

On framing potential features of SWCNTs and MWCNTs in mixed convective flow



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ABSTRACT

Our target in this research article is to elaborate the characteristics of Darcy-Forchheimer relation in carbon–water nanoliquid flow induced by impermeable stretched cylinder. Energy expression is modeled through viscous dissipation and nonlinear thermal radiation. Application of appropriate transformations yields nonlinear ODEs through nonlinear PDEs. Shooting technique is adopted for the computations of nonlinear ODEs. Importance of influential variables for velocity and thermal fields is elaborated graphically. Moreover rate of heat transfer and drag force are calculated and demonstrated through Tables. Our analysis reports that velocity is higher for ratio of rate constant and buoyancy factor when compared with porosity and volume fraction.

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Introduction

A carbon nanotube being shaped material which is isotope of carbon with a cylindrical nanostructure, having a diameter measuring on the nanometer scale. Carbon nanotubes can be subdivided into two categories depending on the structure namely (SWCNTs) and (MWCNTs). Carbon nanotubes have extensive applications in engineering, prostheses, genomics, pharmacogenomics, drug delivery, surgery and general medicine. Choi et al. [1] investigated thermal conductivity enhancement in nanotube suspension. They considered oil based nanoliquids comprising carbon nanotubes and found that nanotubes yields remarkable thermal conductivity enhancement. Impact of non-Fourier heat flux on unsteady chemically reactive flow of SMCNTs and MWCNTs is presented by Hayat et al. [2] They considered Xue model for the effectual thermal conductivity of nanoliquid. They also investigated that Nusselt number enhances for rising values of thermal relaxation and curvature parameters. MHD flow of carbon water nanomaterials with Marangoni convective and thermal radiation due to stretchable disk is examined by Mahanthesh et al. [3]. They implemented Runge–Kutta method through shooting approach to find out the numerical solutions of nonlinear expressions. Their results illustrated that the Nusselt number enhances for larger estimation

of Marangoni number and nanoparticles volume fraction while it decays for Hartman number. MHD slip flow with convective heat transport in the presence of SWCNTs and MWCNTs is scrutinized by Haq et al. [4]. The presence of SWCNTs and MWCNTs in this investigation plays an imperative role in the enhancement of thermal conductivity. Three-dimensional slip flow of SWCNT and MWCNT nanomaterials over a variable thicked surface is studied by Hayat et al. [5]. They have also utilized homogeneous and heterogeneous reactions to regulate the surface temperature. Further their theoretical outcomes presented that heat transfer rate is larger in case of MWCNT + water when compared with SWCNT + water. Recently some representative attempts for flows of SWCNTs and MWCNTs have been presented in Refs. [6–15] and numerous investigations therein.

Thermal motion of the charged particles produces electromagnetic radiation called thermal radiation. Every matter emits thermal radiation at a temperature greater than absolute zero (absolute temperature is also called thermodynamic temperature). When the absolute temperature is less than the body temperature, kinetic energy of molecules change due to inter-atomic collisions. Heat transfer in the presence of thermal radiation has many applications in physics, industrial engineering, space technology for example gas cooled nuclear reactors, aerodynamics rockets, large open water reservoirs, thermal power engineering and so forth. Rosseland approximation has been considered by numerous researchers for radiation effect. This type of approximation

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Nomenclature

u, v	Velocity components	T_m	Melting temperature
C_p	Specific heat	T_∞	Ambient temperature
U_w	Stretching velocity	K	Specific permeability
ν_{nf}	Kinematic viscosity of nanofluid	μ_{nf}	Nanofluid dynamic viscosity
σ^*	Stefan-Boltzman constant	ρ_{nf}	Nanofluid density
$(\rho C_p)_{nf}$	Heat capacity of nanofluid	k_{nf}	Thermal conductivity of nanofluid
q_w	Heat flux	l	Characteristics length
ϕ	Volume fraction of nanoparticles	U_e	Free stream velocity
β^*	Thermal expansion coefficient	μ_f	Dynamic viscosity
ρ_f	Nanofluid density	k^{ast}	Mean absorption coefficient
β_1	Slip parameter	γ	Curvature parameter
σ^*	Stefan-Boltzman constant	Pr	Prandtl number
Re_x	Reynold number	M	Melting parameter
Nr	Radiation parameter	ω	Porosity parameter
θ_w	Temperature ratio variable	κ	Specific or intrinsic permeability
Nu_x	Nusselt number	C_{fx}	Skin friction coefficient
τ_w	Shear stress	q_r	Radiative flux
k	Thermal conductivity		

comprises dimensionless variables called radiation parameter and Prandtl number which are supportable for linearized Rosseland approximation if the temperature difference between the plate and ambient liquid is small. However if the difference is larger than it is valid for non-linearized Rosseland approximation. Radiative flow over a stretched surface is examined by Cortell. [16]. Sheikholeslami et al. [17] investigated MHD two phase nanofluid flow with thermal radiation. Reddy et al. [18] examined the impact of nonlinear radiation in three-dimensional MHD flow of ferromagnetic liquid subject to temperature dependent viscosity. Natural convection along a vertical isothermal plate with linear and nonlinear thermal radiations is studied by Pantokratoras [19]. Consequences of nonlinear thermal radiation and heterogeneous-homogeneous reactions in flow based on Ag-H₂O and Cu-H₂O nanomaterial by a stretched cylinder is presented by Qayyum et al. [20]. Nonlinear radiative flow with temperature dependent viscosity in thin liquid film towards a stretched surface is examined by Pal and Saha [21]. Significance of nonlinear radiation in mixed convection flow of magneto Walter-B nanofluid is explored by Khan et al. [22]. Mixed convective flow with nonlinear thermal radiation of Oldroyd-B liquid near a stagnation region is studied by Hayat et al. [23]. MHD nanofluid slip flow with entropy generation and nonlinear thermal radiation in a porous vertical microchannel is considered by López et al. [24]. Simultaneous effect of gyrotactic microorganisms and nonlinear thermal radiation on Magneto-Burgers nanomaterial is srutinized by Khan et al. [25].

Present work aims to model two-dimensional flow of SWCNTs and MWCNTs with Darcy-Forchheimer porous medium. Heat transfer process is explored subject to nonlinear thermal radiation, melting heat transport and viscous dissipation. Outcomes for SWCNT + Water and MWCNT + Water are achieved and compared. Xue model [15] is employed. The resulting nonlinear expressions are solved via Shooting method [26–36]. Velocity and temperature gradients are computed numerically and analyzed through in Tables 2 and 3.

Simulation of governing problems

Here two-dimensional steady and incompressible flow of water based carbon nanotubes is considered. Flow is due to nonlinear stretching surface. Xue model [15] is accomplished for nanomaterial transport mechanism. Nonlinear thermal radiation and dissipa-

tion effect are accounted. Flow in porous space is characterized by Darcy-Forchheimer relation. Here cylindrical coordinates are chosen in such manner that r-axis is along radial direction while x-axis is along axial direction (see Fig. 1). The governing expressions for mass and momentum are

$$\frac{\partial(rv)}{\partial r} + \frac{\partial(ru)}{\partial x} = 0, \tag{1}$$

$$v \frac{\partial u}{\partial r} + u \frac{\partial u}{\partial x} = U_e \frac{dU_e}{dx} + \nu_{nf} \left(\frac{\partial^2 u}{\partial r^2} + \frac{1}{r} \frac{\partial u}{\partial r} \right) + \frac{\nu_{nf}}{\kappa} (U_e - u) + g\beta_T(T - T_m), \tag{2}$$

$$(\rho c_p)_{nf} \left(v \frac{\partial T}{\partial r} + u \frac{\partial T}{\partial x} \right) = k_{nf} \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r} \right) - \frac{\partial}{\partial r} (q_r) + \mu \left(\frac{\partial u}{\partial r} \right)^2, \tag{3}$$

With

$$\left. \begin{aligned} u &= U_w(x) + \delta_1 \frac{\partial u}{\partial r}, v = 0, T = T_m, \text{ at } r = R \\ u &\rightarrow U_e(x) = \frac{U_\infty x}{l}, T \rightarrow T_\infty, \text{ at } r \rightarrow \infty, \end{aligned} \right\} \tag{4}$$

$$k_{nf} \left(\frac{\partial T}{\partial r} \right)_{r=R} = \rho_{nf} [\lambda_1 + c_s(T_m - T_0)] v(R, x). \tag{5}$$

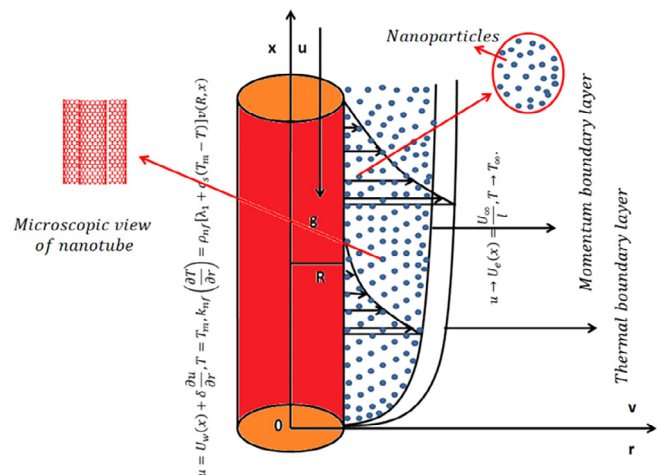


Fig. 1. Schematic flow diagram.

Here u, v represent velocity components, R radius, ρ density, U_e free stream velocity, κ permeability, U_w stretching velocity, ν_{nf} kinematic viscosity, k_{nf} thermal conductivity, c_p specific heat, β_T coefficient of thermal expansion, T temperature, q_r radiative heat flux, l characteristic length, δ_1 velocity slip, λ_1 latent heat and c_s heat capacity.

By Xue [15] one has

$$\left. \begin{aligned} \mu_{nf} &= \frac{\mu_f}{(1-\phi)^{2.5}}, \nu_{nf} = \frac{\nu_{nf}}{\rho_{nf}}, \rho_{nf} = \rho_f(1-\phi) + \rho_s\phi, \\ (\rho c_p)_{nf} &= (\rho c_p)_f(1-\phi) + (\rho c_p)_s\phi, \frac{k_{nf}}{k_f} = \frac{k_s+2k_f-2\phi(k_f-k_s)}{k_s+2k_f+2\phi(k_f-k_s)}, \\ (\rho\beta)_{nf} &= (\rho\beta)_f(1-\phi) + (\rho\beta)_s\phi, \end{aligned} \right\} \quad (6)$$

where μ_{nf} represents dynamic viscosity, ϕ volume fraction of nanoparticle, ρ_f and ρ_s densities of liquid and solid particles, k_f thermal conductivity of continuous phase liquid, k_{nf} thermal conductivity of nanofluid, k_s thermal conductivity of carbon nanotubes, $(c_p)_{nf}$, $(c_p)_f$ and $(c_p)_s$ represent specific heat of nanofluid, base fluid and CNTs respectively.

The radiative heat flux in terms of Rosseland approximation is [20]:

$$q_r = -\frac{4\sigma^*}{3k^*} \frac{\partial T^4}{\partial r} = -\frac{16\sigma^*}{3k^*} T^3 \frac{\partial T}{\partial r}, \quad (7)$$

In above expression k^* denotes the mean absorption coefficient and σ^* denotes the Stefan-Boltzman constant.

Considering

$$\left. \begin{aligned} \eta &= \frac{r^2 - R^2}{2R} \sqrt{\frac{U_0}{\nu_f}}, u = \frac{xU_0}{l} f'(\eta), v = \frac{-R}{r} \sqrt{\frac{\nu_f U_0}{l}} f(\eta), \\ \theta &= \frac{T - T_m}{T_\infty - T_m}, \psi(\eta) = \sqrt{U_w \nu_f x} R f(\eta), \end{aligned} \right\} \quad (8)$$

Eq. (1) is automatically verified and Eqs. (2)–(4) yield

$$\left. \begin{aligned} &\frac{1}{(1-\phi)^{2.5} \left(1-\phi + \frac{\rho_c}{\rho_f} \phi\right)} \left((1+2\gamma\eta) f''' + 2\gamma f'' \right) + \frac{\omega}{(1-\phi)^{2.5} \left(1-\phi + \frac{\rho_c}{\rho_f} \phi\right)} (A-f') \\ &+ \lambda \left(\frac{1-\phi + \frac{(\rho\beta)_c}{(\rho\beta)_f} \phi}{1-\phi + \frac{\rho_c}{\rho_f} \phi} \right) \theta - f'^2 + f f'' + A^2 = 0, \end{aligned} \right\} \quad (9)$$

$$\left. \begin{aligned} &\frac{k_{nf}}{k_f} \frac{1}{\text{Pr} \left(1-\phi + \frac{(\rho c_p)_c}{(\rho c_p)_f} \phi\right)} (2\gamma\theta' + (1+2\gamma\eta)\theta'') \\ &+ \text{Nr} \frac{1}{\text{Pr} \left(1-\phi + \frac{(\rho c_p)_c}{(\rho c_p)_f} \phi\right)} (\theta(\theta_w - 1) + 1)^2 \{ (3\theta^2(1+2\gamma\eta)(\theta_w - 1) \\ &+ 2\gamma\theta'(\theta(\theta_w - 1) + 1) + \theta''(1+2\gamma\eta)(\theta(\theta_w - 1) + 1)) \} \\ &+ \frac{Ec}{(1-\phi)^{2.5} \left(1-\phi + \frac{(\rho c_p)_c}{(\rho c_p)_f} \phi\right)} (1+2\gamma\eta) f'^2 + f\theta' = 0, \end{aligned} \right\} \quad (10)$$

$$\left. \begin{aligned} f'(0) &= 1 + \frac{\beta^*}{(1-\phi)^{2.5}} f''(0), \theta(0) = 0, f'(\infty) = A, \theta(\infty) = 1, \\ \text{Pr} \left(1-\phi + \frac{\rho_c}{\rho_f} \phi\right) f(0) &+ M \frac{k_{nf}}{k_f} \theta'(0) = 0. \end{aligned} \right\} \quad (11)$$

In above expressions $\gamma \left(= \sqrt{\frac{l\nu_f}{U_0 R^2}} \right)$ represents the curvature parameter, $\text{Pr} \left(= \frac{(\rho c_p)_f \nu_f}{k_f} \right)$ the Prandtl number, $\omega \left(= \frac{l\nu_f}{U_0 K} \right)$ the porosity parameter, $\lambda \left(= \frac{Gr}{Re^2 x} \right)$ the mixed convection parameter,

Table 1
Physical properties for nanomaterials and continuous phase liquid.

Thermophysical characteristics	Base fluid	Nanomaterials	
	Water	SWCNT	MWCNT
$\rho(\text{kg}/\text{m}^3)$	997	2600	1600
$c_p(\text{J}/\text{kgK})$	4179	425	796
$k(\text{W}/\text{mK})$	0.613	6600	3000

Table 2
Numerical results of $(Cf_x \text{Re}_x^{\frac{1}{2}})$ for different physical variables.

β	γ	ϕ	M	Nr	Ec	ω	λ	$-Cf_x \text{Re}_x^{\frac{1}{2}}$		
								SWCNT	MWCNT	
0.2	0.1	0.2	0.5	0.8	0.2	0.3	0.4	2.10241	2.00891	
0.3								1.83279 ↑	1.76078	
0.5								1.46558	1.41816	
								2.16560	2.07755	
0.2								2.22733 ↓	2.14422	
0.3								2.34738	2.27301	
0.5								1.69711	1.64382	
								2.10241 ↓	2.00891	
								3.19893	3.06856	
								2.16861	2.06994	
								2.13343 ↑	2.03721	
								2.08819	1.99610	
			0.1	0.1				2.10069	2.00583	
								2.10137 ↓	2.00697	
								2.10241	2.00891	
								2.10785	2.01424	
								2.09163 ↑	1.99835	
								2.07048	1.97763	
								0.1	1.90253	1.79033
									2.00575 ↓	1.90354
									2.10241	2.00891
								0.2	2.24562	2.16071
									2.19748 ↑	2.1098
									2.10241	2.00891
0.4	2.19748 ↑	2.1098								
	2.10241	2.00891								
	2.10241	2.00891								

Table 3
Numerical results of $(Nu_x Re_x^{-\frac{1}{2}})$ for different physical variables.

β	γ	ϕ	M	Nr	Ec	ω	λ	$Nu_x Re_x^{-\frac{1}{2}}$	
								SWCNT	MWCNT
0.1	0.1	0.2	0.5	0.8	0.2	0.3	0.4	-3.80678	-3.62052
0.2								-3.61127 ↓	-3.43972 ↓
0.4								-3.37152	-3.21237
								-3.97809	-3.95358
								-4.3378 ↑	-4.09406 ↑
								-5.0327	-4.72631
								-2.92526	-3.16401
								-3.61127 ↑	-3.43972 ↑
								-5.73744	-5.28077
								-3.93643	-4.36895
								-3.82012 ↓	-3.67172 ↓
								-3.51703	-3.33663
		0.1						-3.14981	-3.38921
		0.2						-3.34662 ↑	-3.17481 ↑
		0.4						-3.61127	-3.43972
			0.2					-3.47514	-3.77364
			0.3					-3.88065 ↑	-3.68915 ↑
			0.6					-4.40807	-4.17676
				0.1			0.1	-3.66602	-3.98068
							0.2	-3.63735 ↓	-3.96615 ↓
							0.4	-3.58744	-3.94266
								-3.56499	-3.94302
								-3.57975 ↑	-3.94559 ↑
								-3.61127	-3.95358

$Gr \left(= \frac{g\beta(T_m - T_\infty)\chi^3}{\nu_f^2} \right)$ the Grashof number, $Nr \left(= \frac{16\sigma^* T_\infty^3}{3k^* k_f} \right)$ the radiation parameter, $\theta_w \left(= \frac{T_w}{T_m} \right)$ the temperature ratio parameter, $Ec \left(= \frac{U_w^2}{(c_p)_f(T_\infty - T_m)} \right)$ the Eckert number and $\beta^* \left(= \delta(U_0 \rho_f l)^{\frac{1}{2}} \right)$ the slip parameter.

Mathematical form for velocity and temperature gradients are

$$\left. \begin{aligned} C_{fx} &= \frac{2\tau_w}{\rho_f U_w^2}, \\ Nu_x &= \frac{xq_w}{k_f(T_w - T_\infty)}, \end{aligned} \right\} \quad (12)$$

where τ_w the shear stress and q_w the surface heat flux and defined as

$$\left. \begin{aligned} \tau_w &= \mu_{nf} \left(\frac{\partial u}{\partial r} \right) \Big|_{r=R}, \\ q_w &= -k_{nf} \left(\frac{\partial T}{\partial r} \right) \Big|_{r=R} + (q_r)_w. \end{aligned} \right\} \quad (13)$$

Invoking Eq. (13) into Eq. (12) we get

$$C_f Re_x^{0.5} = \frac{2f''(0)}{(1 - \phi)^{2.5}}, \quad (14)$$

$$Nu_x Re_x^{-0.5} = - \left(\frac{k_{nf}}{k_f} + Nr(\theta(0)(\theta_w - 1) + 1)^3 \right) \theta'(0), \quad (15)$$

where $Re_x = \frac{U_w x}{\nu_f}$ represents the local Reynold number.

Computational treatment

To solve Eqs. (9) and (10) with boundary conditions (11) numerically, we have apply Built-in-shooting method. This method is well tested procedure to find out the results of ODEs.

Discussion

The objectives of this portion is to investigate the impacts of different physical variables like curvature parameter (γ), porosity parameter (ω), mixed convection parameter (λ), ratio parameter (A), radiation parameter (Nr), melting parameter (M), volume fraction (ϕ), temperature ratio variable (θ_w) and Eckert number (Ec) on the velocity ($f'(\eta)$) and temperature ($\theta(\eta)$) for both SWCNTs and MWCNTs. Table 1 represents the thermophysical characteristics of continuous phase fluid and SWCNTs and MWCNTs. Table 2 presents the numerical data for surface drag force ($C_{fx} Re_x^{0.5}$) for larger values of (Ec), (ω), (λ), (Nr), (γ), (ϕ) and (M) subject to SWCNTs and MWCNTs. Here ($C_{fx} Re_x^{0.5}$) is higher for larger estimation of M , γ , ϕ , Nr and ω . While the reverse trend is observed for Ec , λ and β for both SWCNTs and MWCNTs. Table 3 provides the computational results for heat transfer rate ($Nu_x Re_x^{-\frac{1}{2}}$) for varying (Ec), (ω), (λ), (Nr), (γ), (ϕ) and (M) in both SWCNTs and MWCNTs cases. It is examined that rate of heat transfer enhances for different estimations of (Ec), (M), (β), and λ while it decays for (γ), ω , Nr ,

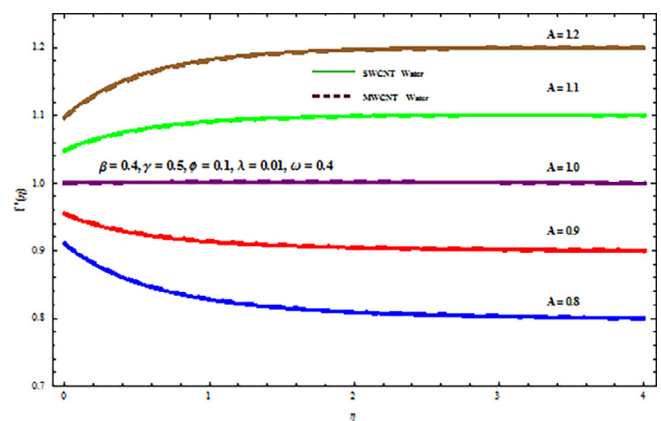


Fig. 2. $f'(\eta)$ via A.

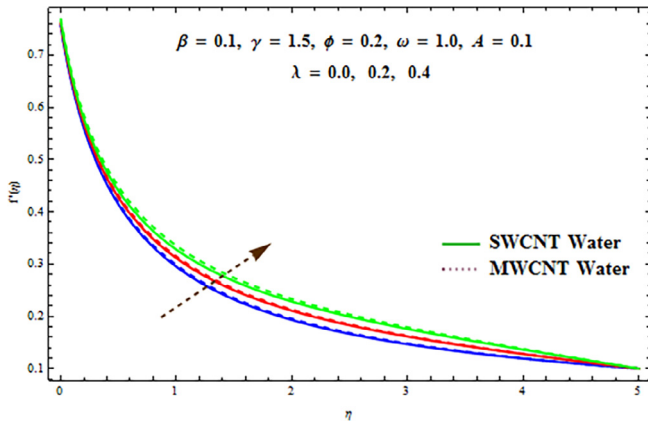


Fig. 3. γ via λ .

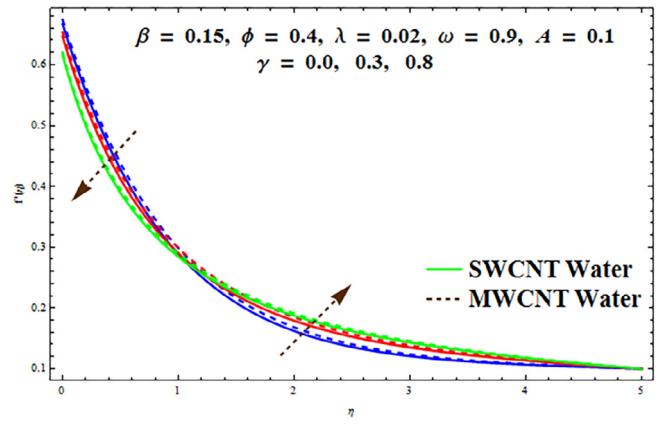


Fig. 6. $f'(\eta)$ via γ .

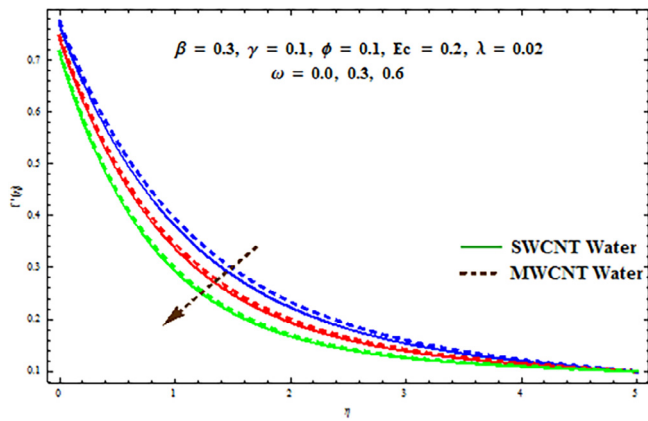


Fig. 4. $f'(\eta)$ via ω .

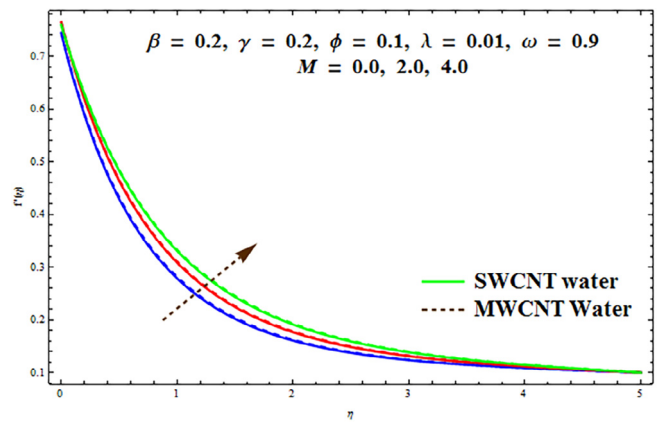


Fig. 7. $f'(\eta)$ via M .

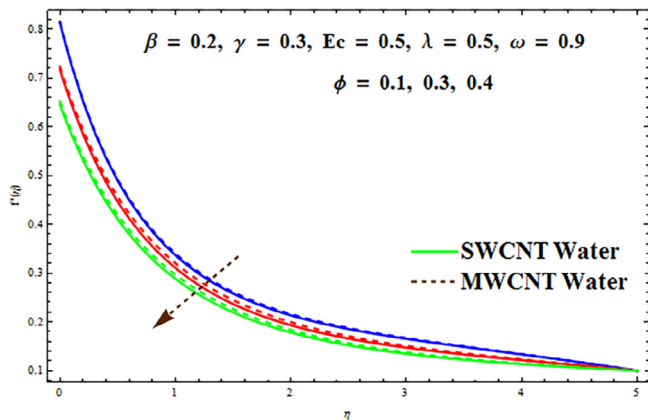


Fig. 5. $f'(\eta)$ via ϕ .

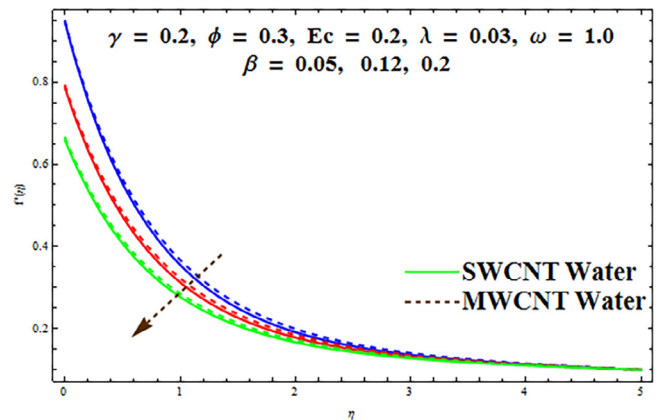


Fig. 8. $f'(\eta)$ via β .

Ec and ω . Behavior of (A) on $(f'(\eta))$ is pictured in Fig. 2. Here $(f'(\eta))$ enhances for both SWCNTs and MWCNTs. Here no boundary layer exists for $A = 1$. In fact both fluid and cylinder move at the same velocity. It is also pointed out that $(f'(\eta))$ have distinct values on the surface of cylinder due to slip condition. Characteristics of (λ) on $(f'(\eta))$ is shown in Fig. 3. Here velocity $f'(\eta)$ and layer thickness are enhanced for higher (λ) . physically (λ) is the ratio of inertial to buoyancy forces. Therefore for various values of (λ) buoyancy force enhances and as a result $(f'(\eta))$ boosts. Fig. 4 demonstrates effect of

porosity variable (ω) on $(f'(\eta))$. Here reduction in $(f'(\eta))$ is noticed for higher (ω) , Variation in velocity $(f'(\eta))$ for higher (ϕ) is shown in Fig. 5. It can be noticed that $(f'(\eta))$ decays with (ϕ) for both SWCNTs and MWCNTs. It is also marked that $(f'(\eta))$ of nanoliquid is larger than of pure liquid $(\phi = 1)$. Effect of (γ) on $(f'(\eta))$ is displayed in Fig. 6. Here both velocity and momentum layer thickness decrease near surface of cylinder while contrast effects are observed away from the surface of cylinder. Also radius of cylinder

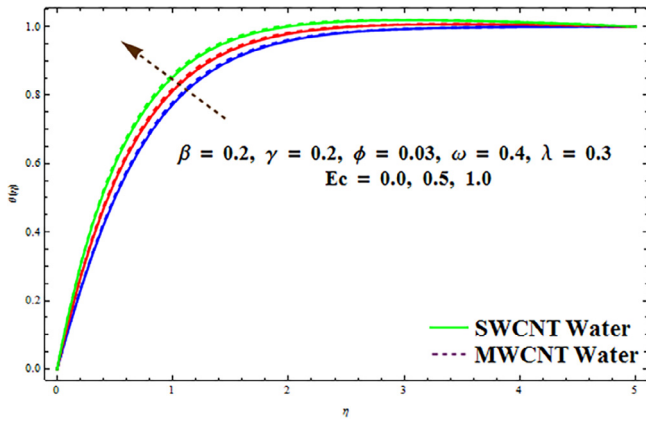


Fig. 9. $\theta(\eta)$ via Ec .

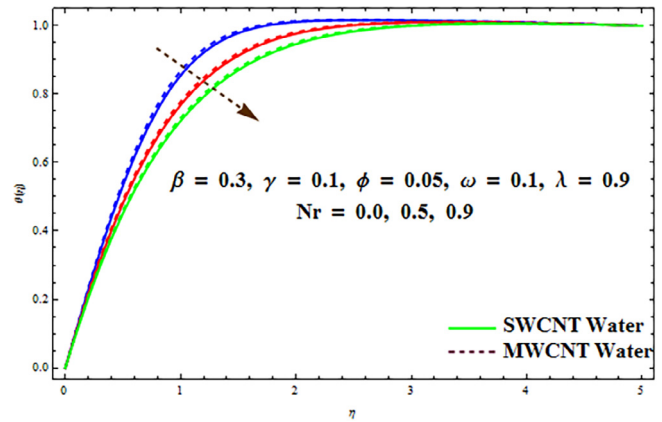


Fig. 12. $\theta(\eta)$ via Nr .

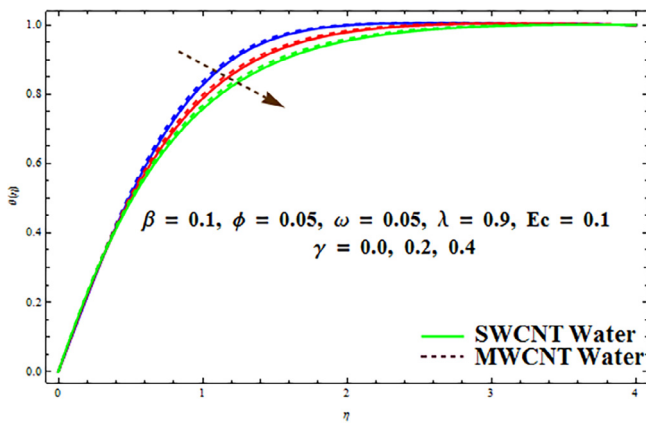


Fig. 10. $\theta(\eta)$ via γ .

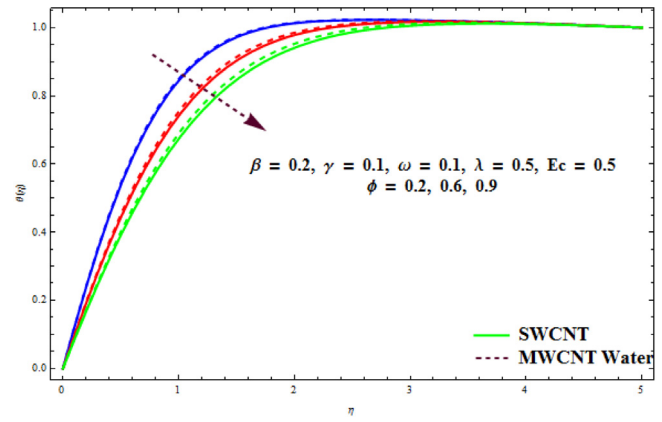


Fig. 13. $\theta(\eta)$ via ϕ .

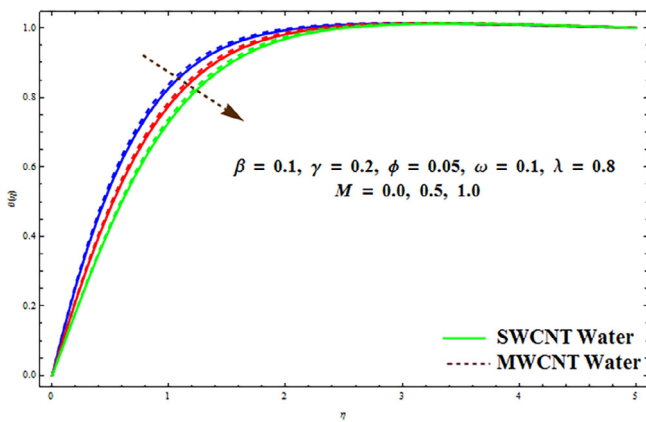
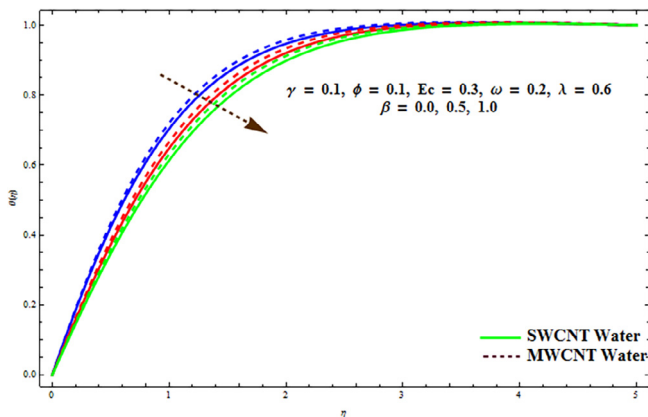
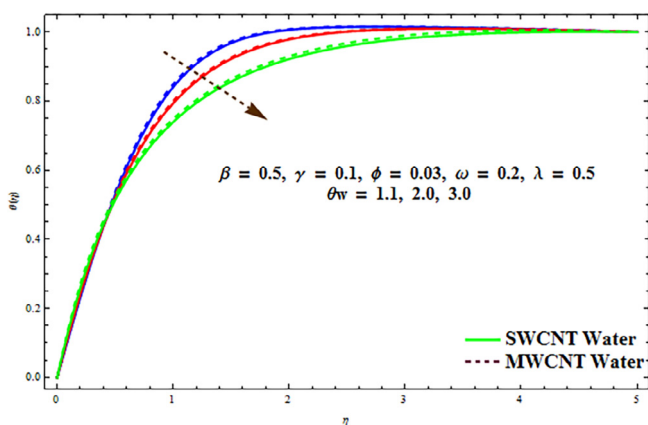


Fig. 11. $\theta(\eta)$ via M .

R decreases for larger curvature parameter(γ). Therefore less particles accommodate on the cylinder surface and as a results less resistance provides to fluid particle. That is why ($f'(\eta)$) increases away from the surface of cylinder. Fig. 7 Indicates that the larger estimations of (M) causes an increase in ($f'(\eta)$) for both SWCNTs and MWCNTs. In fact larger values of (M) lead more heat transport from heated liquid to cold melting surface of cylinder due to the high convection. Therefore velocity and momentum layer thickness increase. Influence of slip parameter (β) on ($f'(\eta)$) is sketched in Fig. 8. Here both velocity and associated layer thickness decay

for higher (β). Moreover ($f'(\eta)$) dominants in case of MWCNTs when compared with SWCNTs. Fig. 9 Captures the influence of Eckert number (Ec) on ($\theta(\eta)$). Temperature is increasing function of higher estimation of Eckert number (Ec). Also thermal layer thickness increases for both SWCNTs and MWCNTs. $\theta(\eta)$ against curvature variable (γ) is exhibited in Fig. 10. Here ($\theta(\eta)$) show dual behavior for larger (γ). with an enhancement in curvature parameter radius of cylinder decays and as a result temperature increases near the surface of cylinder. Temperature diminishes as the radius of cylinder enhances. Consequences of melting parameter (M) on $\theta(\eta)$ is depicted in Fig. 11. Here temperature increases for both SWCNTs and MWCNTs for higher values of (M). It is also investigated that thermal layer thickness enhances for higher melting

Fig. 14. $\theta(\eta)$ via β .Fig. 15. $\theta(\eta)$ via θ_w .

variable. Physically larger melting parameter (M) provides more heat from heated fluid surface to cold surface of cylinder. Fig. 12 depicts the change in temperature field ($\theta(\eta)$) for varying radiation parameter. An increase in (Nr) leads to higher temperature field for both cases i.e., MWCNTs and MWCNTs. Generally larger values of (Nr) produce extra heat to operating liquid that shows associate improvements within ($\theta(\eta)$). Fig. 13 presents that rising values of nanoparticle volume fraction (ϕ) correspond to lower ($\theta(\eta)$) for both MWCNTs and MWCNTs. Physically higher estimations of (ϕ) result in an enhancement of heat transfer by convection phenomenon from heated fluid towards cold surface due to which temperature diminished. Influence of slip parameter (β) on $\theta(\eta)$ is shown in Fig. 14. It is observed that temperature along with thermal layer thickness reduce as (β) rises gradually. Since with the increment in (β) the rate of heat transfer at the surface increases. Therefore temperature field declines. Fig. 15 illustrates effect of (θ_w) on $\theta(\eta)$. Clearly temperature field is a decreasing function of (θ_w).

Conclusions

The main conclusions drawn from the study are as follows:

- Velocity field decreases via (ϕ) and (ω).
- Larger estimation of (M) and (λ) leads to increase of $f'(\eta)$ and momentum layer thickness.
- Both $f'(\eta)$ and $\theta(\eta)$ show dual nature for rising values of (γ).
- Temperature field decays for larger (M), (β) and (Nr). Higher estimations of (M) and (Nr) increase the rate of heat transfer as well as thermal layer. ($Cf_x Re_x^{-1/2}$) decreases for large a (ϕ) and it enhances via (M) and (Ec).

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