissolved in 20 ml of water. The only exception was the catalyst using 1% Pd. In the latter case, a few drops of HCl were added to the solution and stirred overnight to completely dissolve the palladium complex (H<sub>2</sub>PdCl<sub>4</sub>). The solution (metal complex + water) was added dropwise to 10 g of TiO<sub>2</sub>, either anatase or Degussa P25. Then, it was dried in a rotary evaporator (rotovap) at 200 torr in an 80°C water bath (Fig. 2). Occasionally, the photocatalyst was scraped off the walls with a spatula and the flask was placed back on the rotovap. When the powder was dry, it was stored in an oven until calcinations were performed. Prior to calcining, the photocatalysts were ground with an alumina mortar and pestle. All the catalysts were calcined using a Thermolyne 21100 Tube Furnace at 400°C for 2 hours under a flow of dry air. Calcining removes the volatile substances in the photocatalyst, typically nitrate released as nitric oxide (NO) or chloride released as HCl or Cl<sub>2</sub>. Air is allowed to flow through the tube at about 5 ml/min to ensure that the catalyst does not decompose. After that, photocatalysts were characterized and screened for decomposition of RhB in a broadband photoreactor (Ace Glass).

### **2.4 Promoted TiO<sub>2</sub> Photocatalytic Studies**

Photocatalytic experiments were carried out with 10 mg of catalyst added to 10 ml of an 8.0 x 10<sup>-6</sup> molar RhB solution in a quartz photoreactor. The solution was irradiated with broadband light in air and nitrogen from pressurized cylinder tanks through a bubbler. The gas flow maintained the suspended photocatalyst in a motion while providing a good stir to the solution. Aliquots from the reactor (1.5 ml) were taken using a Pasteur pipette at pre-determined time intervals for up to one hour and centrifuged. The concentration of RhB was measured by a

Perkin Elmer Lambda 950 UV/Vis spectrophotometer; UV/Vis spectra were recorded to monitor dye decomposition.



Figure 12 (a) Bench scale reactor system (b) Dried and calcinated photocatalysts

## 2.5 Results and Discussion

Native or metal co-promoted (enhanced) titanium ( $\text{TiO}_2$ ) photocatalyst powders were subsequently characterized by traditional methods and then screened for organic matter decomposition efficacy as discussed below. Exploiting this technology for space missions would entail design, testing and construction of a light-driven system that utilizes photocatalysis, as briefly described in the following section.

## 2.6 Characterization of Photocatalyst Samples

Analyses of promoted-titanium photocatalysts were performed by X-ray diffraction (XRD), scanning electron microscopy (SEM), BET and energy dispersive spectroscopy (EDS) instruments. The BET analysis (Table 4) determined that the photocatalysts with the largest surface areas were anatase- $\text{TiO}_2/\text{Ru}$  1% and anatase- $\text{TiO}_2/\text{Pt}$  1%; while that with the smallest surface area was anatase- $\text{TiO}_2/\text{Ag}$  5%, although all samples differed by at most  $2 \text{ m}^2/\text{g}$ . The surface area of our native anatase  $\text{TiO}_2$  was  $10 \text{ m}^2/\text{g}$ ; this is much lower than the surface area of unmodified P25  $\text{TiO}_2$  ( $\sim 50 \text{ m}^2/\text{g}$ ). It was anticipated that for the lower percent metal containing

samples, the specific surface area would be higher because the metal promoter would not occupy as many surface sites. EDS analysis confirmed the presence of metal promoters on the surface of titania photocatalysts. The analysis for the promoter shows a weight percent range of 1.11% - 2.48% for the photocatalysts with a target value of 1% loading. In the case of the desired 5% promoter loading, the range was 3.78 - 8.68 %. Each catalyst had the same promoter wt% calculated and added but the EDS analysis showed that samples often either exceeded or were under their desired loadings as a result of processing variability. A typical XRD powder pattern is shown in Fig. 3 for a 1% Ru-promoted anatase sample.

Table 4 EDS and BET analysis for metal-doped titanium photocatalysts

Sample	% wt. Ti	% wt. O	% wt. Promoter	% Degradation after 60 min	Surface area (m <sup>2</sup> /g)
Anatase TiO <sub>2</sub> /Ag 1%	47.00	51.90	1.11(Ag)	66	8.38
Anatase TiO <sub>2</sub> /Pd 1%	47.24	51.36	1.40 (Pd)	74	8.75
Anatase TiO <sub>2</sub> /Pt 1%	48.74	48.84	2.24 (Pt)	72	9.49
P25 TiO <sub>2</sub> /Cu 5%	42.51	48.80	8.68 (Cu)	40	8.35
Anatase TiO <sub>2</sub> /Cu 5%	48.10	45.59	6.31(Cu)	28	8.35
Anatase TiO <sub>2</sub> /Ag 5%	46.84	49.38	4.94(Ag)	76	7.52
Anatase TiO <sub>2</sub> /Ru 1%	51.85	46.20	1.95 (Ru)	85	9.26

NB: The weight percentage of each element in each sample is the average of three EDS runs

Morphological analysis of the photocatalysts was accomplished by SEM (Fig. 4). Photocatalyst surfaces look rough with small particles that are not evenly distributed. The particles of the photocatalysts have different shapes and also various sizes (25-100 μm in diameter). XRD

analysis confirmed that the synthesized photocatalysts are polycrystalline (Fig. 3). As shown in Table 4, the % degradation of RhB after 60 min. was in excess of 70% for anatase-TiO<sub>2</sub>/Ag 5%; the anatase-TiO<sub>2</sub>/Ru 1%, showed the highest efficiency (85%), with the lowest being the P25 TiO<sub>2</sub>/Cu 5% (40%). A higher specific surface area typically corresponds to higher catalytic activity as observed for anatase TiO<sub>2</sub>/Ru 1% [173] [174].

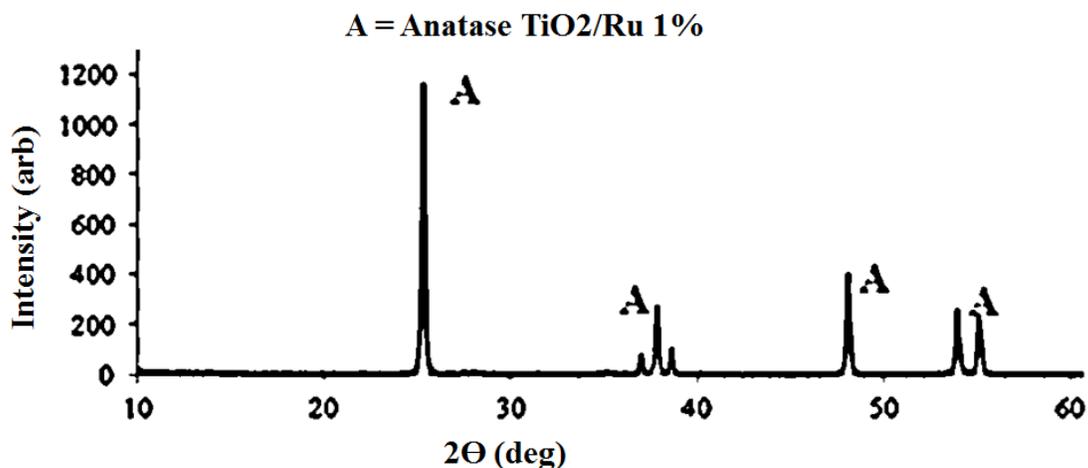


Figure 13 X-ray diffraction powder pattern of the anatase/1% ruthenium sample

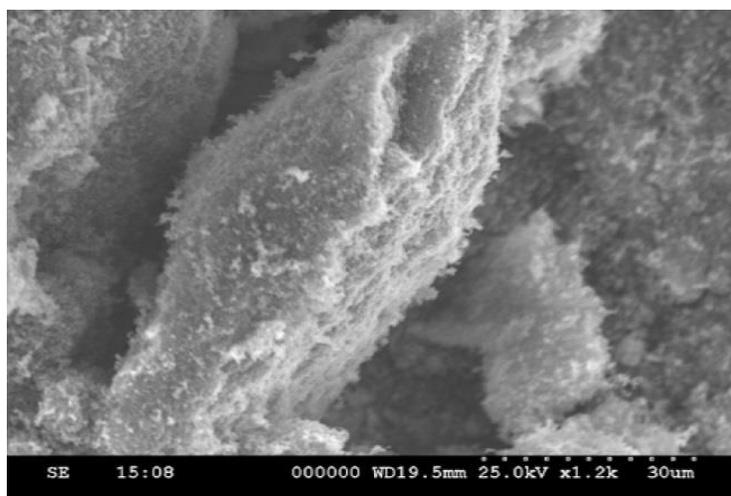


Figure 14 SEM image of anatase TiO<sub>2</sub>/Ru 1% photocatalyst

Table 5 X-ray photoelectron spectroscopy data from metal co-promoted TiO<sub>2</sub> samples

Metal (Level)	TiO <sub>2</sub> Phase(s)	Metal Peak(s)	TiO <sub>2</sub> Peaks	Assignment(s)	Reference
Silver (2.0 %)	Anatase	367.6; 373.5	458.1; 464.1	Ag <sub>2</sub> O (1.5) <sup>a</sup>	[181]
Silver (3.3 %)	Anatase	367.6; 373.6	458.2; 464.1	Ag <sub>2</sub> O (1.6) <sup>a</sup>	[182]
Copper (5.0 %)	Anatase	932.6; 934.3	458.2; 464.1	Cu <sub>2</sub> O and CuO <sup>c</sup>	[183]
Copper (3.6 %)	P25 <sup>b</sup>	932.4; 934.1	458.2; 464.1	Cu <sub>2</sub> O <sup>c</sup> and CuO	[183]
Palladium (0.8 %)	Anatase	336.1; 341.3	457.9; 463.7	PdO	[184]
Platinum (1.1 %)	Anatase	70.9 (sh); 71.8; 73.9; 75.4	458.0; 464.2	Pt <sup>0</sup> and PtO <sup>c</sup>	[184]
Ruthenium (~1 %)	Anatase	283; 287 <sup>d</sup>	458.2; 464.0	Ru <sup>0</sup> and RuO <sub>2</sub> <sup>c</sup>	[185]
Ruthenium	P25 <sup>b</sup>	281; 285 <sup>d</sup>	458.3; 464.2	Ru <sup>0c</sup> and RuO <sub>2</sub>	[185]

<sup>a</sup>FWHM = 1.75 eV (AgO); 1.50 eV (Ag<sub>2</sub>O); 1.15 eV (Ag). <sup>b</sup>P25 = Mixed phase Anatase/Rutile. <sup>c</sup>Majority Phase. <sup>d</sup>Ru XPS peaks obscured by carbon, observed as shoulders.

### 2.6.1 XPS Studies

The XPS spectrum for Ag gives binding energies for Ag of 367.6 eV (3d<sub>5/2</sub>) and 373.5 eV (3d<sub>3/2</sub>). These values indicate that Ag is present on the TiO<sub>2</sub> surface as Ag<sub>2</sub>O, in the monovalent state. The XPS spectrum of Ti shows two peaks located at 464.1 eV (2p<sub>1/2</sub>) and another one located at 458.1 eV (2p<sub>3/2</sub>). The splitting of ~ 6 eV indicates a normal state of Ti<sup>4+</sup> in the as-prepared mesoporous anatase TiO<sub>2</sub>. Data from Cu/TiO<sub>2</sub> XPS shows two kinds of copper species on the surface of the sample. Binding energy of 932.1 eV is characteristic for Cu<sub>2</sub>O, while higher binding energy of 933.68 eV is characteristic for CuO. It is supposed that coexistence of Cu<sup>2+</sup> and Cu<sup>+</sup> can improve the photocatalytic efficiency by fitting results of O 1s and Cu 2p<sub>3/2</sub> XPS of the catalysts with different dopant concentration. XPS data for Pd/TiO<sub>2</sub> reveals the doped catalyst by sol-gel technique depicts a significant (double) impact on the palladium 3d from the electron binding energy of 334–346 eV. By the same method of fabrication, the value of 336.2 eV can be attributed to electron binding energy of palladium (II) oxide (PdO) while the energy of

335.3 eV corresponds to  $\text{Pd}_x\text{O}$ . In addition, the electron binding values of the oxide of palladium is slightly higher than Pd  $3d_{5/2}$  at 337.5 eV. Based on the experimental data, it is proposed that the energy of 337.5 eV may have resulted from the diffusion of  $\text{O}_2$  atom into the subsurface lattice of the palladium (II) oxide. For the impregnation catalyst, the binding energy of Pd  $3d_{5/2}$  at 337.5 eV is slightly lower than that of  $\text{PdO}_2$ . After the reduction reaction, the palladium compounds are converted to metallic Pd which is usually characterized by electron binding energy of 334.7 eV, this will be demonstrated in more detail in future publication.

The chemical state and surface chemistry of platinum was also investigated. Typically, platinum can exist in 3 states: platinum (0), platinum (II) and platinum (IV). Platinum 4f is usually characterized by two major signals within the range of 71.1 eV - 72.3 eV and 72.3 – 75.6 eV which signals corresponds to metallic platinum (0) and oxidized platinum (II), respectively. The oxidation potential of palladium such as from Pd (0) to Pd (II) helps to improve photocatalytic performance. The oxidation state of Pt often plays an important role on the enhancement of photocatalytic activity. However, research has reported that Pt (II) shows less photocatalytic activity to Pt (0) in the degradation of 4-chlorophenol and chloroform.

XPS obtained of Ru/ $\text{TiO}_2$  catalyst are presented for both anatase and P25 substrates. Ru exist in more reduced state with electron binding energy of  $\sim 281$  eV (Ru(0)) and minor phase  $\text{RuO}_2$  on P25, similar to Cu (above). The signal within the range from 279.0 to 283.0 eV is poor due to interference from carbon. These developments can be best clarified by assuming that metallic Ru (denoted as Ru(0) or  $\text{Ru}^0$ ) has occurred due to treatment at elevated temperature, with the higher surface area P25. The contribution of the oxidized  $\text{RuO}_2$  ( $\sim 283$  eV) is more pronounced on anatase.

Summary of the XPS data are illustrated in table 5. Surface area measurements of all the photo catalysts are shown in Appendix C. Topographical images taken by SEM and EDS results, as well as XRD analysis are also illustrated.

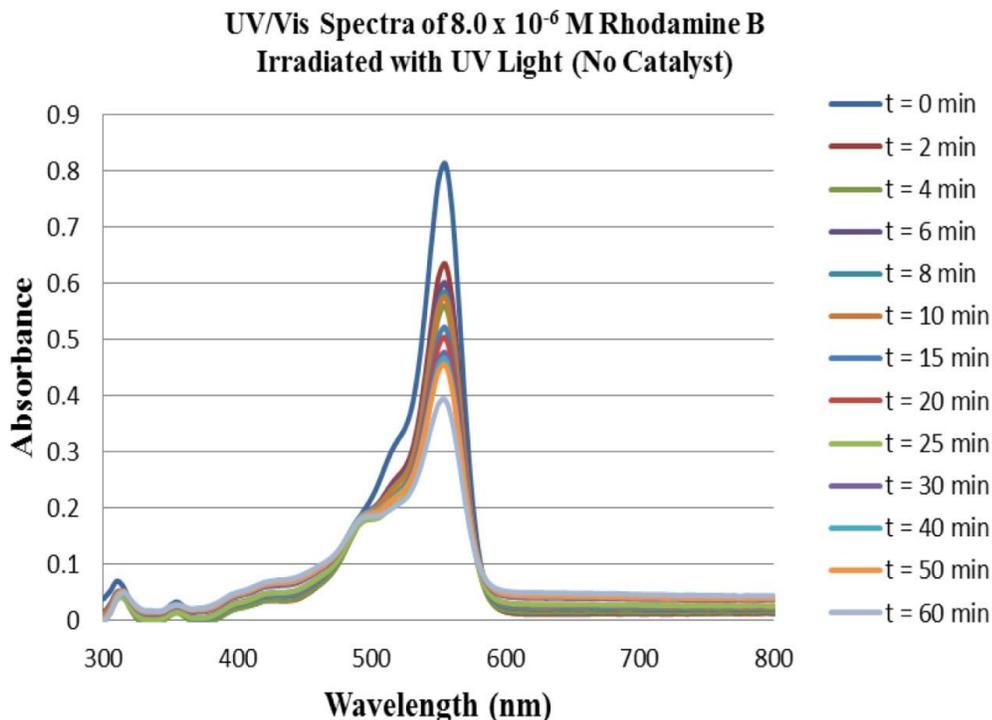


Figure 15 UV-Vis spectra of RhB irradiated without a catalyst for 60 min

## 2.7 Photocatalytic Results

Figure 15 shows a typical absorbance vs. wavelength relationship for the UV/Vis spectra of  $8.0 \times 10^{-6}$  M RhB irradiated with UV light in the absence of a catalyst. The initial (0 min) and final (60 min) absorbance values were 0.82 and 0.39, respectively. Figure 6 illustrates the degradation of a RhB solution in air, in the absence and the presence of a catalyst, and saturated with nitrogen gas with the catalyst present. The highest and lowest efficiency of degradation of RhB was found in a reaction with anatase-TiO<sub>2</sub>/Ru 1% (under aerobic conditions) and anatase-TiO<sub>2</sub>/Ru 1% (under nitrogen saturated conditions), respectively. RhB can react even in the

absence of a catalyst under UV light as shown by the red line in Fig. 6, however, the presence of anatase TiO<sub>2</sub>/Ru 1% accelerates this photoreaction significantly.

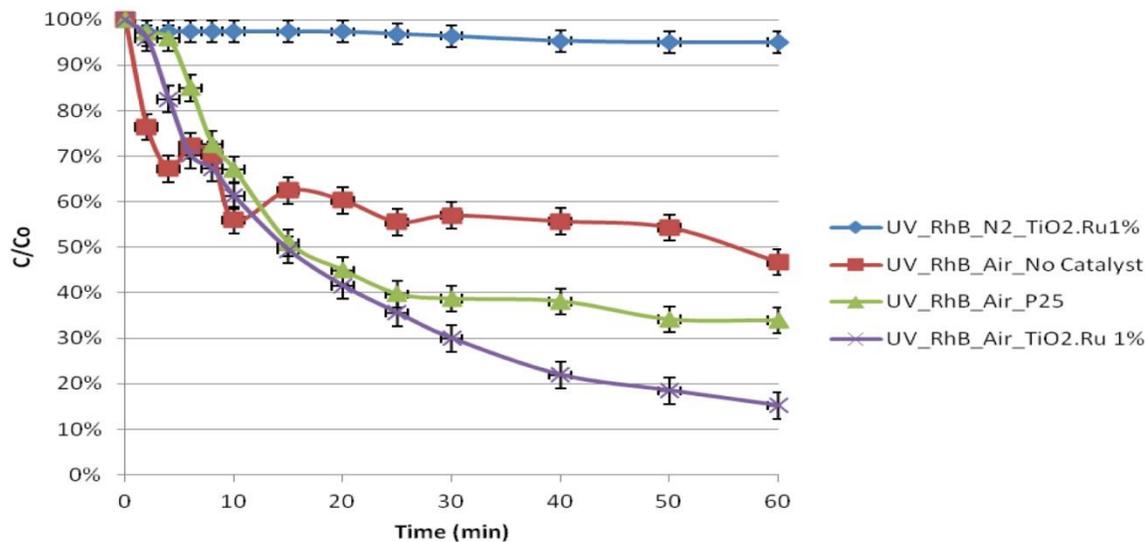


Figure 16 UV-Vis spectra of photocatalytic studies of a metal doped titanium catalyst

## 2.8 Mechanism of Photocatalysis

There have been a number of investigations to evaluate photocatalytic performance under both N<sub>2</sub> and O<sub>2</sub> rich environments. Ali et al. [65] investigated photocatalyzed oxidation of methyl blue using ZnO thin films and suggested that the reaction occurs mostly by a Mars Van Krevlen-method (i.e. “lattice oxygen atoms are used for oxidation, causing degradation of the ZnO lattice over time”) [65]. This analysis proposes that providing O<sub>2</sub> saturated conditions either minimizes or inhibits lattice oxygen from participating in the photocatalyzed oxidation reaction, or replacement of the lattice oxygen atoms are removed during this reaction. It is hypothesized that oxygen atoms are removed from the photocatalyst lattice and utilized in the radical initiation and propagation phase of the follow-on reactions type.

Photocorrosion of photocatalysts was reported, as the reaction progresses under  $O_2$  limited conditions, because there is only a partial  $O_2$  supply to replace the lattice oxygen atoms employed [16]. Consequently, under oxygen-rich conditions, the catalyst degradation is reduced because of the regeneration of the lattice oxygen atoms and maintenance of the physical structure. The Mars Van Krevlen-type mechanism has also been reported for  $TiO_2$  and other (doped) ZnO-containing catalysts. For example, Hurum [186] have shown that lattice oxygen atoms are extracted from mixed-phase  $TiO_2$  (Degussa P25) during the photocatalytic decomposition.

In a related study of the photodegradation of RhB, under ultraviolet and visible light irradiation [187] by Lee et al. [188], a new family of  $BiO(Cl_xBr_{1-x})$  ( $x=0, 0.1, 0.2, 0.5, 0.7, 1$ ) was synthesized by hydrothermal processing. The Bi-based photoactive material with  $x = 0.5$  exhibited a 74.2% degradation efficiency in 60 min, about 10% less compared to anatase- $TiO_2$ /Ru 1% (Table 5).

Zhong et al. [187] carried out the photocatalytic degradation of RhB using  $TiO_2$  supported on activated carbon ( $TiO_2$ -AC) under microwave irradiation. The decomposition of RhB in microwave-enhanced photocatalysis (MPC) 30 mg/L was 96% after 20 min. The reaction rate constant of RhB, a pseudo first-order reaction, using this photocatalyst material was 4.16 times greater than that using Degussa P25.

Houšková et al. [189]” investigated the photocatalytic activity of Ru-doped titanium in the gas phase by the decomposition of acetone during irradiation at both 365 and 400 nm”. To study the BG effect of the fabricated Ru-doped  $TiO_2$  samples, UV-Vis spectroscopy was used. “They established that the intensity of the absorbance in the visible region increases with the

concentration of doped Ru ions; a value of 3.20 eV is reported in the literature for pure anatase “ [77].

Reaction kinetics provides information about the reaction pathways and the rate of conversion from reactants to products. Kinetics is estimated by both the catalyst and the substrate concentrations. A recent study confirms the use of pseudo-first order kinetics to describe the photocatalytic degradation of RhB with a rate expression of  $-dC/dt = k_{obs}C$  [190]. Specific rate constants and correlation to factors such as (photo) catalyst loading, co-promoter and reaction conditions are currently being analyzed and will be reported in a future publication.

## **2.9 Integration of Photocatalysis into Space Missions**

Of particular interest for space missions is the potential applicability of photocatalysis for the decomposition of organics in order to mitigate potential health and environmental problems in the controlled environment of a spacecraft or space station, particularly for long-term manned missions. One resource common to all manned missions in the immediate future is an abundance of sunlight, which presents an opportunity to use concentrated sunlight, through the use of solar concentrators [191], to possibly enhance or augment photocatalytic process(es). Other methods may also be considered for more distant long-term missions.

The most likely scenario for a photocatalytic reactor could include a modest enhancement in the solar intensity brought about by a trough-style reactor, with reactants and catalyst flowing along the axis of the trough and therefore being illuminated for a controlled duration based on flow rate. A rigid concentrator providing a 2000:1 concentration ratio increases the intensity substantially with concurrent undesirable increases in temperature (and potential recombination of electrons and holes). A less stringent concentrator is likely to be far more desirable, one

providing a modest concentration ratio, perhaps a factor of 10:1, akin to flexible Fresnel concentrators developed in the 1990s for photovoltaics [192].

Other concepts utilizing mass produced-composite strips, developed more recently as part of a Small Business Innovative Research effort funded by NASA GRC, may also be considered as they also provide a line focus which is conducive to illuminating a lengthy reactor tube over an extended period of time when utilizing a sun tracking system. More study is needed to better understand the requirements of the receiving tube that would be located along the line focus, including such parameters as transparency, diameter and length. With the degradation reaction occurring in tens of minutes, a modest flow rate on the order of a liter per minute, and a reasonable diameter tubing machined to ensure mixing, one could envision a trough system on the order of a few meters in length to process a few liters of fluid over a few hours, suggesting a reasonable trough size. Identifying mechanisms and technologies for separating gases generated from photocatalytic reactions and recycling the catalyst, in a microgravity environment, also warrant further study.

Another scenario for a photocatalytic reactor could include illumination of the reactants and catalyst utilizing energy derived from fluorescent lamps or light emitting diodes [193]. Of course, such a scenario would need abundant electrical power for the lamps or diodes. Missions in the distant future, to locations beyond Mars where sunlight is far less abundant, could be powered via nuclear reactors, and such fluorescent lamp or light emitting diode concepts could be facilitated by greater available power.

## CHAPTER 3: ZnO NANOWIRES PHOTOCATALYST

### 3.1 Introduction

In our industrial society, excessive amounts of organic waste ( $>100$  kg *per capita*), including dyes, are discharged into wastewater and effluents causing significant environmental problems. Photodegradation of these contaminants via photocatalysis has become a very active research topic in the past several decades [38, 39, 85, 89, 194, 195] A growing list of semiconductor photocatalysts including  $\text{WO}_3$ ,  $\text{Bi}_2\text{O}_3$ , ZnS, titanium dioxide ( $\text{TiO}_2$ ) and zinc oxide (ZnO) have been employed for the remediation of organic pollutants and deactivation of numerous microorganisms due to their photocatalytic properties [42, 43, 196] ; among these,  $\text{TiO}_2$  and ZnO are the most often studied materials.

Although, compared to other photocatalysts,  $\text{TiO}_2$  has been the most widely investigated photocatalyst by researchers for air and water purification, ZnO is a promising substitute primarily due to its similar band gap ( $\sim 3.3$  eV) [60], and quite low toxicity relative to the benchmark photocatalyst,  $\text{TiO}_2$ . Moreover, further advantages of ZnO as a photocatalyst over  $\text{TiO}_2$ , includes lower cost of production, abundance in nature, chemically-stable crystal structure and potential superior photoactivity during visible light irradiation [10, 63, 78] photocatalytic purification. The issue of ZnO photostability can be resolved by adjusting the water pH prior

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<sup>2</sup>Portions of this chapter was published in Thin Solid Films (I. Udom, Zhang Y., Ram, M. K., Stefanakos, E. K., Hepp, A. F., Elzein, R., Schlaf, R., Goswami, D. Y., A simple photolytic reactor employing Ag-doped ZnO nanowires for water purification, Thin Solid Films, (2014)).

to photocatalytic decontamination. The higher photocatalytic efficiency of zinc oxide over titanium is due to higher production efficiency of electrons and prevention of electron-hole recombination, for example in the decomposition of phenol and 2-phenylphenol, [80, 82, 83]. Due to ZnO showing good number of electron trapping sites at emission close to 500 nm, Kuo et al. [197] applied a ZnO photocatalyst via a vapor transport grown technique to effectively decompose rhodamine B and 4-hydroxychlorobenzene under sunlight irradiation.

Thus, modification of ZnO photocatalyst morphology is one approach to enhancing the photocatalytic performance and potential practical applicability of the catalyst particularly in the longer-wavelength portion of the solar spectrum. To this end, there has been significant effort in increasing the aspect ratio (among several ZnO nanostructures, i.e. ZnO nanowires (NWs)) to increase the efficiency of photoreaction because molecules are adsorbed on the (relatively) larger surface (area) of the catalyst, and are eventually broken down to simpler and benign products [66, 198]. Additionally, due to its photostability and re-usability, ZnO nanowire arrays grown on inert substrates eliminate the issues (separation or low efficiency) associated with employing other photocatalyst structures, such as nanoparticles, thin films, and bulk materials for water purification [199, 200]. Compared to other fabrication techniques such as chemical vapor deposition [201], physical vapor deposition [93], and vapor liquid-solid [202], hydrothermal processes are low temperature, simple, scalable, and catalyst-free. Moreover, ZnO NWs synthesized by hydrothermal methods typically possess oxygen vacancies in the ZnO crystal [66]. To further improve photocatalytic efficiency, ZnO photocatalysts can be further modified by addition of a dopant that functions as an electron trap by suppressing electron-hole recombination. A number of transition metals including Ni [81], Co [203], Ag [204], and Mn

[205] have been used as dopants. These dopants also help in lowering the activation energy (band gap) so that the electrons are effectively excited by lower energy photons.

Enhanced photocatalytic performance was observed with doped ZnO-Cr NWs over commercial TiO<sub>2</sub> (P25) in the photodegradation of methyl orange (MO) [206], whereas cobalt-doped ZnO (Co-ZnO) NWs showed enhanced deactivation of 1,2-dihydroxyanthraquinone relative to TiO<sub>2</sub> [207]. Further, Korake et al. [208] investigated the degradation of phosphamidon, an organophosphate insecticide, using doped Ag-ZnO nanorods under visible light. Compared to data available in the literature, we observed more efficient photocatalytic decomposition as determined by degradation over time. Although transition metal doping of ZnO nanowire by several metals has been studied via several processing and irradiation methods and reported in the literature, detailed investigation of photocatalytic performance of Ag-doped ZnO NWs prepared by hydrothermal techniques warrants further investigation.

There are a variety of photocatalytic reactor configurations that have been reported in the literature including: a flat-plate reactor [209], compound parabolic collector [210], packed-bed reactors [211, 212] and a shallow solar pond [213]. Several photocatalysts, including TiO<sub>2</sub> and ZnO, have been studied in both suspension and immobilized systems. Photocatalyst suspension in water provides larger surface area compared to an immobilized system. However, difficulty in separation and recovery of photocatalyst is a drawback in practical applications. Goswami et al. studied the design, construction and testing of a solar photocatalytic treatment facility for a commercial site with contaminated groundwater by using flat plate solar reactors. TiO<sub>2</sub> was used as the catalyst in suspended mode, and was settled down at the bottom of the tank overnight at the end of treatment [213]. The result showed the flat plate solar facility worked well in field tests. Nogueira and Jardim [214] investigated a photocatalytic reactor using immobilized TiO<sub>2</sub> on

a flat glass plate as a support and found that reactor performance was influenced by two factors: the fluid thickness film which flowed over the plate and the light intensity that reached the system. A thick film can result in mass and light transfer limitations. In this study, we report the design of a simple, efficient and scalable photocatalytic reactor and the fabrication of an anisotropic doped ZnO and Ag-ZnO nanowire via a conventional seeded hydrothermal technique on a borosilicate glass substrate. Both grown nanowires were tested for the photodegradation of MO, a model contaminant, in water. The results were compared with P25, a benchmark photocatalyst.

## **3.2 Experimental Procedure**

### **3.2.1 Synthesis of ZnO Nanowires**

All chemicals used in this experiment are of analytical grade and used without further purification. Heat-resistant borosilicate glass (area: 7x2 in, 1/8 mm thickness) and aluminum sheets were purchased from the McMaster-Carr Company.

In the preparation of growth solution and seeded ZnO seed particle, a mixture of equimolar ratio (25mM) of hexamethylenetetramine ( $C_6H_{12}N_4$ ) and zinc nitrate hexahydrate ( $Zn(NO_3)_2 \cdot 6H_2O$ ) were dissolved in water to form the growth solution. The preparation of a ZnO seed particle solution involves preparation of an aqueous solution of 5mM zinc acetate ( $Zn(CH_3COO)_2$ ) in ethanol.

In the fabrication of ZnO NWs, an aliquot of 0.5 ml seed particle solution was placed on the substrate (borosilicate glass or silicon wafer) and randomly tilted in different directions to ensure uniform distribution. The seeded substrate was dried in an oven at 100 °C for 10 min to remove moisture and another 30 min. at 350 °C to remove unreacted organic matter. After cooling, the substrate was placed in a reactor containing the growth solution, and stirred for 2

hours at 90 °C. After this step, the substrate was rinsed with water and oven dried at 100 °C for 10 min. and 350 °C for 30 min.

A seed solution of equimolar ratio (5 mM) of AgNO<sub>3</sub> and Zn(CH<sub>3</sub>COO)<sub>2</sub> in ethanol was prepared; a 1.25 ml aliquot of this solution was placed on a substrate. The rest of the growth process was completed similar to the ZnO NW growth. After several growth cycles, the mean weight of doped and undoped ZnO NW photocatalysts was determined as shown in Table 6.

### 3.2.2 Photocatalyst (P25) Coating

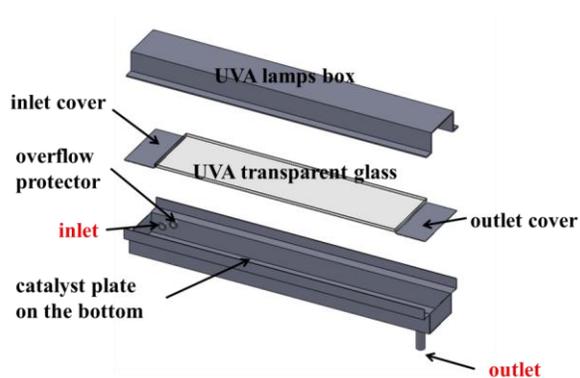
To compare the photoactivity of prepared ZnO NWs (doped and undoped) to P25, a commercial TiO<sub>2</sub> photocatalyst (Degussa P25) was immobilized on borosilicate glass plates by a spray coating method. The plates were cleaned by 190 proof (95%) ethanol prior to spraying. The same amount of nanowires, 100 mg of TiO<sub>2</sub> powder was suspended in 50 ml 95% ethanol to produce a TiO<sub>2</sub>-ethanol slurry. The slurry was stirred by a mini-vortexer for 5 min to enhance slurry uniformity. The suspension was evenly sprayed on the cleaned glass plates using a Paasche HAPK airbrush. After spraying, the glasses were maintained at room temperature for 1h and then dried in an oven at 80 °C for 30 min, 105 °C for 30 min, and 400 °C for 2 hours. The catalyst plates were tested in a commercial dishwasher to make sure that the catalyst adhered well to the plates. Due to some uncertainty about TiO<sub>2</sub> being sprayed outside the plate, the amount of TiO<sub>2</sub> sprayed on the plate (W) is calculated from:

$$W = \frac{V_s \times C_{TiO_2}}{A_s} \times A_p \quad (11)$$

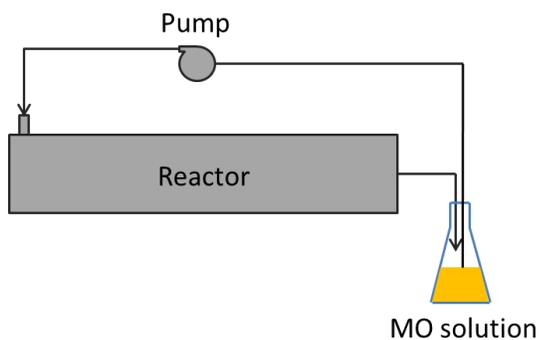
W is the total weight of TiO<sub>2</sub> sprayed on the plate, V<sub>s</sub> is the volume sprayed, C<sub>TiO<sub>2</sub></sub> is the concentration of the TiO<sub>2</sub>-ethanol solution, A<sub>s</sub> is the area of spray and A<sub>p</sub> is the area of the plate.

### 3.2.3 Photolytic Reactor Design and Fabrication

A photolytic reactor was designed and built “in-house” (see Fig. 17). The reactor consists of a water channel with a  $25.4 \times 50.8$  mm ( $1 \times 2$  in., H×W) cross-section and 380 mm (15 in.) length. A reflective aluminum sheet (0.559 mm thickness) is used to build the reactor channel. Water inlet is at a side-wall under the inlet cover and water outlet is at bottom wall under outlet cover which is shown in the Fig. 17a.



**a**



**b**

Figure 17 Scheme of: (a) photocatalytic reactor and (b) reactor system

The catalyst plates are  $50.8 \times 177.8$  mm borosilicate glass with photocatalyst coated on it. A UVA transparent glass ( $76.2 \times 304.8$  mm) and two reflective aluminum sheets ( $76.2 \times 38.1$  mm) are used as lid of the channel. A UVA lamp box is placed on the top as the light source. The

lamp box consists of two Southern New England Ultraviolet Company Rayonet RPR-3500 Å UVA lamps (304.8 mm long) and a reflective cover. The UV lamps were later replaced with a white light to emit radiation in the visible range in a wavelength range > 400 nm with an approximate Gaussian spectral distribution ( $\lambda_{\text{max}} = 350 \text{ nm}$ ). The spectral distribution shows the intensity of irradiation at different wavelengths. The reflective cover was made from a reflective aluminum sheet.

### 3.2.4 Evaluation of Photocatalytic Activity

The photocatalytic reactor (Fig. 17) was tested in the clean-up of 200 ml of 20 ppm MO in water. A water pump (Masterflex L/S) was connected to the reactor, and pumped the water from beaker to the inlet port, see Fig. 17. The water went through the reactor and returned to the beaker from outlet port. The average UV intensity on the catalyst plate level was measured by an LI-COR pyranometer and was equal to  $70 \text{ W/m}^2$ , while the visible was determined to be  $80 \text{ W/m}^2$ . The experiment was carried out at room temperature (293K). An Ocean Optics spectrophotometer was employed to analyze the sample and monitor the photodegradation and decolorization of the MO by detecting the absorption at the maximum of 460 nm.

Table 6 Mass of prepared nanowires on  $50.8 \times 117.8 \text{ mm}^2$  borosilicate glass

Experiments	1	2	3	4	5	Average
Weight of catalyst (mg)	100.4	98.1	97.5	99.5	102.8	99.7

### 3.2.5 Characterization

Scanning electron microscopy (Hitachi S-800, 25eV) was used to observe the crystalline structure and orientation of the prepared nanowires. The diffraction pattern has been measured using an analytical Philips X-pert Pro X-ray Diffraction (XRD) for  $2\theta$  angles ranging from 5 to

50 degrees. An Ocean Optics spectrophotometer was used to acquire the UV-Vis diffuse reflection spectra.

### **3.3 Results and Discussion**

#### **3.3.1 The Weight of Prepared Nanowires**

Table 6 lists the individual weights of the NW arrays grown on two catalyst plates (borosilicate glass), placed at the bottom of the channel. The homogeneously distributed NWs were fabricated for a total of 2 hours with an estimated density of  $0.495 \text{ mg/cm}^2$ . In the preparation of Ag-ZnO NWs, various volumes of seed solution (1300 ml – 3000 ml) containing equimolar (5 mM) of  $\text{AgNO}_3$  and zinc acetate in ethanol were used in the formation of the seed layer. Thus, Ag-ZnO film containing different concentrations of Ag atoms is expected to be in the seeding layer. The estimated percentage of Ag atoms in the prepared Ag-ZnO nanowires from 1300 ml, 2300 ml and 3000 ml seeding solutions were 0.7%, 1.2% and 1.6%, respectively.

#### **3.3.2 Structural and Morphological Characterization Studies**

The SEM micrographs, depicted in Fig. 18 illustrate the similar morphology of the ZnO and doped Ag-ZnO nanowires with varying sizes of nanowires. The diameter and length of ZnO nanowires vary from 30-70 nm and 280-420 nm with average diameter and length to be 55 nm and 400 nm. The diameter and length of Ag-ZnO nanowires vary from 40-70 nm and 300-500 nm with average diameter and length to be 65 nm and 450 nm, respectively. The diameter of the prepared nanowires is influenced by the thickness of the seed layer due to the consumption rate of  $\text{ZnO}^{2+}$ , growth rate of nanowire side walls and nanowire density [43]. Tips of the nanowires are observed to have a predominantly hexagonal structure, in good agreement with results obtained by Wang et al. [215].

The XRD shown in Fig. 19 reveals that both synthesized nanowires show the (002) plane as a dominant reflection, a pattern initiated by the predominant growth of the wires along the c-axis perpendicular to the substrate surface. The XRD results reveal that the ZnO and Ag-ZnO nanowires are highly crystalline. From the XRD data, no significant difference in the diffraction pattern was observed between the undoped (ZnO) and doped ZnO (Ag-ZnO) nanowires, due to extremely low doping of Ag atom in the ZnO lattice. Additional explanation is that Ag atoms are deposited near the surface of the Ag-ZnO samples [27].

UV-Vis (electronic) absorption spectrum comparing both nanostructures is shown in Fig. 20. Within the visible range, 400-700 nm, Ag-ZnO nanowires show better absorption compared to ZnO nanowires. Also, the former shows better absorption in UV irradiation, demonstrating a better catalyst for photocatalytic technologies under solar illumination.

The possible states of Ag element in as-prepared catalyst Ag-ZnO nanowire were investigated by a commercial multichamber system SPECS GmbH (Berlin, Germany) under ultrahigh vacuum conditions ( $2 \times 10^{-10}$  mbar base pressure), consisting of two preparation chambers and one x-ray photoemission spectroscopy analyzing chamber. Based on the XPS data (Fig. 21), peaks of Ag 3d<sub>5/2</sub> and Ag 3d<sub>3/2</sub> are clearly located at 374.1 and 367.6 eV. The binding energies clearly reveal that Ag is deposited on the ZnO nanowires. Further experiment is required to confirm the oxidation state of silver atom in the catalyst, the identity of its nearest-neighbor atom, its bonding hybridization to that nearest-neighbor atom, as well as the bonding hybridization between the Ag atom in question and the next-nearest-neighbor atoms.

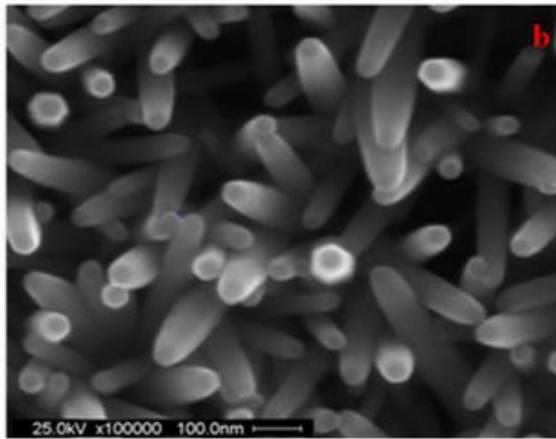
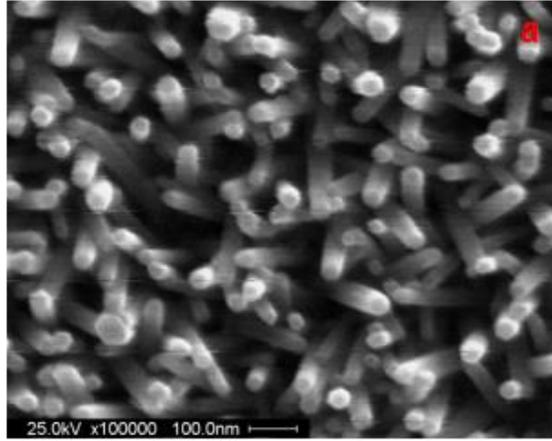


Figure 18 SEM images: a) ZnO nanowires b) ZnO/Ag nanowires

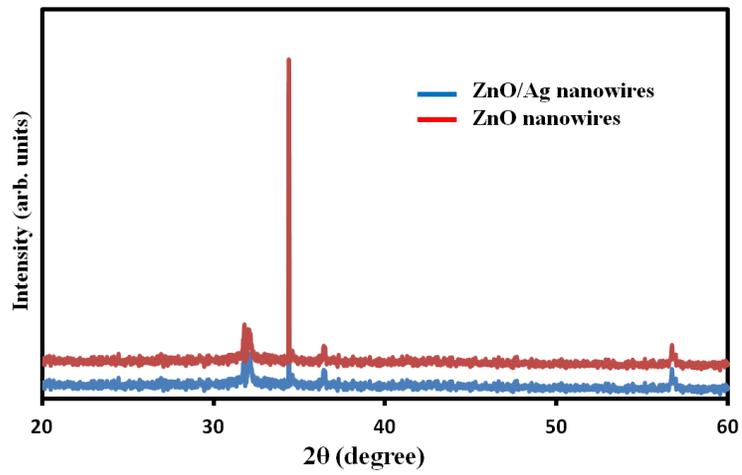


Figure 19 XRD powder patterns of ZnO (blue) and ZnO/Ag (red)

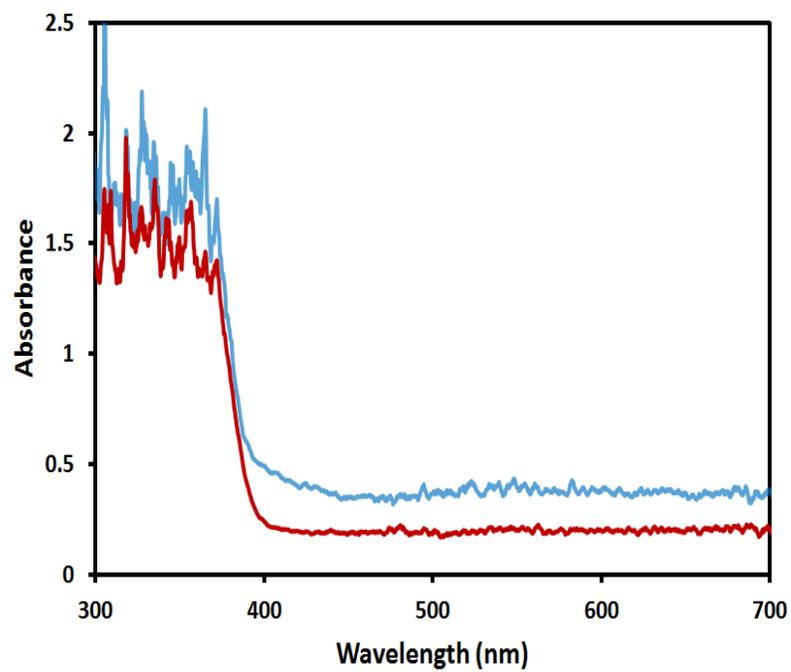


Figure 20 UV-vis absorption spectra of ZnO (blue) and ZnO/Ag (red)

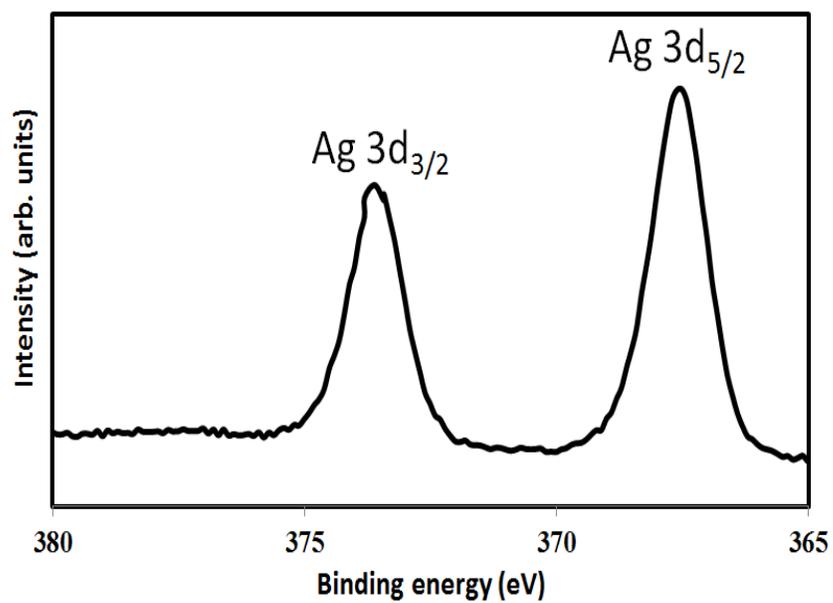


Figure 21 XPS spectra of the as-synthesized sample of Ag-ZnO nanowire

### 3.3.3 Optimization of Photocatalytic Reactor

Once the photoreactor was designed and fabricated, the operating parameters were optimized for the degradation of MO under visible and UV light irradiation. The reactor was effective using sprayed P25 on borosilicate (or soda lime) glass. The impact of experimental parameters including water flow rate and/or depth was investigated to achieve optimal conditions for effective operation (Table 7). In the degradation of 20 ppm MO with  $0.50 \text{ mg/cm}^2$  of  $\text{TiO}_2$  catalyst sprayed on the glass, there was no significant difference in the photodegradation efficiency within a flow rate range 60-300 ml/min. However, increased water depth reduced the overall reaction, with a net lowering of efficiency. This could be due to the absorption of UV light by the MO solution, blocking photons from reaching the active reaction sites. Optimization values achieved for the fabricated photoreactor for the degradation of 200 ml of MO at initial concentration of 20 ppm at room temperature were found at (Table 7): catalyst loading of  $0.50 \text{ mg/cm}^2$ , UV light intensity  $47.2 \text{ W/m}^2$ , flow rate 60 ml/min and water depth 2 mm.

### 3.3.4 Photocatalysis Studies

Once the optimization of the operational parameters of the photocatalytic reactor using 100 mg of P25 ( $\text{TiO}_2$ ) at initial concentration of MO of 20 ppm was established, an initial study was conducted with different doping levels of Ag for the degradation of MO under UV irradiation to determine best dosage for further study (data not shown). It was found that photocatalytic activity and target percentage of Ag doping in ZnO varies in the following order: Pure ZnO < Ag-ZnO (0.5%) < Ag-ZnO (1.0%) > Ag-ZnO (1.9%) < Ag-ZnO (1.2%). Based on these experimental results, Ag-ZnO (1.2%) was selected for further study because it inferred the highest photodegradation efficiency; Ag doping levels beyond the optimal point resulted in reduced efficiency.

Subsequently, the photocatalytic activity of ZnO and Ag-ZnO nanowires was evaluated, and compared to P25 for the degradation of MO in water at initial concentration of 20ppm in visible and UV light (Fig. 22). In Figure 22a, Ag-ZnO (1.2%) has shown a significantly higher photodegradation performance than ZnO, while similar results were obtained when compared to TiO<sub>2</sub> under visible light for 4 h. Under UV light irradiation, ZnO nanowires revealed less photocatalytic performance than Ag-ZnO nanowires, while TiO<sub>2</sub> demonstrated the similar performance as the doped Ag-ZnO nanowires.

Variation in the activity of the different dosage (Ag %) were most likely due to the Ag atom which captures electrons and enhances the separation of electron-hole pair. Photocatalytic performance of Ag-ZnO nanowire was parallel to those observed by Ren et al [38]. In a similar result under visible light irradiation, without any surfactant, ZnO/Cr nanowires prepared by

Table 7 Effect of water flow rate and depth in the reactor on photocatalytic degradation of methyl orange after 4 h with sprayed P25 film as catalyst

MO solution flow rate (ml/min)	MO solution depth (mm)	% MO degradation in 4 h	Best operating condition
50	2	88	
62	2	98	62 ml/min
150	2	99	
300	2	99	
62	1	84	
62	2	97	2 mm
62	4.5	94	

solvothermal technique revealed higher photocatalytic degradation of MO solution compared to ZnO nanowire and P25. The visible light photoactivity could be credited to the modification of interactions between the conduction band (CB) and valence bands [216]. Further, doped ZnO/Sb (Antimony) and ZnO nanowires were fabricated via a vapor-solid method and tested for photoactivity performance under visible and UV light. The doped catalyst has shown a superior photocatalytic performance over ZnO nanowires base on the effect of oxygen defect and reduction of electron/hole recombination [217].

In a related work of photocatalytic activity of Ag-ZnO nanorods, though synthesized by a photolytic deposition method, the mechanism of photodegradation of MO typically involves a combination of hydroxylation and demethylation [218]. Hydroxylation breaks the nitrogen-carbon bond of the R-N(CH<sub>3</sub>)<sub>2</sub> group as a result of hydroxyl (OH•) radical attack on an aromatic ring. Subsequently, the terminal R-N(CH<sub>3</sub>)<sub>2</sub> group loses a -(CH<sub>2</sub>)- via substitution by a hydrogen (H) atom, this process is called demethylation. Further hydroxylation and demethylation reactions break down the intermediate by-products into simpler compounds eventually producing carbon dioxide and water.

### **3.5 Catalyst Stability and Reusability**

A major drawback of ZnO photocatalysts is the photocorrosion induced by electron/hole separation; this is a vital concern for multiple applications of the photocatalyst, particularly for a large-scale production and commercialization. The photocatalytic experiments were conducted over several cycles similar to as-prepared catalysts (ZnO, Ag-ZnO nanowires (1.2 %) and P25) at 20 ppm of MO for 2 h under UV-light irradiation (Figure 23). After each experiment, the catalysts were rinsed repeatedly with water, dried and used for the next experiment. After the fourth cycle, the photoreduction of MO by the catalysts were 61 %, 76 %, 80 %, respectively.

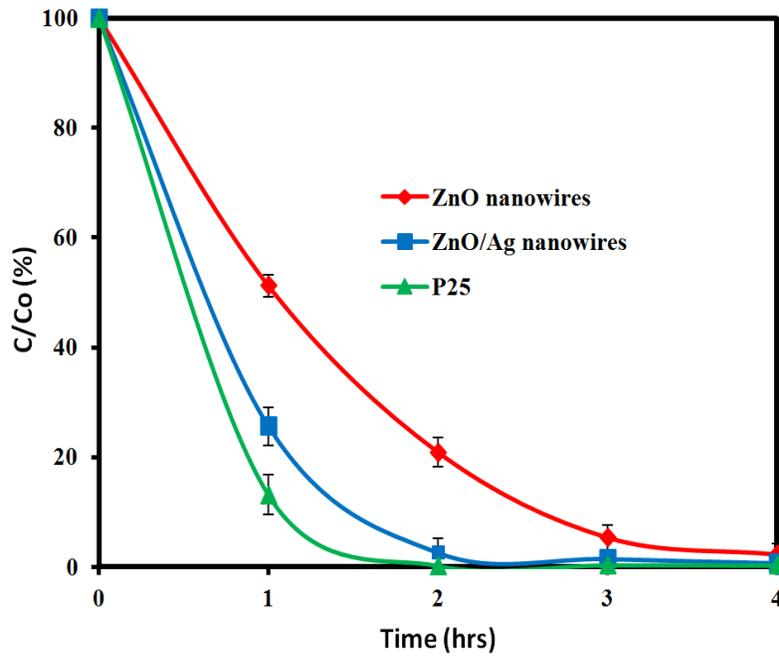
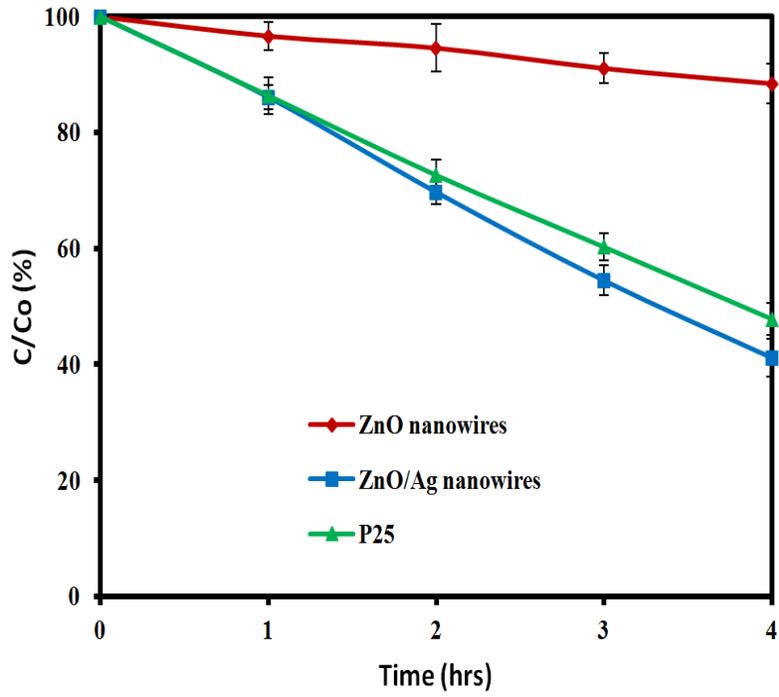


Figure 22 Photodegradation of MO under: visible (top) and UV (bottom) light irradiation

Although ZnO nanorods array were fabricated by a combined wet chemical and photolytic deposition method by Ren et al. [219], similar photostability results were reported. Clearly photocorrosion, due to several competing factors, is a complex process requiring further investigation.

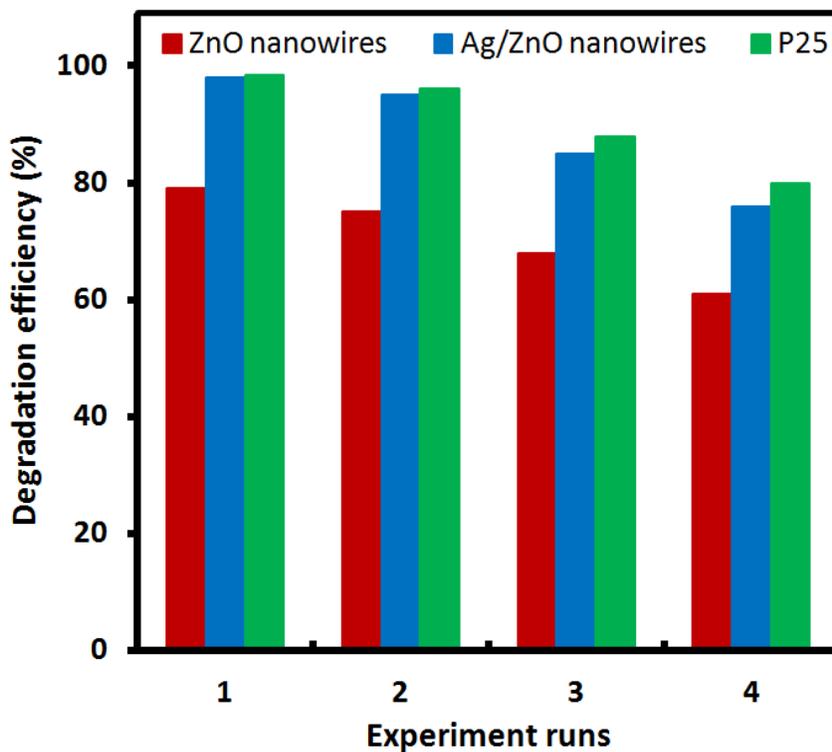


Figure 23 Repeated cycles of MO photodegradation using ZnO, Ag-ZnO nanowires and P25 catalysts under UV irradiation for 2 hours

## CHAPTER 4: PHOTOCATALYTIC DEGRADATION OF PHENOL

### 4.1 Introduction

Phenols are among the numerous organic pollutants and toxic chemicals discharged into the aquatic environment that cause negative flavor and unpleasant odors in potable water. Phenols are recalcitrant and stem from industrial sources, including pesticide, paint, petroleum and petrochemical industries, to mention a few [195, 220, 221]. Despite their low dosage, these pollutants may pose a major health hazard due to their mutagenicity and genotoxicity. Phenols are mutagenic and may be absorbed through the skin and harmful even at low dosage [222, 223]. Hence, degradation of phenol is important. A large body of researchers have worked on a number of remediation processes and come up with several chemical [224-226], biological [227], and physical [228, 229] processes. Since the application of these processes involve high cost and could possibly introduce more contaminants into the environment, developing energy efficient and 'green' technologies to minimize these limitations while producing the desired complete mineralization of organic contaminants is of particular importance. Advanced oxidation processes (AOP), a process of mineralization of organic compounds into simple products such CO<sub>2</sub> and water, has emerged as the most promising technology in the last few decades [230-232]. Among the semiconductors for AOPs, TiO<sub>2</sub> and ZnO are the most often studied materials and

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<sup>3</sup>Portions of this chapter is presently in press in American Journal of Analytical Chemistry (I. Udom, P. Meyers, Y. Zhang, M. K. Ram, A. F. Hepp, E. K. Stefanakos, D. Y. Goswami, Optimization of photocatalytic degradation of phenol using simple photocatalytic reactor, American Journal of Analytical Chemistry).

employed due to their ability to produce hydroxyl radicals to destroy numerous types of organic contaminants [233]. Moreover, they are non-toxic, cheap and abundant.

A number of researchers have investigated the photodegradation of phenol using metal-doped photocatalysts, for example, Grabowska et al. [220] reported a three times higher photodegradation with 3% -W-TiO<sub>2</sub> compared to pure TiO<sub>2</sub> under visible light irradiation. In the presence of W-TiO<sub>2</sub> under visible light phenol was degraded to catechol and muconaldehyde. Devi and Rajashekhar [234] doped TiO<sub>2</sub> with N<sub>2</sub> gas to mineralized phenol under visible and UV light irradiation. Higher photodegradation was achieved with 0.15% dopant concentration compared to sol-gel TiO<sub>2</sub> for the photodecomposition of phenol under UV/solar irradiation employing H<sub>2</sub>O<sub>2</sub> and ammonium peroxydisulfate as acceptors. Furthermore, Kavitha and Palanivelu [235] conducted a batch study of using phenol as a model pollutant in industrial water to optimize parameters such as a pH, hydrogen peroxide and ferrous oxide concentrations affecting Fenton-related oxidation reaction. The highest photodegradation efficiencies were Fenton (41%), solar (96%) and UV-Fenton (97%) processes.

As evident from the literature, not much research has been done in optimization of photodegradation of phenol with immobilized ZnO-Ag nanowires using a simple photocatalytic reactor under UV irradiation.

## **4.2 Experimental**

### **4.2.1 Materials**

All chemicals are of analytical standard and were used without further purification. Silver nitrate (AgNO<sub>3</sub>, 99.9%) was purchased from Sigma-Aldrich and used to provide doping, zinc acetate [Zn(CH<sub>3</sub>COO)<sub>2</sub>, 99.9%] was procured from Fisher Scientific. Sodium hydroxide

(NaOH, 44%) and hydrochloric acid (37%) were also obtained from Fisher Scientific. The double-distilled water was employed to prepare the desired phenol concentration.

#### **4.2.2 Photoreactor**

All experiments were carried out in a laboratory fabricated aluminum photoreactor with dimension of 38.1 cm (15 in) long by 5.1 cm (2 in) wide by 2.5 cm (1 in) high. Aluminum sheet of 5.6 cm was used to build this reactor. A peristaltic pump (Masterflex L/S, 160 ml/min flow) was connected and pumped water from the glass beaker to the reactor. The water circulated through the reactor and returned to the beaker continuously during the experiment. The reactor system contained a lid, a UVA transparent glass, which was employed to prevent evaporation. The vessel top contains a light source. A lamp box which consisted of two Southern New England Ultraviolet Company Rayonet RPR-3500 Å UVA lamps (30.5 cm long) was used; the lamps provided irradiation in the UVA range of 350 – 400 nm. Other information about the photoreactor can be found at Udom et al. [236]. The light intensity at the surface of the reactor in the photoreactor was measured by an LI-COR pyranometer.

#### **4.2.3 Preparation of Ag-Zn NWs**

A seed solution of equimolar ratio (5 mM) of  $\text{AgNO}_3$  and  $\text{Zn}(\text{CH}_3\text{COO})_2$  in ethanol was prepared; a 1.25 ml aliquot of this solution was placed on a substrate. An aliquot of 0.5 ml seed particle solution was placed on the substrate (borosilicate glass) and randomly tilted in different directions to ensure uniform distribution. The seeded substrate was dried in an oven at 100 °C for 10 min to remove moisture and another 30 min. at 350 °C to remove unreacted organic matter. After cooling, the substrate was placed in a reactor containing the growth solution, and stirred for 2 hours at 90 °C. After this step, the substrate was rinsed with water and oven dried at 100 °C for 10 min. and 350 °C for 30 min.

#### **4.2.4 Procedure and Analysis**

The reaction mixture was initially placed in the dark for 30 min to establish adsorption equilibrium of phenol solution on the photocatalyst and then UV irradiated for 150 min. At certain interval, aliquots (5ml) were collected and analyzed to assess photodegradation. Gas chromatograph (SRI8600) with 3000 cm DB-624 capillary column and flame ionization detector (FID) capability was employed to study the degradation of phenol analytes. To evaluate the impact of initial concentration and catalyst dosage on photocatalytic efficiency, experiments were performed at initial phenol concentration from 10 - 60 mg/L and catalyst loading 250 - 7500 mg/L. After determination of the optimal values, additional parameters including pH and light intensity were investigated for optimization and a model was established. Diluted NaOH and HCl were used to adjust pH within range 2.7 to 11 and was measured using Orion 5 Star ThermoScientific. The unadjusted initial phenol solution measured pH 8.2.

### **4.3 Result and Discussion**

#### **4.3.1 Effect of Initial Phenol Concentration**

The effect of initial phenol concentration on the removal rate equation is vital for the optimization of the different concentration of phenol and development of a model. The reaction rate constant,  $K$  ( $\text{min}^{-1}$ ), decreases as the initial concentration increases while holding other parameters constant. This could be due to saturation of active sites on the photocatalyst by intermediates, hereby creating fewer sites for adsorption and creation of hydroxyl ions. Unlike other contaminants, the transmittance of UV light through the aqueous solution of phenol, due to its transparency, does not contribute to the decrease in rate constant. In the Figure 24, the empirical first-order relationship of different initial concentrations of phenol to the reaction rate constant is illustrated. Shukla et al. [237] examined the role of initial concentration (12.5 -37.5

ppm) in the photodegradation of phenol. Optimum value was achieved at 12.5 ppm, under the conditions studied (ZnO = 0.4 g/L, persulfate = 2g/L and power = 330W). Pardeshi and Patil demonstrated that the degradation of phenol decreased as the phenol concentration increases in range 25 300mg/L [66]. Due to the constant reaction condition, the lesser amount of OH and O<sub>2</sub> radicals are available as more and more substrates molecules are adsorbed on the surface on the photocatalyst.

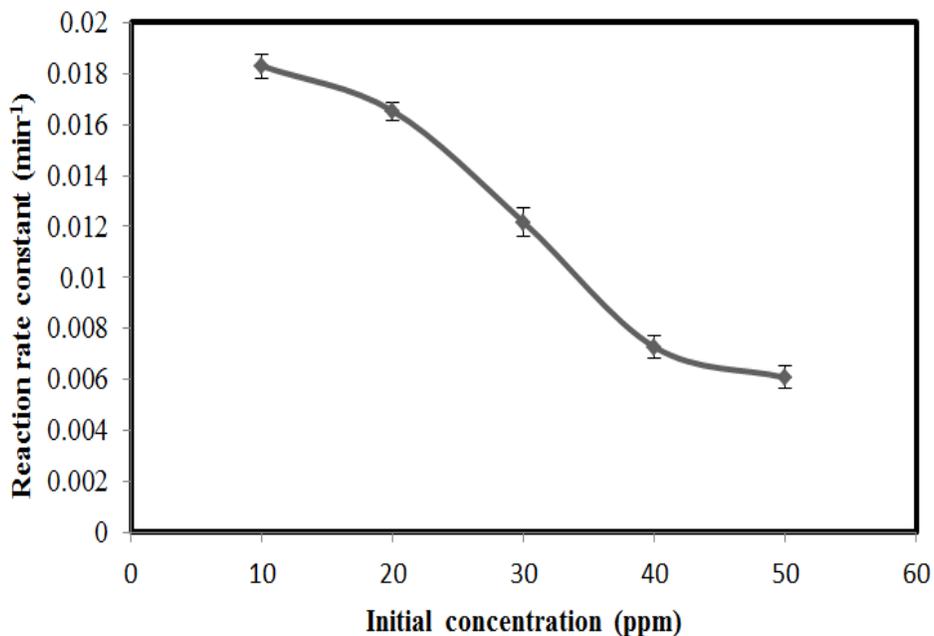


Figure 24 Effect of the initial concentration of phenol on reaction rate constant. Ag-ZnO NW = 500 mg/L, T = 295 ± 2 K, pH =8.7, Light intensity = 60 W/m<sup>2</sup>

#### 4.3.2 Effect of UV Intensity

The effect of UV light intensity on the photocatalytic degradation of aqueous organic compound is significant, as the UV irradiation creates the photons needed to move electrons from the valence band to the conduction band of the semiconductor photocatalyst. The irradiation produces the energy to drives the overall reaction, thus the reaction rate constant depends on the intensity of the irradiation. The rate of photocatalytic mineralization of phenol

increases as more photons (increasing radiation) of sufficient energy reach the surface of the catalyst. The light intensity plays a key role in the initiation of electron-hole formation in the photochemical reaction. Chiou et al. [238] examined the effect of UV light intensity (20-40 W) on the phenol degradation. Under UV irradiation over TiO<sub>2</sub> photocatalyst, the reaction rate constants were 0.0083, 0.012 and 0.031 min<sup>-1</sup> with light intensity of 20, 100 and 400 W, respectively. A more or less linear correlation was established between the rate constants and light intensity. Ollis et al. [239] have studied the photocatalytic degradation of organic pollutants such as benzene and perchloroethylene in UV/TiO<sub>2</sub> system at intensity within the range  $\leq 25$  mW/cm<sup>2</sup> and above. They reported that the reaction rate was independent of the light intensity at a higher intensity.

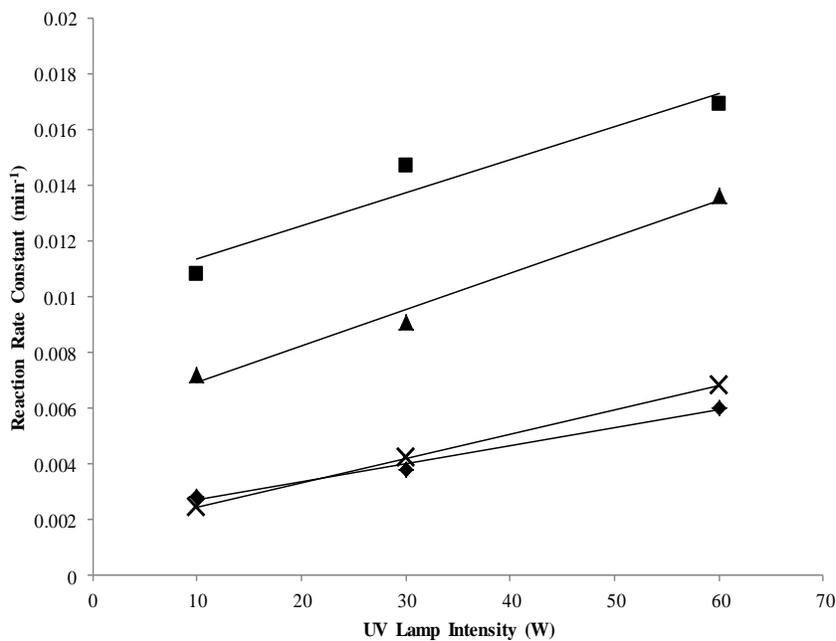


Figure 25 Effect of the UV light intensity on reaction rate constant. Ag-ZnO NW = 500 mg/L, T = 295 ± 2 K, initial concentration = 30 ppm, and pH = 2.7 (♦), 5.0 (■), 8.7 (▲), and 11 (×)

In this study, varying intensities of UV radiation (10, 30, and 60 W) were used with Ag-ZnO NWs to catalyze the degradation of phenol in water at varying pH (2.7, 5.0, 8.1, and 11.0).

The data are plotted in Figure 25 as reaction rate constant versus UV lamp intensity. Approximate linearity with respect to lamp intensity is observed at each pH level considered.

### **4.3.3 Effect of pH**

The role of pH on the performance of photocatalytic degradation of phenol was investigated in the pH range 2.7 – 11; the results are plotted in Figure 26. The three sets of data, reaction rate versus pH level, correspond to data collected at constant UV lamp intensity (10, 30, or 60 W). While the choice of interpolation curve is somewhat arbitrary (for each set of data, a cubic polynomial is fit to the data points), each curve suggests a maximum reaction rate at a pH level of approximately 5.5 – 6.0. At pH (5-6), most of the phenol molecules are adsorbed on the surface of the photocatalyst due to the undissociated nature of the phenol thereby producing higher photocatalytic efficiency. The surface of the photocatalyst is negatively charged, at higher pH (higher alkalinity), phenolate intermediates may be repelled away from the catalyst surface thereby opposing adsorption of contaminant molecules. As a result, lower degradation of phenol is observed in alkaline environments. Similar results were reported by Pardeshi and Patil [66] and Lathasree [240]. Also, Akbar and Onar [241] studied the effect of pH on the photodegradation of phenol at the pH range 3-8. At mildly acidic condition, such as pH 5, the highest photocatalytic activity was observed, while addition of an oxidant/electron acceptor ( $H_2O_2$ ) to the system increased phenol degradation to 99.2 %.

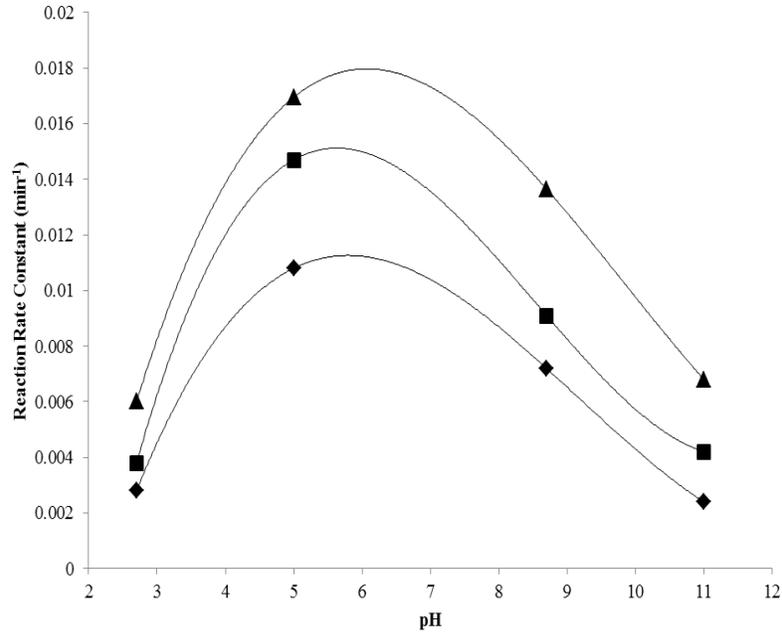


Figure 26 Effect of pH on reaction rate constant. Ag-ZnO NW = 500 mg/L, T = 295 ± 2 K, initial concentration = 30 ppm, and UV lamp intensity = 10 W (♦), 30 W (■), and 60 W (▲)

#### 4.3.4 Empirical Correlation

In formulation of a complete model equation for the degradation of phenol by Ag-ZnO nanowires at varying pH and UV intensities, the data and their dependence on each variable initially were examined separately, as depicted in Figures 23 and 24. As can be seen in Figure 23 the dependence on UV lamp intensity is adequately modeled by a linear equation; that is:  $K(I) = a_1I + a_0$ . Here,  $I$  is the UV lamp intensity, in W, and  $a_1$  with units of  $W^{-1} \text{ min}^{-1}$ , represents the constants that fit the empirical model to the collected data. Similarly, the data suggest that the pH dependence can be captured by a polynomial, albeit with more terms. In other words:

$$K(\text{pH}) = \sum_{i=0} b_i \text{pH}^i$$

For the case of a cubic polynomial, for instance:

$$K(\text{pH}) = b_3\text{pH}^3 + b_2\text{pH}^2 + b_1\text{pH} + b_0$$

Here,  $b_i$  (units of  $\text{min}^{-1}$ ) likewise represents the constants of the empirical model. In fitting the multivariate model, the most obvious choice for a mathematical description of the data would be a similar polynomial, which can be formulated as follows;

$$K(I, \text{pH}) = \sum_{i=0} \sum_{j=0} c_{ij} I^i \text{pH}^j$$

In this case,  $C_{ij}$  ( $\text{W}^{-i} \text{min}^{-1}$ ) represents the constants of the multivariate model. In fleshing out the form of the final model, it is useful to recall the linearity of the data with respect to variable UV lamp intensity; hence, in this study, we neglected any terms of quadratic or higher order in intensity. Similarly, we recognize that, given that cubic polynomials capture the pH dependence quite well, we can neglect quadratic and higher order terms in pH (i.e.,  $j \leq 3$ ).

The data obtained from experiment were fitted to potential polynomial models using a least-squares regression. The results of the analysis of various potential models are tabulated as shown in Table 8. For each equation, derived constants and the corresponding coefficient of determination ( $R^2$ ) are given.

Table 8 Derived model parameters and coefficient of determination for candidate model equations

Model equation	$c_{00}$	$c_{10}$	$c_{01}$	$c_{11}$	$c_{02}$	$c_{12}$	$c_{03}$	$c_{13}$	$R^2$
$c_{00} + c_{10}I + c_{01}\text{pH} + c_{11}I\text{pH} + c_{02}\text{pH}^2$	-0.01392	8.116E-05	0.007423	2.846E-06	-5.604E-04				0.8943
$c_{00} + c_{10}I + c_{01}\text{pH} + c_{11}I\text{pH} + c_{02}\text{pH}^2 + c_{12}I\text{pH}^2$	-0.009616	-4.796E-05	0.005811	5.118E-05	-4.428E-04	-3.528E-06			0.9057
$c_{00} + c_{10}I + c_{01}\text{pH} + c_{11}I\text{pH} + c_{02}\text{pH}^2 + c_{12}I\text{pH}^2 + c_{03}\text{pH}^3$	-0.02801	-4.796E-05	0.01637	5.118E-05	-0.002168	-3.528E-06	8.393E-05		0.9934
$c_{00} + c_{10}I + c_{01}\text{pH} + c_{11}I\text{pH} + c_{02}\text{pH}^2 + c_{12}I\text{pH}^2 + c_{03}\text{pH}^2 + c_{13}I\text{pH}^3$	-0.02819	-4.257E-05	0.01648	4.808E-05	-0.002184	-3.023E-06	8.475E-05	-2.459E-08	0.9934

It can be seen that on the basis of the coefficient of determination, the best fit is given by the following equation:

$$K(I, \text{pH}) = c_{00} + c_{10}I + c_{01}\text{pH} + c_{11}I \text{pH} + c_{02}\text{pH}^2 + c_{12}I \text{pH}^2 + c_{03}\text{pH}^3$$

This equation is plotted in Figure 27 with experimental data for comparison. It is interesting to note that the addition of the  $c_{13}I \text{pH}^3$  term does nothing appreciable to improve the accuracy of the fit of the model equation. Also, the authors examined higher order polynomials with similar deficiency in accuracy: a simple quadratic polynomial gives an  $R^2$  value of 0.9866. As such, the above equation is recommended for further design calculations and scale up of the bench scale reactor.

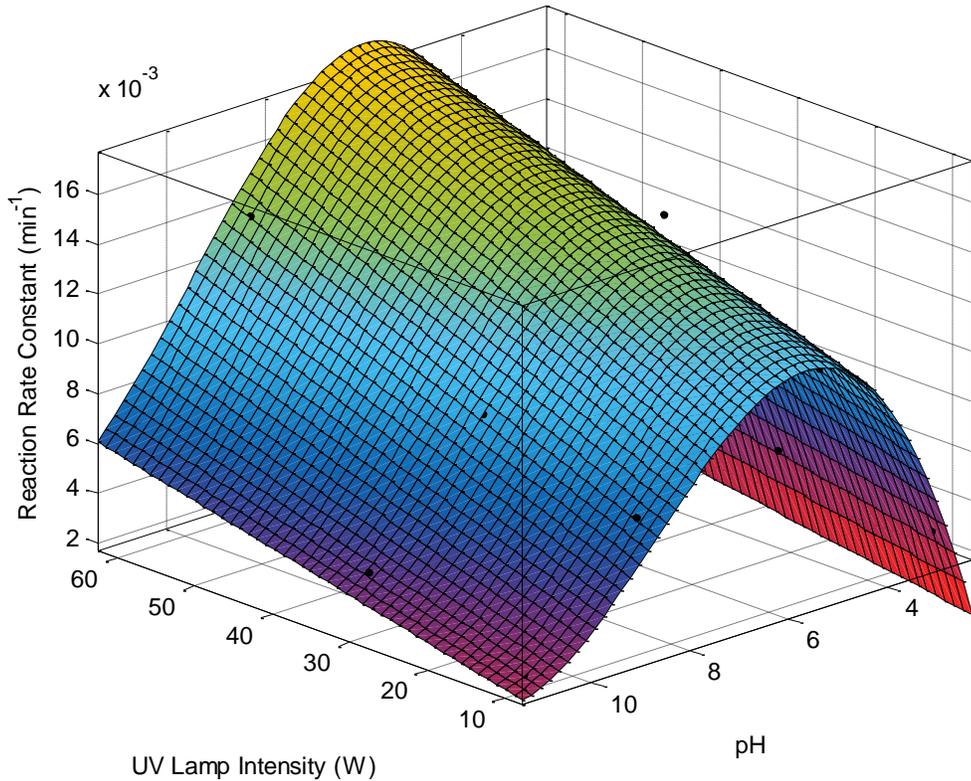


Figure 27 The recommended polynomial model equation plotted on three axes as a surface with experimental data (•) overlain

Finally, we consider the uncertainty in the derived model equation parameters. For the chosen equation, 95% percent confidence intervals were generated for each equation parameter; the results are presented in Table 9. It can be seen that while a good fit was obtained, on the basis of the coefficient of determination, there is a good degree of variability over the 95% confidence intervals for most of the model parameters. It may be beneficial as a part of future investigative work to examine operating conditions of intermediate pH and / or UV intensity to the work considered here; by considering a greater breadth of data, a greater degree of certainty regarding the equation parameters of the resultant model may be obtained.

Table 9 Derived model equation with parameter values of >95% confidence intervals

$c_{00} + c_{10}I + c_{01}pH + c_{11}I pH + c_{02}pH^2 + c_{12}I pH^2 + c_{03}pH^3$			
Parameter	Value	95 % Confidence Interval	
$c_{00}$	-0.02801	-0.03554	- -0.02048
$c_{10}$	-4.796E-05	-1.710E-04	- 7.504E-05
$c_{01}$	0.01637	0.01265	- 0.02009
$c_{11}$	5.118E-05	8.586E-06	- 9.377E-05
$c_{02}$	-0.002168	-0.002723	- -0.001612
$c_{12}$	-3.528E-06	-6.599E-06	- -4.564E-07
$c_{03}$	8.393E-05	5.752E-05	- 1.103E-04

## CHAPTER 5: CONCLUSIONS AND FUTURE WORK

As presented in Chapter 1, the research includes three main goals:

- a. Determine the effect of transition metal dopants on photocatalytic material performances.
- b. Development of a simple, inexpensive, scalable and effective ZnO nanowire (NW) photocatalyst by modifying the morphology via a synthesis method.
- c. Optimization of the photocatalytic degradation of phenol using a simple photocatalytic reactor.

Relative to the first goal, Chapter 2 reported the materials characterization analysis which showed that we have successfully produced different photocatalysts promoted using transition metal co-catalysts with various concentrations (1 to 5 percent) and using anatase or mixed anatase and rutile (P25). EDS confirms an approximate elemental composition of each of the promoted photocatalysts. However, some of them did not yield the expected weight percent target. As seen in the SEM photographs, the catalyst particles tend to conglomerate smaller particles on the surface, probably from co-promoters. Five weight-percent Cu in anatase and P25 proved to be ineffective. 1% wt. Pt in P25 proved to be effective. The best catalyst in this study was 1% wt. Ru in anatase. According to the XPS data, Ru is in the more reduced state with a BE of  $\sim 281$  eV (Ru(0)) and minor phase RuO<sub>2</sub> in P25, similar to Cu (above). The resolution between the peaks from 279.0 to 283.0 eV is poor due to interference from C. These trends can be best explained by assuming that metallic Ru (denoted as Ru(0) or Ru<sup>0</sup>) has emerged by the

high-temperature treatment, with the higher surface area P25. The contribution of the oxidized  $\text{RuO}_2$  ( $\sim 283$  eV) is more pronounced on anatase.

Future work will include testing of the photocatalyst in a UV reactor to determine how effective it is in the decomposition of other organic compounds.

In Chapter 3, a facile technique, hydrothermal processing, was successfully employed to fabricate ZnO and Ag-ZnO nanowires on reaction plates. This alternative approach is simple, scalable, cost effective and environmental friendly for the production of quality Ag-ZnO, with enhanced photocatalytic activity for water purification. The conclusion of this study also indicates that Ag-ZnO nanowires shown better photocatalytic performance, in both light sources, than ZnO nanowires, and a similar level of performance with P25. For future work, the fabricated photocatalyst should undergo further characterization and be tested on microorganism for disinfection. In addition to the disinfection application, the fabricated nanowires should be investigated for photocatalytic efficiency in air purification and under sunlight.

Finally, Chapter 4 demonstrates the successful immobilization of Ag-ZnO NWs on a borosilicate glass for successful degradation of phenol, relative to the third goal. From a preliminary study, an optimal initial concentration (30 mg/L) of phenol was attained. An attempt to form an overall model for the variation in the phenol degradation rate as a function of UV light intensity and pH level was made. For constant pH, it was found that the reaction rate is approximately linear with respect to UV light intensity. For constant UV light intensity, the reaction rate is approximately cubic in pH. As such, a cubic model equation was derived (see Table 9) with only linear terms in UV light intensity. The equation was found to fit the data with a coefficient of determination ( $R^2$ ) of 0.9934, and 95% confidence intervals were generated for all model parameters. Additional terms to the model equation were found not to improve the

overall fit to the experimental data. Recommendations for future work include the incorporation of more variables in the overall equation to improve the accuracy of the present model. Also, the applicability of the current model should be examined for visible light irradiation with the fabricated catalyst applied to the disinfection of microorganisms.

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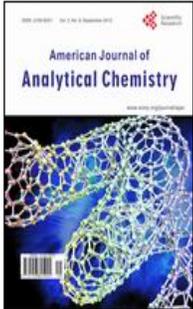
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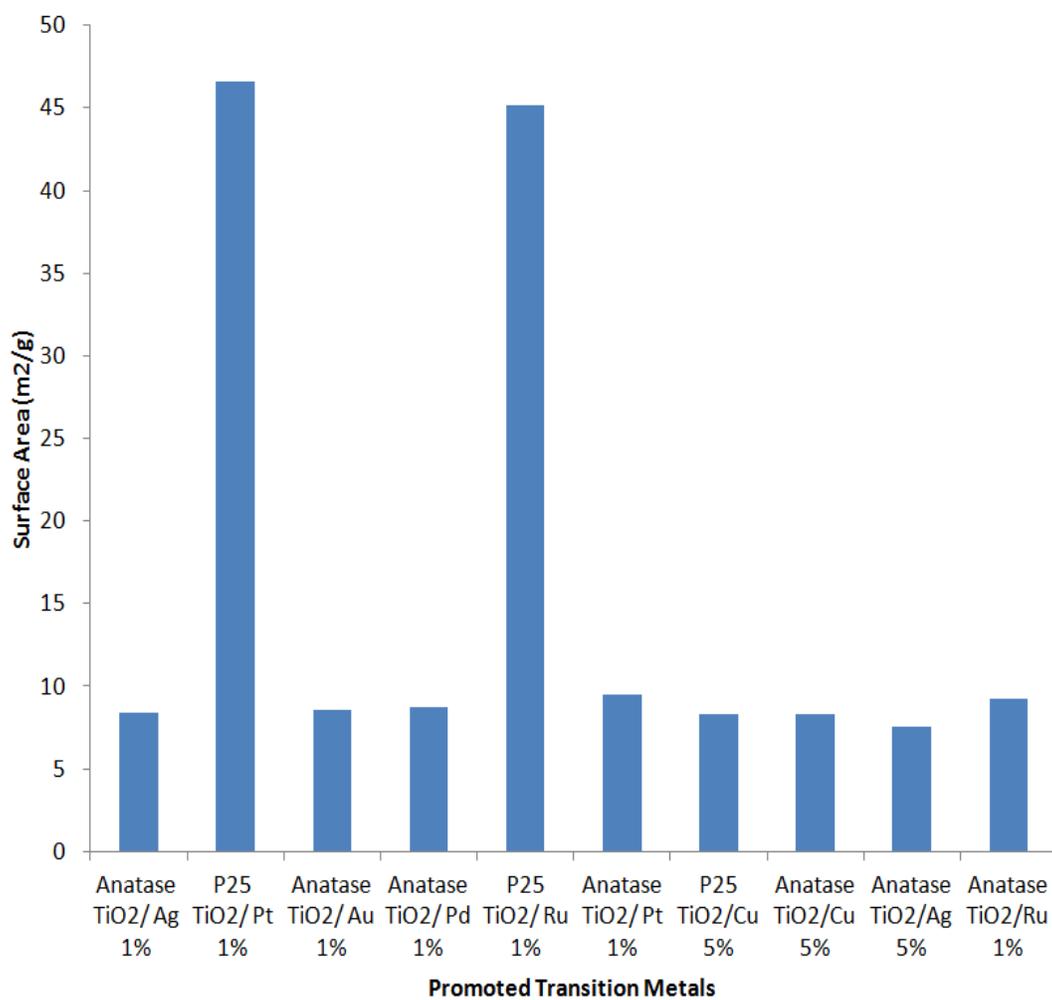


Figure B.1 Surface area measurements of all the photo catalysts

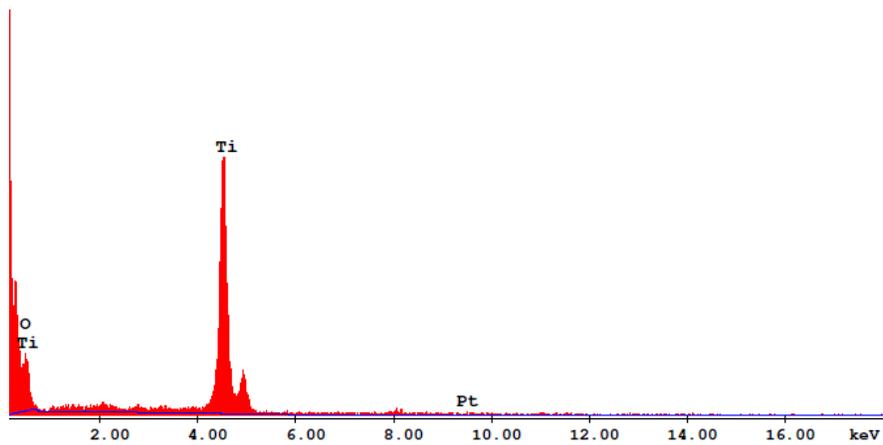


Figure B.2 EDS graphical elemental composition analysis of anatase TiO<sub>2</sub>/Pt 1%

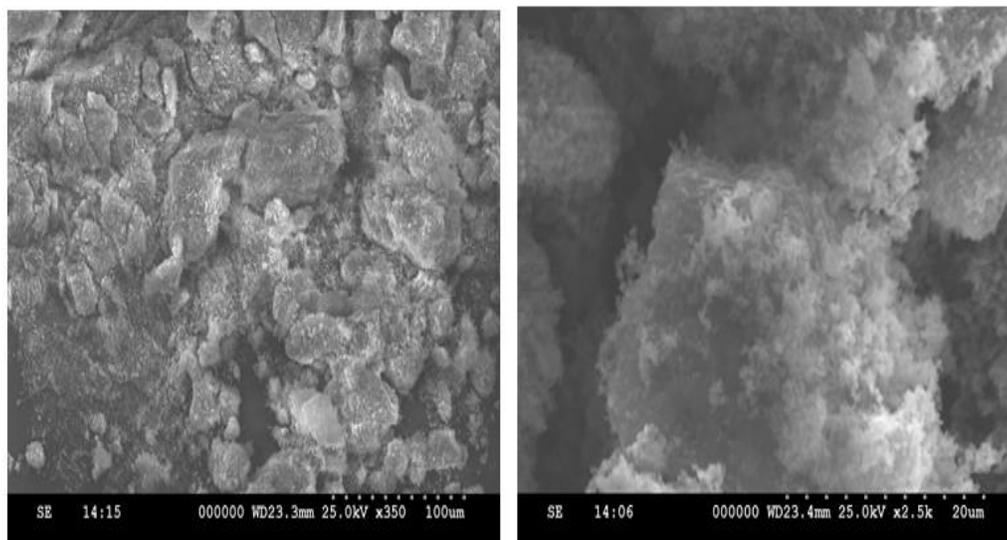


Figure B.3 Topographical images of photocatalyst made of anatase TiO<sub>2</sub>/Pt 1%

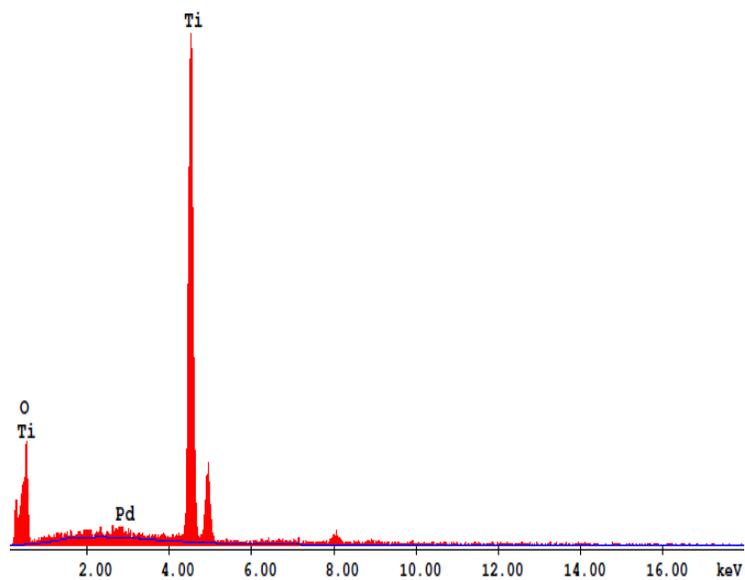


Figure B.4 EDS graphical elemental composition analysis of anatase  $\text{TiO}_2/\text{Pd}$  1% photocatalyst (MDM-2-Pd 1%)

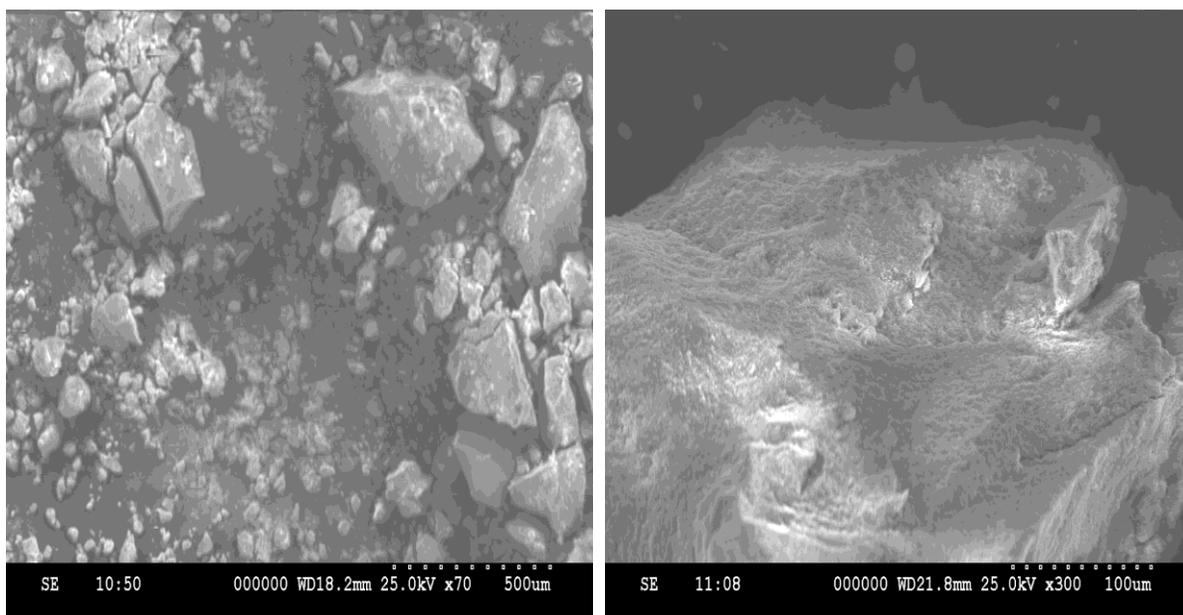


Figure B.5 Topographical images of photocatalyst made of anatase  $\text{TiO}_2/\text{Pd}$  1%

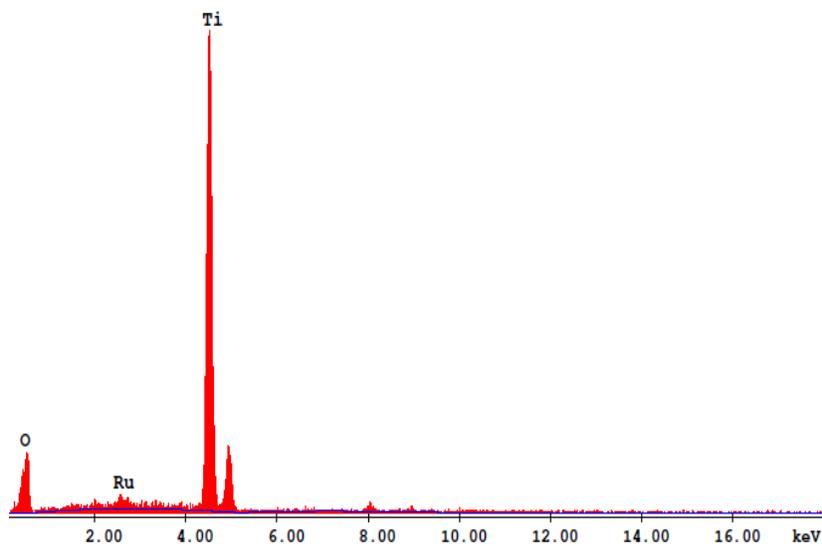


Figure B.6 EDS graphical elemental composition analysis of anatase  $\text{TiO}_2/\text{Ru}$  1% photocatalyst (MDM-3-Ru 1%)

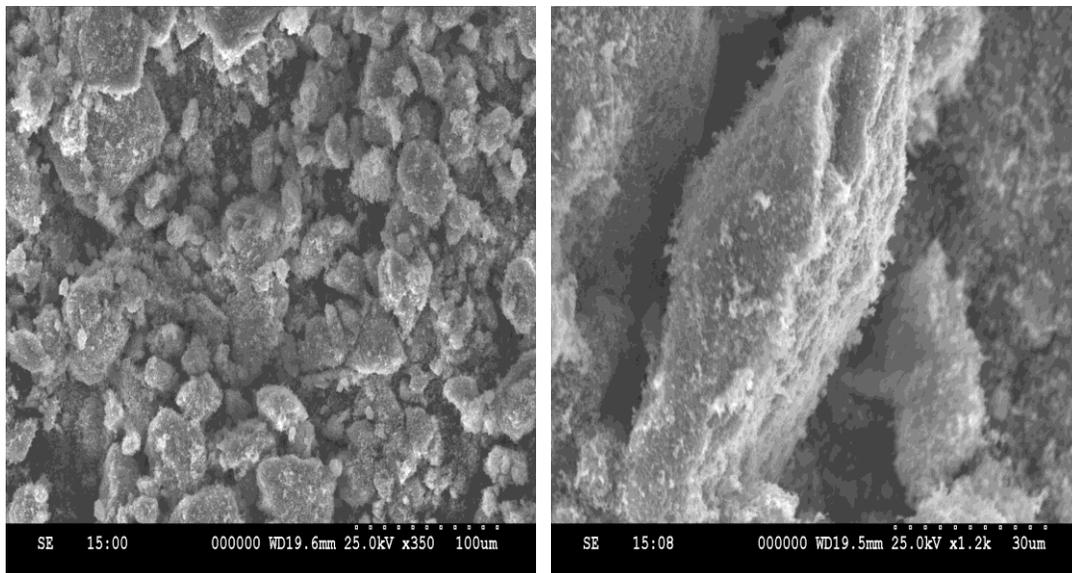


Figure B.7 Topographical images captured of anatase  $\text{TiO}_2/\text{Ru}$  1%

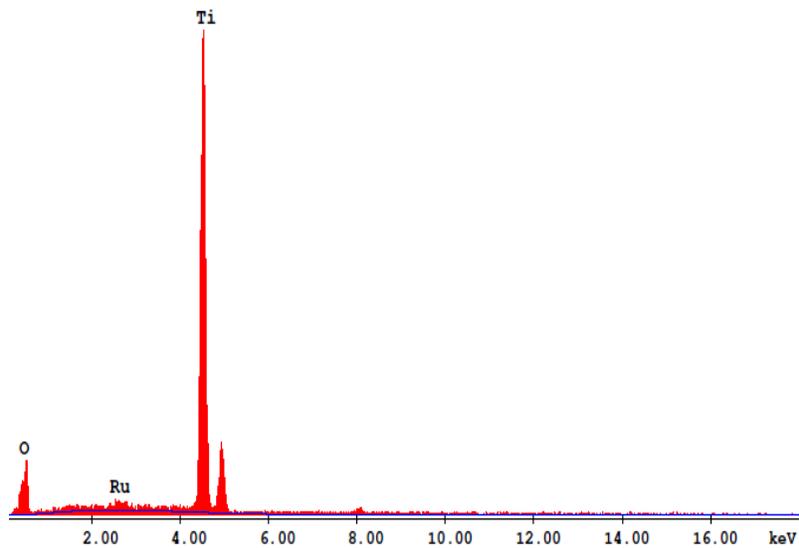


Figure B.8 EDS catalyst elemental composition of photocatalyst made of P25 TiO<sub>2</sub>/Ru 1%

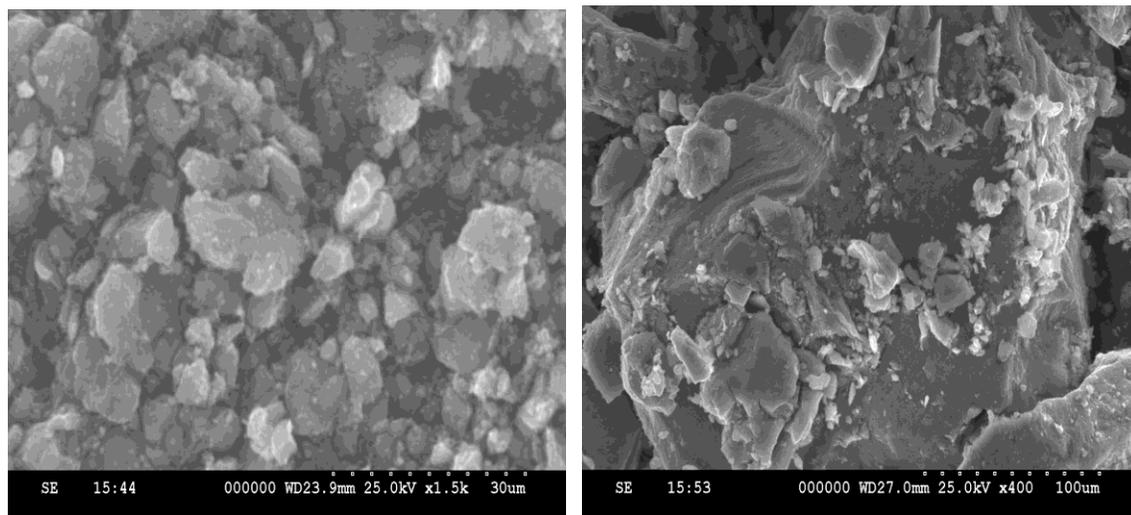


Figure B.9 Topographical images of photocatalyst made of P25 TiO<sub>2</sub>/Ru 1%

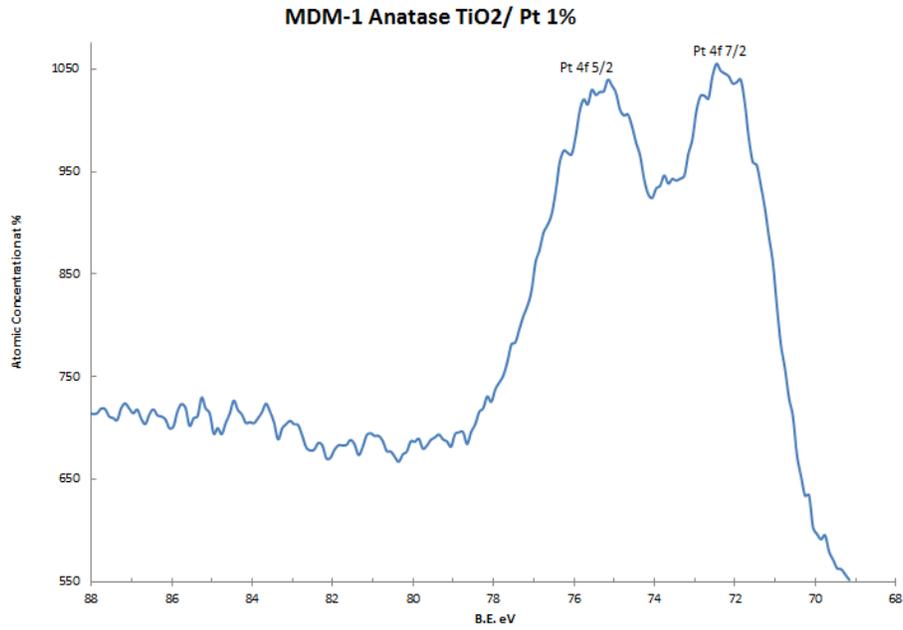


Figure B.10 XPS data for anatase titanium/Pt 1%

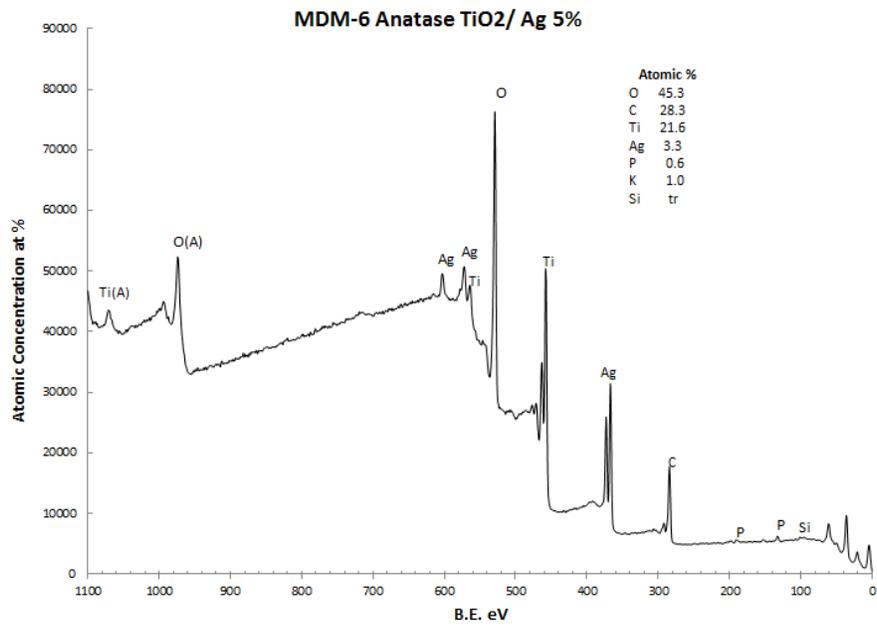


Figure B.11 XPS data for anatase titanium/Ag 5%

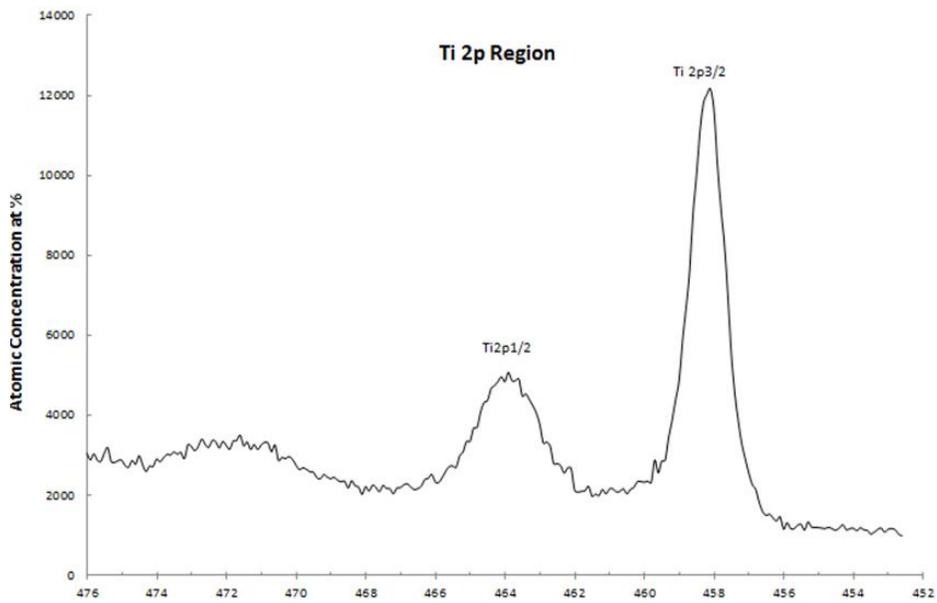


Figure B.12 XPS data for titanium/Ag 5% (Ti 2p region)

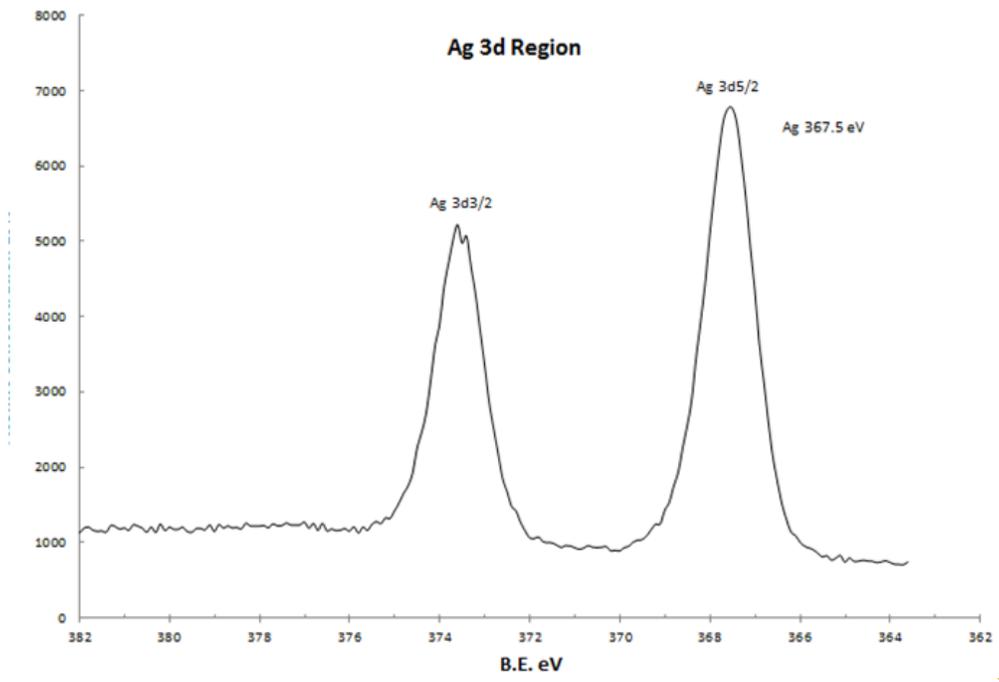


Figure B.13 XPS data for anatase TiO<sub>2</sub>/Ag 5% (Ag 3d region)